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# From zero to hero – Production of bio-based nylon from renewable resources using engineered *Corynebacterium glutamicum*

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#### ABSTRACT

Polyamides are important industrial polymers. Currently, they are produced exclusively from petrochemical monomers. Herein, we report the production of a novel bio-nylon, PA5.10 through an integration of biological and chemical approaches. First, systems metabolic engineering of Corynebacterium glutamicum was used to create an effective microbial cell factory for the production of diaminopentane as the polymer building block. In this way, a hyper-producer, with a high diaminopentane yield of 41% in shake flask culture, was generated. Subsequent fed-batch production of C. glutamicum DAP-16 allowed a molar yield of 50%, a productivity of  $2.2 \text{ g L}^{-1} \text{ h}^{-1}$ , and a final titer of  $88 \text{ g L}^{-1}$ . The streamlined producer accumulated diaminopentane without generating any by-products. Solvent extraction from alkalized broth and two-step distillation provided highly pure diaminopentane (99.8%), which was then directly accessible for poly-condensation. Chemical polymerization with sebacic acid, a ten-carbon dicarboxylic acid derived from castor plant oil, yielded the bio-nylon, PA5.10. In pure form and reinforced with glass fibers, the novel 100% bio-polyamide achieved an excellent melting temperature and the mechanical strength of the well-established petrochemical polymers, PA6 and PA6.6. It even outperformed the oil-based products in terms of having a 6% lower density. It thus holds high promise for applications in energy-friendly transportation. The demonstration of a novel route for generation of bio-based nylon from renewable sources opens the way to production of sustainable biopolymers with enhanced material properties and represents a milestone in industrial production. © 2014 International Metabolic Engineering Society. Published by Elsevier Inc.

1. Introduction

Polyamide (PA), commonly known as nylon, is a polymer with a myriad of pharmaceutical and industrial applications. Chemically, the polymer backbone is composed of repetitive units of diamines and dicarboxylic acids that contain different numbers of carbon atoms, imparting a variety of material properties. Commercialized in the 1940s, polyamides have entered the market place on a large scale for the manufacturing of fibers for clothing or thermoplastics for carpets, cogs, car parts, tire reinforcements, and other products. Currently, the global market requires 6.6 million tons per annum, making polyamides one of the most important industrial polymers. Its good biocompatibility has further led to its implementation in medical applications, such as providing a scaffold for tissue cultures (Yoo et al., 2011), foil for orbital implants (Park et al., 2008), and bone support in arthroplasty (Edwards et al., 2011).

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Novel developments extend the application range of polyamides to diagnostics (Cox, 2001) and cellular control devices in molecular medicine (Schmitz and Schepers, 2004). Interest in a "green" route for polyamides has arisen due to the inevitable stoichiometric wastes of classical petrochemical production routes, commonly thought to cause global warming and ozone depletion, as well as acid rain and smog (Sato et al., 1998). Compared to other industrial polymers, the production of petrochemical nylon has a markedly severe impact on global climate change, expressed as carbon dioxide equivalents released (Vink et al., 2003). Moreover, it exhibits an exceptionally high requirement for fossil energy, which is particularly unfavorable in the light of the increasing shortage and rising price of fossil resources. Alternative chemical routes, such as the direct oxidation of cyclohexene to the nylon precursor adipic acid (Sato et al., 1998), promise attractive solutions for the reduction of the carbon footprint of polyamides, but these methods still rely on fossil fuels.

Without doubt, a highly promising bio-block for polyamides is 1,5-diaminopentane (cadaverine, diaminopentane), a five-carbon diamine (Qian et al., 2010). Polyamides based on diaminopentane exhibit excellent and well-known material properties (Carothers,

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| Table  | 1 |
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Lysine and diaminopentane-producing Corynebacterium glutamicum strains used and constructed in the present study.

