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Hongbing Ding, Chao Wang, Chao Chen

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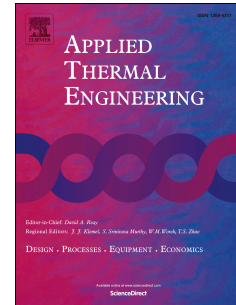
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## Non-equilibrium condensation of water vapor in sonic nozzle

Hongbing Ding, Chao Wang, Chao Chen

School of Electrical Engineering and Automation

Tianjin University, Tianjin 300072, China

Corresponding author Tel.: +86 022 27402023

wangchao@tju.edu.cn

**Abstract:** The non-equilibrium condensation phenomenon during the operation of sonic nozzle is very complicated, and will affect the flow measurement and control of sonic nozzle. Two-dimensional multi-fluid  $k-\varepsilon$  turbulence models for both homogeneous and heterogeneous nucleation of condensation were constructed to investigate the effect of vapor condensation on mass flow-rate of sonic nozzle. These models were validated by experimental data of homogeneous nucleation in the moist nitrogen flow through a convergent-divergent nozzle by Wyslouzil and the numerical solutions of heterogeneous nucleation in wet steam flow by Dykas respectively. Finally, both models above were applied to study the condensation flow in sonic nozzle. It was showed that the discharge coefficient of sonic nozzle is affected by both homogeneous and heterogeneous nucleation. When the flow is homogeneous, there is significant influence on discharge coefficient with high inlet relative humidity, which agrees with the thermal choking theory. The discharge coefficient deviation reaches 0.275% when the inlet relative humidity is 95%, which is close to the Lim's experimental data with accuracy of 0.15%. However, under low relative humidity condition, the experimental discharge coefficient deviation is larger, which is explained by the heterogeneous nucleation fortunately.

**Keywords:** vapor condensation; nucleation; transonic flow; sonic nozzles; CFD

| Nomenclature |   | $T_s$        | saturation temperature, K                      |
|--------------|---|--------------|--|
| $A$          | area, $m^2$                                       | $u$          | velocity, m/s                                  |
| $C_d$        | discharge coefficient, -                          | $w$          | mass fraction of liquid, $m_l/m$ , -           |
| $C^*$        | critical flow function, -                         | $Y$          | wetness fraction, -                            |
| $c_p$        | specific heat capacity, J/(kg·K)                  | $x_v$        | inlet mole fraction of water vapor, -          |
| $d$          | throat diameter of nozzle, mm                     | $Y_s$        | inlet mass fraction of water vapor, -          |
| $E$          | energy, J/kg                                      | <i>Greek</i> |  |
| $h_{lg}$     | latent heat of water, kJ/kg                       | $\alpha$     | heat transfer coefficient, W/( $m^2 \cdot K$ ) |
| $J$          | nucleation rate, $kg^{-1} \cdot s^{-1}$           | $\kappa$     | isentropic exponent, -                         |
| $k$          | Boltzmann's constant. $1.38 \times 10^{-23}$ J/K  | $\lambda$    | thermal conductivity, W/(m·K)                  |
| $l$          | mean free length of vapor molecule, m             | $\mu$        | viscosity, Pa·s                                |
| $M$          | Mach number, -                                    | $\rho$       | density, $kg/m^3$                              |
| $m_m$        | mass of water molecule, $2.99 \times 10^{-26}$ kg | $\sigma$     | liquid surface tension, N/m                    |
| $m_v$        | liquid mass changing rate, kg/s                   | $\tau$       | reduced temperature, $T_0/T_c$ , -             |
| $n_p$        | the droplet number density, $kg^{-1}$             | $v$          | volume of liquid molecule, $m^3$               |

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