



CeO₂-catalyzed direct synthesis of dialkylureas from CO₂ and amines



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ABSTRACT

CeO₂ showed higher activity for the direct synthesis of 1,3-dibutylurea (DBU) from CO₂ and *n*-butylamine than the metal oxides tested. The solvent largely influenced the reaction over CeO₂, and *N*-methylpyrrolidone (NMP) was preferable among various solvents tested from the viewpoints of activity and selectivity. The catalyst system composed of CeO₂ catalyst and NMP solvent (CeO₂ in NMP) was applicable to the reactions of various amines such as linear primary alkylamines or branched primary alkylamines, although *tert*-butylamine afforded low conversion. In contrast, secondary amines and aniline provided no yield of the ureas. The combination of 2-cyanopyridine with CeO₂ in NMP (CeO₂ in NMP with 2-cyanopyridine) promoted the transformation of the unreactive amines, showing that *tert*-butylamine and aniline were converted to the corresponding ureas in 82% and 80% yields, respectively. These yields are much higher than those reported in the previous literatures, indicating that CeO₂ in NMP with 2-cyanopyridine drastically promoted transformation of amines with low reactivity.

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1. Introduction

CO₂ is an abundant, non-toxic, non-flammable and inexpensive C1 source [1–3]. Many methods for direct conversion of CO₂ to chemicals have been developed [4–16]. Compared with reductive transformation of CO₂ to chemicals such as methanol and formic acid [4–13], non-reductive transformation to chemicals such as carbonates, carbamates and ureas [3,14–16] is preferable from the viewpoint of energy input, while the direct transformation of CO₂ is generally difficult because CO₂ is very stable due to the very strong double bonds [3]. Urea derivatives are an important class of carbonyl compounds and can be used for many applications as intermediates for the synthesis of pharmaceuticals or agrochemicals, and also used as additives for fuels [17].

Urea derivatives have been traditionally prepared with phosgene or its derivatives [17]. However, the phosgene process has considerable drawbacks such as toxicity of phosgene and co-production of large amount of salts by the neutralization. Other various methods for the synthesis of urea derivatives have been also studied, such as oxidative carbonylation of amines with CO, reductive carbonylation of amines with CO, transamidation of ureas with amines, reaction of carbonates with amines, and reaction of CO₂ and amines [17–19]. Among these methods, direct reaction of CO₂ with amine to urea derivatives will be promising

because only water is produced. Homogeneous catalysts and catalyst systems were reported such as CsOH, Cs₂CO₃, [BMIm]OH, Co(acac)₃ and TBA₂[WO₄] [20–24]. However, heterogeneous catalysts or non-catalyst systems are more desirable than homogeneous ones from the industrial, environmental, and economical viewpoints. Deng and co-workers reported that polymer supported Au nanoparticles (Au/Poly), which showed the high activity (TOF = 2900 h^{−1}) using cyclohexylamine among the reported heterogeneous catalysts, although the catalyst has drawbacks such as use of the precious metal of Au [25]. KOH/PEG catalyst and Mg–Al hydrotalcite catalyst were also reported [26,27], and these catalysts however have some problems such as low selectivity, cumbersomeness of catalyst preparation and/or narrow scope of substrate. Zhao and co-workers reported non-catalyst and non-solvent system; however, low activity and narrow scope of substrates were problems to be solved [28].

Recently, CeO₂-catalyzed organic reactions have been vigorously studied [29,30] such as transformation of nitriles [31–33], transformation of CO₂ to carbonate derivatives [34–57], reduction of alkynes and carboxylic acids [58,59], and transamidation and transesterification of amides or esters [60–69]. In our laboratory, it was firstly reported that CeO₂ showed activity for the activation of CO₂, and applied CeO₂ catalyst to transformation of CO₂ to organic carbonates such as dialkyl carbonates and cyclic carbonates, and carbamates such as methyl benzyl carbamate and cyclic carbamates [15,16,36–49]. It was also reported that CeO₂ is efficient for the direct synthesis of cyclic ureas from CO₂ and diamines [37]. In this report, CeO₂ catalyst was applied to the synthesis of

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1,3-disubstituted ureas from CO₂ and amines, and CeO₂ showed higher activity than the metal oxides tested. NMP is a preferable solvent for the reaction and enhances the activity of CeO₂.

2. Experimental

2.1. Catalysts and reagents

Preparation of pure CeO₂ catalyst was carried out by calcining cerium oxide HS (Daiichi Kigenso, Japan) for 3 h in air at 873 K, which is the optimized calcination temperature of CeO₂ according to the result of DMC synthesis for CO₂ and methanol [41]. The specific surface area (BET method) of the CeO₂ was 84 m²/g. The purity of the CeO₂ is 99.97%. All the chemicals for organic reactions were commercially available and were used without further purification. Other metal oxides were commercially available, supplied from the Catalysis Society of Japan or synthesized by the precipitation method: ZrO₂ (Daiichi Kigenso Kogyo Co., Ltd., Zr(OH)₄ was calcined under air at 873 K for 3 h), MgO (Ube Industries, Ltd., MgO 500A, 873 K, 3 h), TiO₂ (Nippon Aerosil Co., Ltd., P-25), γ-Al₂O₃ (Nippon Aerosil), ZnO (FINEX-50, Sakai Chemical Industry Co., Ltd.), and SiO₂ (Fuji Silysia Chemical Ltd., 773 K, 1 h). Y₂O₃, La₂O₃, Pr₆O₁₁ and Sm₂O₃ were prepared by the precipitation method. Y(NO₃)₃·nH₂O (Wako Pure Chemical Industries Ltd., >99.9%), La(NO₃)₃·6H₂O (Wako Pure Chemical Industries Ltd., >99.9%), Pr(NO₃)₃·nH₂O (Wako Pure Chemical Industries Ltd., >99.5%) and Sm(NO₃)₃·6H₂O (Wako Pure Chemical Industries Ltd., >99.5%) were used as precursors. A precursor (25 g) was dissolved in water (100 ml) and NH₃aq (1 M) was dropped with stirring. The pH of the solution was set to 10, resulting in a precipitate. The precipitate was filtered and washed by water, followed by drying at 383 K overnight (12 h) and calcining under air at 873 K (673 K for La₂O₃) for 3 h.

