

Article

Promotion of Ni/clay catalytic activity for hydrogenation of naphthalene by organic modification of clay

Shibiao Ren *, Hongzhi Wen, Xianzhong Cao, Zhicai Wang, Zhiping Lei, Chunxiu Pan, Shigang Kang, Hengfu Shui #

Anhui Key Laboratory of Clean Coal Conversion and Utilization, School of Chemistry and Chemical Engineering, Anhui University of Technology, Ma'anshan 243002, Anhui, China

ARTICLE INFO

Article history: Received 7 December 2013 Accepted 7 January 2014 Published 20 April 2014

Keywords: Nickel Organic montmorillonite High activity Naphthalene Hydrogenation

ABSTRACT

A Ni/montmorillonite (MMT) catalyst was prepared by an impregnation method using cetyltrimethylammonium bromide (CTAB)-pillared MMT as the supporting matrix and was characterized using infrared spectroscopy, X-ray diffraction, H₂ temperature-programmed desorption, N₂ adsorption-desorption, and ultraviolet diffuse reflectance spectroscopy. The catalytic activity of the Ni/MMT for the hydrogenation of naphthalene was also evaluated. The results show that the organic modification of MMT greatly improved the Ni dispersion and textural properties of the Ni/MMT catalyst. The as-prepared Ni/MMT catalyst showed high naphthalene conversion (88.2%) in the hydrogenation reaction; this is much higher than those achieved using Ni supported on pristine MMT (13.1%), Al₂O₃-pillared MMT (24.2%), and SBA-15 (68.2%). As a result of thermal decomposition of CTAB pillars during reduction of the Ni/MMT catalyst, the CTAB pillars mainly play a role in the Ni/MMT catalyst during impregnation. A mechanism for the promotion of the Ni/MMT catalytic activity by organic modification during impregnation is proposed.

> © 2014, Dalian Institute of Chemical Physics, Chinese Academy of Sciences. Published by Elsevier B.V. All rights reserved.

1. Introduction

Supported Ni catalysts are used in various industrially important chemical processes such as (de)hydrogenation, methanation, reforming, and hydrocracking [1–5]. Inorganic-pillared clays (PILCs) have been widely used as catalysts due to their high specific surface areas and pore volumes, and tunable pillars [6–8]. Therefore, PILC-supported Ni catalysts have been investigated [9–12]. However, the use of organic-PILCs is limited because of their low thermal stability at high temperatures.

Recently, supported noble-metal catalysts with excellent performance have been designed and prepared, based on the organophilic characteristics of organic-PILCs [13,14], which improve catalyst dispersion in organic solvents [13] and enable tuning of the catalyst polarity [14]. The organophilic characteristics of the catalysts are destroyed by thermal decomposition of the organic pillars at high temperatures, so catalysts derived from organic-PILCs need to be prepared and used at low temperatures (usually below 100 °C) [13,14]. Ni catalysts are usually used at high temperatures, so they are not suitable for use in catalysts designed on the basis of the organophilic characteristics are used.

This work was supported by the Project of Coal Joint Fund from Natural Science Foundation of China and Shenhua Group Corporation Limited (U1361125, U1261208), the Natural Scientific Foundation of China (21176001,51174254), the Provincial Innovative Group for Processing & Clean Utilization of Coal Resource, and Innovative Research Team in Anhui University of Technology.

DOI: 10.1016/S1872-2067(14)60028-0 | http://www.sciencedirect.com/science/journal/18722067 | Chin. J. Catal., Vol. 35, No. 4, April 2014

^{*} Corresponding author. Tel: +86-555-2311367; Fax: +86-555-2311822; E-mail: rensb@ahut.edu.cn

[#] Corresponding author. Tel: +86-555-2311367; Fax: +86-555-2311822; E-mail: shhf@ahut.edu.cn

teristics of organic clays. However, highly dispersed metal oxide catalysts can be obtained using as-prepared mesoporous materials because the templates in such materials can occlude and interact with introduced species [15]. Organic clays are very similar to the mesoporous materials; an organic pillar such as cetyltrimethylammonium bromide (CTAB) is usually used as a template in the preparation of MCM-41, and the basal spacing of the clay is enlarged by the large organic pillar molecules. Highly dispersed Ni catalysts could therefore be obtained using organic-PILCs as the supporting matrixes.

Hydrogenation of aromatic hydrocarbon is normally used for catalytic tests because it is not only a useful model reaction for evaluating the activity of metal catalysts, but is also of commercial importance in the upgrading of coal liquids and diesel fuels [16–19]. Here, a highly active Ni/montmorillonite (MMT) catalyst for naphthalene hydrogenation was prepared via an impregnation method, using CTAB-pillared MMT as the supporting matrix. Ni supported on Al₂O₃-pillared MMT was also prepared for comparison. The mechanism of the promoting effect of CTAB pillars on the Ni/MMT catalyst is discussed.

