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# Thermal decomposition of Li<sub>3</sub>AlH<sub>6</sub> with TiAl<sub>3</sub> catalyst

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#### Abstract

It has been found that the reaction products between TiCl<sub>3</sub> and Li<sub>3</sub>AlH<sub>6</sub> by mechanical milling consist of LiCl and TiAl<sub>3</sub> together with TiH<sub>2</sub>. Thermodynamic calculation also predicts that TiAl<sub>3</sub> becomes dominant over TiH<sub>2</sub> with increasing temperature. Based on this, ultra-fine TiAl<sub>3</sub> powder having the primary particle size of about 100 nm has been mechanochemically synthesized from a mixture of TiCl<sub>3</sub>, AlCl<sub>3</sub> and Mg. The addition of this TiAl<sub>3</sub> powder into Li<sub>3</sub>AlH<sub>6</sub> clearly shows a good catalytic effect on the thermal decomposition of Li<sub>3</sub>AlH<sub>6</sub> as expected. The use of fine TiAl<sub>3</sub> catalyst is certainly more favorable than TiCl<sub>3</sub> in terms of hydrogen storage capacity as it does not produce irreversible chloride byproduct in alanates.

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### 1. Introduction

The development of solid-state hydrogen storage at low and medium temperatures has been recognized as one of the key technologies for hydrogen fuel cell applications. Especially for vehicular applications, it is important to find new light-weight hydrogen storage materials that exhibit high reversible hydrogen capacity [1].

Alkali and alkali-earth metal alanates (aluminum hydrides) have received great attention as promising hydrogen storage materials owing to their inherent high theoretical hydrogen capacity, since Bogdanović and Schwickardi [2] first demonstrated in 1997 that reversible hydrogen storage could be achieved under moderate conditions (temperature and pressure) with accelerated kinetics in NaAlH<sub>4</sub> and Na<sub>3</sub>AlH<sub>6</sub> by adding a small amount of Ti-containing catalysts such as TiCl<sub>3</sub> and Ti(OBu)<sub>4</sub> through wet chemistry. Following this finding, Jensen and his coworkers [3,4] reported improved kinetics by dispersing Ti-containing catalysts using a dry milling process. Currently, mechanical ball milling is being widely adopted to disperse a small amount of catalysts effectively into sodium

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alanates in solid state [5,6]. In addition to sodium alanates, it has been shown that other alanates such as lithium alanates could also be catalyzed with Ti-containing materials [7]. In spite of the outstanding performance of Ti-containing catalysts, there is still no clear understanding on how they play a catalytic role in alanates. The first step toward the understanding of this catalytic mechanism would be to confirm what form of Ti exists in alanates. However, it is quite difficult to confirm unambiguously the state of Ti (e.g. metallic Ti, Ti compounds or Ti substitution in alanates) in alanates using most analytical techniques, because a very small amount of Ticontaining catalysts are usually added. On the whole, there exit two hypotheses on the Ti state in alanates. While the results of recent investigations [8–12] seem to support the hypothesis that Ti in situ forms TiAl<sub>3</sub> when introduced into alanates, there is another hypothesis that Ti substitutes for metal sites in alanates [13-15].

Assuming that Ti does transform into TiAl<sub>3</sub> in alanates, it is worthwhile to confirm its efficacy by adding TiAl<sub>3</sub>, instead of TiCl<sub>3</sub>, into alanates because TiCl<sub>3</sub> permanently reduces hydrogen storage capacity of alanates by reacting with part of alanates to form very stable salts such as NaCl and LiCl. In fact, Balema et al. [8] and Resan et al. [16] have recently attempted to confirm the catalytic activity of TiAl<sub>3</sub> by dispersing TiAl<sub>3</sub> powder prepared by milling the arc melted

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Fig. 1. Calculated stability diagram of LiH, Li<sub>3</sub>AlH<sub>6</sub> and LiAlH<sub>4</sub> [18].

sample and commercial powder (<150  $\mu$ m), respectively, into LiAlH<sub>4</sub>. They showed that the addition of TiAl<sub>3</sub> indeed decreased the dehydrogenation starting temperature of LiAlH<sub>4</sub> by about 10 °C, although the catalytic effect may not be significant. It is, therefore, desirable to produce as fine TiAl<sub>3</sub> powder as possible as the catalytic efficacy will be naturally enhanced with decreasing particle size of catalyst. Mechanical milling is one of the simple and cost-effective methods for producing TiAl<sub>3</sub> powders. However, it might be difficult to obtain fine TiAl<sub>3</sub> particles using conventional milling techniques because TiAl<sub>3</sub> is relatively ductile and thus they easily agglomerate during milling [17].