2.2. Catalytic test

All the reactions were carried out in an autoclave reactor with an inner volume of 190 ml. The standard procedure of the 1,3-

(10 ml) was added to the liquid phase as a solvent, and 1-hexanol (~0.2 ml) was also added as an internal standard substance for a quantitative analysis. The reactor was washed with methanol, and the liquids used in washing were added to the reaction mixture. The products were analyzed by a gas chromatograph equipped with an FID using a CP/Sil 5 CB capillary column (Agilent Technologies Inc., length = 50 m, I.D. = 0.25 mm, df = 0.25 μm). The following operating conditions were used: carrier gas: N₂, initial flow rate: 0.86 ml/min (pressure control mode), split ratio: 55:1, injection temperature of 573 K, column temperature program: 313 K (7 min), 20 K/min to 433 K (4 min), 20 K/min to 473 K (10 min), and 20 K/min to 573 K (26 min), detection temperature of 573 K. The qualitative analysis of the products was conducted by a gas chromatograph equipped with a quadrupole mass spectrometer (GC–MS) using the same capillary column.

Conversion and selectivity to each product in the reaction of CO₂ and amines were calculated on the basis of the amine amount as follows:

$$\text{Conversion (\%)} = \left(1 - \frac{\text{Amount of amine after the reaction}}{\text{Amount of amine before the reaction}} \right) \times 100$$

$$\text{Selectivity (\%)} = \frac{\text{Product amount based on alkyl moiety of the substrate}}{\text{Amount of reacted amine}} \times 100$$

The products that were not identified by GC–MS are denoted as “Others”. The selectivity of “Others” was calculated as follows:

$$\begin{aligned} \text{Selectivity of others (\%)} \\ = \frac{\text{Amount of reacted amine} - \text{Amount of identified products}}{\text{Amount of reacted amine}} \times 100 \end{aligned}$$

The urea formation rate per catalyst gram (V_1 , mmol h^{−1} g^{−1}) and the urea formation rate per specific surface area (V_2 , mmol h^{−1} m^{−2}) were calculated as follows:

$$\begin{aligned} V_1 \text{ (mmol h}^{-1} \text{ g}^{-1}) &= \{(\text{amount of urea, mmol}) - (\text{amount of urea at 0 h, mmol})\} / (\text{reaction time, h}) \\ &\quad - \{(\text{amount of urea without catalyst, mmol}) \\ &\quad - (\text{amount of urea at 0 h without catalyst, mmol})\} / (\text{reaction time, h}) / (\text{catalyst, g}) \end{aligned}$$

$$V_2 \text{ (mmol h}^{-1} \text{ m}^{-2}) = (V_1, \text{ mmol h}^{-1} \text{ g}^{-1}) / (\text{specific surface area, m}^2 \text{ g}^{-1})$$

dibutylurea (DBU) synthesis from CO₂ and *n*-butylamine was as follows: CeO₂ (0.34 g, 2 mmol), *n*-butylamine 1.46 g (20 mmol) and *N*-methylpyrrolidone (NMP) 8 ml (81 mmol) were put into the autoclave together with a spinner, and then the reactor was purged with 1 MPa CO₂ (Shimakyu Co., Ltd., >99.5%) three times. The autoclave was pressurized with CO₂ to the desired pressure (typically 5.0 MPa) at room temperature, and then the autoclave was heated to 433 K, where the CO₂ pressure was about 12 MPa. In the experiments for determination of the reaction rates, the autoclave with substrate, solvent and catalyst was first purged with 1 MPa Ar (Taiyo Nippon Sanso Corporation >99.9999%) three times and pressurized with Ar to 0.1 MPa. The autoclave was heated to 433 K and was pressurized with CO₂ to 5.0 MPa (CO₂ + Ar). The time when the temperature reached 433 K was set as 0 h. The mixture was constantly stirred during the reaction. After the reaction time, the reactor was cooled in water bath to room temperature. Methanol

The procedure of the reverse reaction of DBU synthesis was as follows: CeO₂ (0.34 g, 2 mmol), DBU 1.72 g (10 mmol), H₂O 0.18 g (10 mmol) and *N*-methylpyrrolidone (NMP) 8 ml (81 mmol) were put into the autoclave together with a spinner, and then the reactor was purged with 1 MPa CO₂ (Shimakyu Co., Ltd., >99.5%) three times. The autoclave was pressurized with CO₂ to 5.0 MPa at room temperature, and then the autoclave was heated to 433 K. The mixture was constantly stirred during the reaction. After the reaction time, the reactor was cooled in water bath to room temperature. The analysis of the products was conducted similar to that in the synthesis of DBU from CO₂ and *n*-butylamine.

The reusability test of CeO₂ was conducted as follows: After the reaction, the used catalyst was collected by decantation. The collected catalyst was washed with ethanol and dried at 383 K for 12 h. After the treatment, the recovered catalyst is applied to the next reaction. The catalyst was more or less lost during the

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