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Promotion by Co of a NiO-BaCO₃ catalyst for N₂O decomposition



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1. Introduction

Nitrous oxide (N₂O) destroys the ozone in the stratosphere and it is a strong greenhouse gas [1,2]. The continuous increase of its concentration in the atmosphere is mainly from the tail gas of adipic acid and nitric acid plants [3]. This calls for the developing of efficient catalysts for its decomposition into N₂ and O₂.

In recent years, 3*d* transition metal oxides such as Co_3O_4 [4–12], NiO [13,14], Fe₃O₄ [15], and CuO [16] have been shown to exhibit high activity for N₂O decomposition. Fundamental and applied research has focused on these materials, in particular on Co_3O_4 based materials. Many additives have been studied to improve the catalytic activity of Co_3O_4 . The alkali metals Na⁺, K⁺, Cs⁺ [4,5,9–11] and alkaline earth metals Mg²⁺ [8], Ca²⁺, Ba²⁺ [12] and some other transition metals like Ce [6], Ni, Zn [7,8] have been reported to be effective. On the other hand, although NiO has a comparable catalytic activity to Co_3O_4 [11], fewer additives for it have been investigated, apart form Cs [13] and Ce [14]. Concerning the mechanism of the additive promo-

ABSTRACT

A series of $Co_x Ba_{1.5}Ni_9$ catalysts prepared by a co-precipitation method were investigated for N_2O decomposition. Co improved the activity of NiO when $BaCO_3$ was present but had the opposite role when it was absent. This was because Co strengthened the Ni–O bond and decreased the surface area when added into pure NiO without $BaCO_3$, while in the presence of $BaCO_3$, it dramatically increased the surface area and amount of active sites of NiO.

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tion of the NiO catalyst, it was reported that Cs [13] significantly facilitated the desorption of the oxygen produced from N_2O decomposition by weakening the Ni–O bond. In the case of Ce as additive, the promotional effect was attributed to a significant increase of the catalyst surface area since it did not much strengthen the Ni–O bond [14]. This influence of Ce on NiO was confirmed in our previous work [17], and on this basis, we suggested that BaCO₃ not only played the same role as Cs, but also increased the surface area of the catalyst.

In the present work, a Co-modified NiO-BaCO₃ catalyst was studied, and a significant promotional effect by Co on the activity of NiO in the presence of $BaCO_3$ was found.

2. Experimental

All catalysts were prepared by the co-precipitation method with the following procedure. A Na₂CO₃ aqueous solution (0.2 mol/L) was added dropwise to a mixed solution containing known amounts of Ni(NO₃)₂·6H₂O and Ba(NO₃)₂ at 40 °C with strong stirring until the pH of the solution was 9.3. The slurry

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Fig. 1. (a) XRD patterns of the catalysts; (b) Amplification of the (200) (according to JCPDS 78-0643) reflection of NiO.

was stirred for an additional 2 h before it was filtered. Then the resultant precipitate was washed with distilled water until the pH of the filtrate reached 7. This sample was dried at 100 °C overnight, followed by calcination at 500 °C in air for 3 h. The catalysts were labeled as CoxNi9 or CoxBa1.5Ni9 according to the mole ratios of Co(NO₃)₂·6H₂O and Ba(NO₃)₂ to Ni(NO₃)₂·6H₂O in the mixed solution used for the catalyst preparation.

The characterization of the catalysts with X-ray diffraction, H₂ temperature-programmed reduction, O₂ temperature-programmed desorption, N₂ adsorption-desorption for measuring the BET surface area, and the activity tests were the same as our previous work [17].

3. **Results and discussion**

3.1. Structural properties

Figure 1 presents the XRD patterns of the catalysts. No diffraction peak belonging to Co₃O₄ or other cobalt oxide was observed on the Co1.0Ni9 and Co1.0Ba1.5Ni9 catalysts, indicating that the cobalt was well dispersed on them. Moreover, the diffraction peaks of NiO for the Co1.0Ni9 and CoxBa1.5Ni9 catalysts were obviously shifted to lower angles as compared to pure NiO and Ba1.5Ni9, respectively. This resulted from the larger crystalline interplanar spacing of the (111), (200), (220), and (311) planes for Co1.0Ni9 and CoxBa1.5Ni9 with respect to their counterparts (Table 1). This is consistent with the radius of Co^{2+} (72 pm) > Ni²⁺ (69 pm). The result indicated that Co²⁺ was incorporated into the NiO phase and partially replaced Ni²⁺ in the Co_{1.0}Ni₉ and Co1.0Ba1.5Ni9 catalysts. Table 1 shows the BET surface areas

Table 1

Textural	l and	crystal	properties	of the	catalysts
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	BET surface	Crystal	d values (nm)					
Catalyst	area (m²/g)	sizeª (nm)	(111)	(200)	(220)	(311)		
NiO	29	18	0.2406	0.2083	0.1475	0.1258		
Co _{1.0} Ni ₉	9	21	0.2413	0.2090	0.1478	0.1260		
Ba _{1.5} Ni ₉	32	9	0.2406	0.2083	0.1475	0.1258		
Co1.0Ba1.5Ni9	41	13	0.2413	0.2090	0.1478	0.1260		
^a Calculated from XRD analysis according to Scherer's equation [18]								

of the catalyst samples. The surface area drastically decreased due to the formation of a solid solution (Co dissolved into NiO) in Co_{1.0}Ni₉. Interestingly, when BaCO₃ was in the catalyst, the opposite occurred. For Ba1.5Ni9 and Co1.0Ba1.5Ni9, the specific surface areas were 32 and 41 m^2/g , respectively, indicating that Co was effective for increasing the surface area of the NiO-BaCO3 catalyst.

3.2. Chemical properties

Figure 2 exhibits the H2-TPR profiles of the NiO, Co1.0Ni9, Ba1.5Ni9, and Co1.0Ba1.5Ni9 catalysts. Three H₂ consumption peaks at 360, 408, and 435 °C appeared for pure NiO. The two peaks at the lower temperature were associated with the NiO reduction steps of NiO \rightarrow Ni^{$\delta_+}<math>\rightarrow$ Ni^{0.33} [14], while that at the</sup> higher temperature was due to the reduction of NiO and Ni δ^+ inside larger NiO crystallines. Over Ba1.5Ni9, the last peak nearly did not appeared, which was associated with the small crystallite size of NiO in the sample (Table 1). Compared to the pure NiO, all of the H₂ consumption peaks of Co_{1.0}Ni₉ were shifted to higher temperature, which reflects that Co in the solid solution suppressed the reduction of NiO. Nevertheless, the shift of the reduction peaks on Co1.0Ba1.5Ni9 with respect to Ba1.5Ni9 was less than that due to the presence of BaCO₃. This means that the



Fig. 2. H2-TPR profiles of the catalysts.

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