2. Experimental

2.1. Catalyst preparation

Preparation of CTAB-pillared MMT (MMT-CTAB). Na-MMT (Zhejiang Sanding Group Co., Ltd.) was used directly without further purification. Na-MMT (2.0 g) was dispersed in H₂O (100 mL) and CTAB (2.0 g) was dissolved in H₂O (50 mL). The CTAB aqueous solution was slowly added to the Na-MMT suspension at 80 °C. After ion exchanging for 8 h, the suspension was subjected to centrifugation. Excess CTAB was removed by washing the solid several times with 50% ethanol until no Br- ions were detected using AgNO₃ solution. After drying at 80 °C for 12 h, MMT-CTAB was obtained.

Preparation of Al₂O₃-pillared MMT (MMT-Al₂O₃). Na-MMT (1.0 g) was dispersed in H₂O (200 mL). The Al polycations as the pillar agent [20] were obtained by microwave-assisted hydrolysis of AlCl₃ via decomposition of urea. The Na-MMT suspension was then equilibrated with the Al polycation solution (25 mmol) for 20 h, and the product was separated by centrifugation. The solid was washed several times with H₂O until no Cl⁻ ions were detected using AgNO₃ solution. After drying at 120 °C for 12 h, and then calcined at 550 °C for 4 h, the MMT-Al₂O₃ was obtained.

Preparation of Ni/MMT, Ni/MMT-CTAB, and Ni/MMT-Al₂O₃. MMT, MMT-CTAB, or MMT-Al₂O₃ (1.0 g) was impregnated with an aqueous solution containing required amount of Ni(NO₃)₂·6H₂O (0.3 mol/L) under stirring at 60 °C until dryness, and drying at 100 °C overnight. The supported Ni precursors were then reduced at 550 °C by H₂ flow (30 mL/min) for 4 h, and passivated in 1.0% O₂/N₂ flow at room temperature for 3 h to obtain the supported Ni catalysts, i.e. Ni/MMT, Ni/MMT-CTAB, and Ni/MMT-Al₂O₃. The Ni loading on each catalyst was 10.0 wt%, determined by flame atomic absorption spectroscopy (TAS-990F, Beijing Purkinje General Instrument Co., Ltd.).

2.2. Catalyst characterization

Fourier-transform infrared (FT-IR) spectra were recorded using a Nicolet 6700 FT-IR spectrometer at a resolution of 4 cm⁻¹. X-ray diffraction (XRD) data were obtained with a Shimadzu XD-3A diffractometer, using Cu K_{α} radiation (λ = 0.15418 nm) at 40 kV and 40 mA. The specific surface areas and pore structure were determined by N2 adsorption-desorption at -196 °C using a Micromeritics ASAP 2420 analyzer. H₂ temperature-programmed desorption (H₂-TPD) experiments were carried out using a Quantachrome instrument (ChemBET 3000) as described previously [21,22]. Before the measurements, the catalyst (50 mg) was heated to 550 °C in 10% H₂/Ar at a rate of 20 °C/min, and kept at 550 °C for 0.5 h. The catalyst was then cooled to 40 °C and kept at this temperature for 0.5 h. The H₂/Ar flow was then switched to pure Ar (40 mL/min) for 0.5 h at 40 °C. Finally, the catalyst was heated from 40 to 500 °C at a rate of 10 °C/min, and the H₂-TPD curve was recorded. The peak area was used to calculate the volume of chemisorbed H₂. The peak area was calibrated by running a pure H₂ pulse-titration experiment on a blank sample. The Ni surface area (S, m^2/g), dispersion of metallic Ni (D, %) and average particle size of metallic Ni (d, nm) were calculated from the volume of H₂ chemisorbed, using the reported method [21,22]. Ultraviolet diffuse reflectance spectroscopy (UV-DRS) was performed in the range 200-800 nm using a PE Lambda 750S spectrophotometer.

2.3. Catalytic hydrogenation of naphthalene

Naphthalene hydrogenation was performed in a 60 mL stainless-steel autoclave (Ordino CS340, Premex) equipped with a heating system and a magnetic-coupled paddle stirrer. In a typical run, a solution of naphthalene in *n*-dodecane (10.0 wt%; 10 g) and catalyst (0.12 g) were loaded into the reactor. The reaction conditions were 300 °C and $p(H_2) = 5.0$ MPa. Each catalytic test was performed for 2.0 h. The reaction products were analyzed using a gas chromatograph (GC-7890II, Tech-Com) equipped with an OV-1 column (30 m × 0.25 mm × 0.33 µm) and a flame ionization detector.

3. Results and discussion

3.1. Characterization of MMT-CTAB

MMT-CTAB was obtained by ion exchange of CTAB onto MMT. FT-IR spectra of MMT, MMT-CTAB, and CTAB were recorded between 4000 and 400 cm⁻¹ to determine whether the organic cations were exchanged onto MMT (Fig. 1(a)). Unlike the spectrum of pristine MMT, the C-H bonds (2919, 2849 cm⁻¹) of methylene groups for CTAB are clearly observed in the MMT-CTAB. CTAB adsorbed on the external surface of MMT was washed out during preparation of MMT-CTAB, so it indicates CTAB intercalation into MMT interlayers. The basal spacing of MMT-CTAB was characterized using XRD in the small-angle range (Fig. 1(b)). Similar to the results obtained by Su group [23], the basal spacing of MMT was 1.24 nm, and the Download English Version:

https://daneshyari.com/en/article/59780

Download Persian Version:

https://daneshyari.com/article/59780

Daneshyari.com