| Strain    | Modification   | Reference     |
|-----------|--|---------------|
| LYS-12    | Wild-type ATCC 13032 + nucleotide exchange resulting in the amino acid exchange T3111 in <i>lysC</i> , encoding aspartokinase ( <i>lysC</i> <sup>T3111</sup> ); over   | Becker et al. |
|           | expression of $lysC^{T3111}$ by replacement of the native promoter with the promoter of <i>sod</i> , encoding superoxide dismutase ( $P_{sod}lysC^{T311}$ );   | (2011)        |
|           | overexpression of $dapB$ , encoding dihydropicolinate reductase, under the sod promoter ( $P_{sod}dapB$ ); duplication of $ddh$ , encoding   |               |
|           | diaminopimelate dehydrogenase (2x <i>ddh</i> ); duplication of <i>lysA</i> , encoding diaminopimelate decarboxylase (2x <i>lysA</i> ); deletion of <i>pepck</i> ,  |               |
|           | encoding PEP-carboxykinase (Δ <i>pepck</i> ); nucleotide exchange resulting in a V59A change in <i>hom</i> , encoding homoserine dehydrogenase   |               |
|           | (hom sol); overexpression of pycA, encoding pyruvate carboxylase, by replacement of the native promoter with the sod promoter  |               |
|           | $(P_{sod}pycA)$ ; nucleotide exchange resulting in the P458S change in $pycA$ $(P_{sod}pycA)$ ; replacement of the AIG start codon with the rare   |               |
|           | GIG in <i>ica</i> , encoding isocitrate denyarogenase ( <i>ica</i> <sup>**</sup> ); replacement of the natural promoter of <i>ipp</i> by the <i>tup</i> promoter, encoding   |               |
|           | erongation factor to $P_{tuf}(Dp)$ ; replacement of the natural promoter of the <i>iki-operon</i> , comprising the genes <i>zw</i> ) and <i>uu</i> , encoding the standard promoter of the <i>iki-operon</i> , comprising the genes <i>zw</i> ) and <i>uu</i> , encoding the standard promoter of the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the standard promoter of the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the standard promoter of the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the <i>iki-operon</i> , <i>comprising</i> the genes <i>zw</i> ) and <i>uu</i> , encoding the <i>iki-operon</i> , <i>comprising</i> the <i>iki-operon</i> , <i>comprinte</i> , <i>comprising</i> the <i>iki-operon</i> , <i>comprising</i> |               |
| transaido | transationase, its, encoung transiendase, $\phi(z)$ , encoung a putative sublimit of guesse behaviorable denydrogenase, and $pg$ , encoung constrained and $g(z)$ encoung transationase is a sublimit of guesse behaviorable denydrogenase, and $pg$ , encoung   |               |
| DAD 12    | $\sigma$ -phosphograconolactoniase, by replacement of the narve phonoter with the sou phonoter ( $r_{south}$ )   | This study    |
| DAP-15    | replacement of the native promoter by the <i>tuf</i> promoter ( $P_{tuf} dcC^{opt}$ ), insertion at the <i>bioD</i> locus, encoding distribution synthetase  | This study    |
| DAP-14    | DAP-13 + deletion of NCgl1469, encoding a N-acetyltransferase ( $\Delta$ NCgl1469)   | This study    |
| DAP-15    | DAP-14+deletion of <i>lysE</i> , encoding the lysine exporter ( $\Delta lysE$ )  | This study    |
| DAP-16    | DAP-15+overexpression of cg2893, encoding a major facilitator permease, by replacement of the native promoter by the sod promoter  | This study    |
|           | (P <sub>sod</sub> cg2893)  |               |

22 1938). However, due to the lack of efficient petrochemical routes 23 for production of this monomer, the corresponding polymers are 24 not considered industrially valuable. In particular, bio-based dia-25 minopentane would open up green routes to production of novel bio-nylons, such as PA5.10 and PA5.4, copolymerized with sebacic 26 27 acid from natural castor oil (Ogunniyi, 2006) and succinic acid 28 from microbial fermentation (Hong et al., 2004), respectively (Kind 29 and Wittmann, 2011). Moreover, systems metabolic engineering is 30 currently available to facilitate design and improvement of the 31 performance of microorganisms for fermentative production of an 32 increasing number of chemicals, materials, and fuels from low-cost 33 04 renewable resources (Becker and Wittmann, 2012a, 2012b; Jang et 34 al., 2012). This opens new possibilities for the creation of bio-35 based polymers at the required titers, yields, and productivities. 36 Recently, pioneering studies have enabled diaminopentane pro-37 duction from sugar in engineered cells of the soil bacterium 38 Corynebacterium glutamicum (Mimitsuka et al., 2007). These 39 synthetize the desired chemical from the natural amino acid lysine 40 through heterologous expression of the E. coli lysine decarboxylase 41 CadA (Mimitsuka et al., 2007) or LdcC (Kind et al., 2010a). Further 42 rounds of systems metabolic engineering have allowed improvement 43 of the biosynthetic capacity and supporting reactions (Kind et al., 44 2010a) and elimination of competing pathways generating undesired 45 by-products (Kind et al., 2010b), and have increased product secre-46 tion (Kind et al., 2011) and extended the substrate spectrum to starch 47 (Tateno et al., 2009) and xylose (Buschke et al., 2011). Currently, the 48 reported product yields of the best strains are still far from economic 49 applicability, but at least demonstrate promising proof-of-concepts 50 (Becker and Wittmann, 2012a, 2012b).