The purpose of this study is to elucidate if TiCl<sub>3</sub> indeed forms TiAl<sub>3</sub> in Li<sub>3</sub>AlH<sub>6</sub> using both experimental work and theoretical calculations and to investigate the catalytic effect of TiAl<sub>3</sub> on thermal decomposition (dehydrogenation) of Li<sub>3</sub>AlH<sub>6</sub> using ultrafine TiAl<sub>3</sub> powder prepared by mechanochemical reaction between TiCl<sub>3</sub>, AlCl<sub>3</sub> and Mg powders. The main reason to adopt Li<sub>3</sub>AlH<sub>6</sub> (5.6 wt.% H<sub>2</sub>) instead of LiAlH<sub>4</sub> (7.9 wt.% H<sub>2</sub>) is that the hydrogen pressure required to rehydrogenate LiAlH<sub>4</sub> is estimated to be an order of 10<sup>4</sup> bar, according to our recent thermodynamic calculation shown in Fig. 1 [18].

# 2. Experimental procedure

LiAlH<sub>4</sub> (95%), LiH (95%), TiCl<sub>3</sub> (99%) and AlCl<sub>3</sub> (99.9%) powders were purchased from Sigma–Aldrich, and Mg (99.8%) powder from Alfa–Aesar. In order to synthesize Li<sub>3</sub>AlH<sub>6</sub> mechanochemically, a 5 g mixture of LiAlH<sub>4</sub> and LiH with a molar ratio of 1:2 was charged together with ten 15 mm and thirty 10 mm diameter zirconia balls into a 250 ml silicon nitride bowl under an argon atmosphere in a glove box. The ball-to-powder weight ratio was approximately 37:1. The mixture was milled in a Fritsch P4 planetary mill at 350 rpm for 4 h 30 min.

A 1 g mixture of mechanochemically prepared  $Li_3AlH_6$  and  $TiCl_3$  was charged together with seventeen 7.9 mm diameter Cr-steel balls into a tool steel vial under an argon atmosphere. The ball-to-powder weight ratio was approximately 35:1. The mixture was milled in a SPEX-8000 mill for 2 h. Some of the milled powders were rinsed in distilled water and filtered to remove chloride formed during milling. The mole ratio between  $Li_3AlH_6$  and  $TiCl_3$  was changed from 1:1 to 6:1.

In order to synthesize fine TiAl<sub>3</sub> mechanochemically, a mixture of TiCl<sub>3</sub>, AlCl<sub>3</sub> and Mg powders with a molar ratio of 1:3:6 was milled for 4 h using the SPEX-8000 mill at the same milling condition as described before. The milled powder was rinsed in distilled water and filtered to remove MgCl<sub>2</sub> byproduct formed during milling.

The product powders were characterized by X-ray diffraction (XRD) using Bruker D8 Advance with Cu K $\alpha$  radiation and scanning electron microscopy (SEM) using FEI XL-30 FEG.

In order to confirm the catalytic effect of fine TiAl<sub>3</sub> on the thermal decomposition of  $Li_3AlH_6$ , 5 mol% TiAl<sub>3</sub> was dispersed into  $Li_3AlH_6$  by milling the mixture in the SPEX-8000 mill for 30 min. The same amount of TiCl<sub>3</sub> was also dispersed into  $Li_3AlH_6$  for comparison. The thermal decomposition behavior of  $Li_3AlH_6$  with and without catalyst was analyzed by differential scanning calorimetry (DSC) using NETSCH DSC204 and thermogravimetry (TG) using NETSCH TG209. The heating rate was 2 °C/min and the flow rate of 99.9999% argon gas was 50 ml/min for both DSC and TG measurements. The kinetics of the thermal decomposition reaction was volumetrically measured by a Sievert type apparatus.

# 3. Thermodynamic calculation

Thermodynamic calculation of the Li–Al–H–Ti–Cl system was performed based on the Gibbs-energy minimization criterion [19] to understand what the equilibrium phases are in the Li<sub>3</sub>AlH<sub>6</sub> and TiCl<sub>3</sub> mixtures. The phases included in this calculation were Li<sub>3</sub>AlH<sub>6</sub>, LiAlH<sub>4</sub>, LiH, TiCl<sub>3</sub>, LiCl, Ti, Al, TiAl, TiAl<sub>3</sub>, Ti<sub>3</sub>Al, TiAl<sub>2</sub>, Ti<sub>5</sub>Al<sub>11</sub>, TiH<sub>2</sub> and H<sub>2</sub>. The Gibbs energy data for Li<sub>3</sub>AlH<sub>6</sub> and LiAlH<sub>4</sub> were taken from Ref. [18]. The data for the Ti–Al intermetallic phases and all the other phases were from the SGTE solution and substance databases, respectively, which are incorporated into Thermo-Calc [20].

## 4. Results and discussion

The XRD pattern of the mixture of  $\text{LiAlH}_4$  and LiH milled for 4 h 30 min is presented in Fig. 2. The peak positions are in good agreement with those of  $\text{Li}_3\text{AlH}_6$  obtained by Zaluski et al. [21] and Balema et al. [22]. It is, therefore, confirmed that  $\text{Li}_3\text{AlH}_6$  forms during milling according to the following reaction:

$$LiAlH_4 + 2LiH \rightarrow Li_3AlH_6 \tag{1}$$

The XRD patterns of reaction products between  $LiAlH_6$  and  $TiCl_3$  milled for 2 h are shown in Fig. 3. For the 6:1 mixture,

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