51 In this work, we describe a sustainable value chain, extending 52 from renewable resources to a novel, bio-based polyamide PA5.10. 53 The development integrated engineering of C. glutamicum at the 54 cellular and the process level to ensure fermentative supply of the 55 polyamide building block, diaminopentane. Thereafter, we further 56 developed processes for the fermentation and down-stream purifica-57 tion of the monomer, poly-condensation into a novel bio-nylon, and 58 further conditioning by generating enforced industrial polymers. 59

# 2. Materials and methods

# 2.1. Strains and plasmids

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The lysine producer *C. glutamicum* LYS-12 (Table 1) was used as parent strain (Becker et al., 2011). For genetic engineering work,

the *Escherichia coli* strains DH5 $\alpha$  and NM522 (Invitrogen, Karlsruhe, Germany) and the plasmids pClik int *sacB* and pTc were applied as described previously (Kind et al., 2010a).

# 2.2. Genetic engineering

All modifications were introduced into the genome of *C. glutamicum* using homologous recombination and a two-step selection, using kanamycin resistance and the *sacB* system (Becker et al., 2005; Jäger et al., 1992). Construction, purification, and analysis of plasmid DNA, as well as transformation of *E. coli* and *C. glutamicum* were performed as described previously (Becker et al., 2011; Kind et al., 2010a). Targeted gene deletion was carried out by replacement of the coding region of the gene of interest by a shortened gene fragment. For overexpression, the strong *sod* and *tuf* promoter was inserted in front of the candidate gene. The primers used for construction and verification of the introduced genetic changes have been described previously (Becker et al., 2011; Kind et al., 2010a; Kind et al., 2010b).

# 2.3. Chemicals

Tryptone, beef extract, yeast extract, brain heart infusion (BHI), and agar were obtained from Difco Laboratories (Detroit, MI, USA). All other chemicals were of analytical grade and were obtained from Sigma-Aldrich (Steinheim, Germany), Merck (Darmstadt, Germany), or Fluka (Buchs, Switzerland). Ultramid B27 and Ultramid A27 were supplied by BASF SE (Ludwigshafen, Germany).

# 2.4. Media

For shake flask studies, a complex medium was applied for the first pre-culture, whereas the second pre-culture and the main culture were carried out in glucose-based minimal medium (Kind et al., 2010a). For fed-batch production in the bioreactor, the pre-culture was grown in shake flasks in a complex medium containing 37 g L<sup>-1</sup> BHI and 20 g L<sup>-1</sup> glucose. The production process started with a batch medium that contained the following amounts of substances per liter: 90 g glucose, 15 g yeast extract, 2 g citric acid, 25 g (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, 1.25 g KH<sub>2</sub>PO<sub>4</sub>, 1.25 g Na<sub>2</sub>HPO<sub>4</sub>, 1.25 g MgSO<sub>4</sub> · 7H<sub>2</sub>O, 70 mg FeSO<sub>4</sub> · 7H<sub>2</sub>O, 30 mg ZnSO<sub>4</sub> · 7H<sub>2</sub>O, 14 mg MnSO<sub>4</sub> · 6H<sub>2</sub>O, 168 mg CaSO<sub>4</sub> · 2H<sub>2</sub>O, 0.43 mg boric acid, 0.34 mg CoSO<sub>4</sub>, 0.42 mg CuSO<sub>4</sub>, 0.07 mg Na<sub>2</sub>MoO<sub>4</sub>, 4.5 mg biotin, 7.5 mg thiamin, 9 mg nicotinamide, 30 mg pantothenic acid, 10 mg pyridoxal hydrochloride, and 1 mL antifoam (polyoxyethylene)

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