

Contents lists available at [ScienceDirect](http://www.sciencedirect.com/science/journal/22129820)

Journal of CO₂ Utilization

[T](http://crossmark.crossref.org/dialog/?doi=10.1016/j.jcou.2018.04.017&domain=pdf)

journal homepage: www.elsevier.com/locate/jcou

Swelling behavior of polyester in supercritical carbon dioxide

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1. Introduction

Industrial and academic researchers have shown convincingly that $CO₂$ can be used as a green dyeing medium instead of water in textile dyeing due to the significant economical and ecological benefits, such as nontoxicity, nonflammability, low energy consumption, no water consumption, and recyclability $[1-3]$ $[1-3]$. In supercritical state, $CO₂$ displays numerous unique properties, for example, high diffusivity and solubility, zero surface tension, and almost no risk of heat deformation with relatively low critical temperature and pressure [[4](#page--1-1),[5](#page--1-2)].

In recent years, great interest was given to the dyeing of synthetic fibers in supercritical $CO₂$ with the aim to achieve their eco-friendly production by manipulating the dyeing temperature, pressure and time [6–[8\]](#page--1-3). During supercritical dyeing process, $CO₂$ fluid near or slightly above its critical points (T_c = 31.10 °C, P_c = 7.38 MPa) produces substantial polymer swelling because of the dissolution of $CO₂$ in polymers [[9](#page--1-4)]. This provides a good possibility to control the dyeing quality of polymer since the swelling of fibers is directly connected with their dyeability. Therefore, the swelling behavior of polymers in supercritical $CO₂$ is the emphasis of current research.

To probe polymer swelling under supercritical $CO₂$ state, interferometric dissolution rate monitor was used by C. Ober, and estimated that the maximum swollen film thickness for tetrahydropyranyl methacrylate was 35 mol% at 45 °C for pressures ranging from 12.8 MPa to 19.7 MPa [[10\]](#page--1-5). K. P. Johnston measured the swelling of a 50 nm monodisperse polystyrene latex by dynamic light scattering at 25 °C at pressures up to 35 MPa, and found that the polystyrene (PS) latex swelled by up to 1.6 times as much as bulk PS at the higher pressures [[11\]](#page--1-6). T. Tassaing investigated the polymer swelling in situ at 40 °C from 2 MPa to 15 MPa by employing an FT-IR microscope, and determined the swelling of polyethylene oxide was highly dependent on the polymer crystallinity [[12\]](#page--1-7). A. Gibaud reported the swelling properties of confined poly(n-butyl methacrylate) (PBMA) films at 8 MPa and 35 °C using X-ray reflectivity technique, and found that PBMA films exhibited a greater amount of swelling than do PS films (bulk $T_g \approx 100$ °C) owing to the lower glass-transition temperature (bulk $T_g \approx 29$ °C) [[13\]](#page--1-8). It is also proved that Associated Lattice Fluid Equation of State (ALF EOS) is able to predict the extent of swelling of the polymer due to $CO₂$ using a single parameter obtained from one solubility isotherm [[14\]](#page--1-9). In addition, R. Dohrn summarized the experimental high-pressure phase-equilibrium data in the periods between 2000 and 2008, which provided essential references for the solubility (sorption) of volatile components in polymers [\[15](#page--1-10)[,16](#page--1-11)]. However, to date, swelling data of polymers at higher $CO₂$ temperatures and pressures are rather rare, although they are directly related to the fibers' dyeability in supercritical CO₂.

The current study aims to develop an in situ visible method for polyester swelling in supercritical CO₂. The effects of major process parameters including temperature, pressure, and time on the swelling of polyester were studied using the response surface methodology. A swelling model for polyester in supercritical $CO₂$ was established, and its effectiveness was validated. Furthermore, swelling mechanism of

<https://doi.org/10.1016/j.jcou.2018.04.017>

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Received 25 January 2018; Received in revised form 8 March 2018; Accepted 22 April 2018 2212-9820/ © 2018 Elsevier Ltd. All rights reserved.

Fig. 1. Schematic representation of the supercritical CO₂ apparatus used for the swelling measurement: (1) CO₂ reservoir; (2) filter; (3) heater; (4) high pressure chamber; (5) control terminal; (6) micrometering valve; (7) temperature gauge; (8) pressure gauge.

polyester in supercritical $CO₂$ was also proposed.

2. Experimental

2.1. Materials

Polyester yarns (0.47 mm) in this study were obtained from Liaoning Chaoyi Industry & Trade Group (Fuxin, China). $CO₂$ gas was purchased from China Haohua (Dalian) Research & Design Institute of Chemical Industry Co., Ltd., with a purity of 99.90%.

2.2. Swelling detection

Swelling of polyester was analyzed and detected optically inside a phase equilibria apparatus (T_{max} = 140 °C, P_{max} = 40 MPa) purchased from Waters in USA. Schematic representation of the supercritical $CO₂$ apparatus is presented in [Fig. 1.](#page-1-0) Polyester was fixed on a shelf, and loaded into a high pressure chamber. The chamber was sealed and $CO₂$ in a reservoir was discharged through a syphon, and filtered with a filter to remove the impurities. The liquid $CO₂$ was then injected into the high pressure chamber to increase system pressure. The system temperature was controlled by a heater rolled around the chamber to make CO₂ reach supercritical state. During test, the system pressure and temperature in the chamber were regulated within 0.1 MPa and 0.1 °C.

Polyester diameter change in supercritical $CO₂$ because of swelling was observed in situ through the high pressure view chamber equipped with a monochromatic light source and a CCD video camera, as displayed in [Fig. 2.](#page-1-1) A halogen lamp connected with an optical fiber was located in a sapphire window to illuminate the interior of the chamber. Digital pictures of the polyester yarns under different supercritical CO_2 conditions were recorded using the CCD video camera in order to calculate the swelling data.

2.3. Experimental design and analysis

A class of the Response surface methodology (RSM) called Box-Behnken design was employed for investigating the supercritical $CO₂$ experiments to ascertain the effect of the three independent parameters including system temperature, system pressure and treatment time on the swelling of polyester. The optimum ranges of system temperature (100–140 °C), system pressure (22–26 MPa) and time (30–60 min) were determined according to our preliminary experiments $[7]$. A $3³$ full factorial design is generated as shown in [Table 1.](#page-1-2) To express the swelling data as a function of the independent variables, a second-order polynomial equation (Eq. (1) (1)) was used as follows $[17]$ $[17]$:

Fig. 2. Schematic representation of the high pressure chamber in supercritical $CO₂$ apparatus: (1) CCD camera; (2) light source; (3) visible window; (4) magnetic stirrer; (5) gas pipeline.

$$
Y = \beta_0 + \sum_{i=1}^n \beta_i x_i + \sum_{i=1}^n \beta_{ii} x_i^2 + \sum_{i=1}^n \sum_{j=2}^n \beta_{ij} x_i x_j + \varepsilon
$$
\n(1)

where x_i , x_i are the independent variables; Y is the predicted response value; $β_0$, $β_i$, $β_{ii}$, $β_{ij}$ are the regression coefficients for intercept, linear, quadratic and interaction effect, respectively; ε is the random error, and n is the number of variables.

The three independent experimental parameters were assigned as X_1 (temperature, $°C$), X_2 (pressure, MPa) and X_3 (time, min). The variables and levels in the $3³$ design were listed in [Table 1](#page-1-2). A second-order polynomial model containing these three independent variables was established as follows (Eq. [\(2\)](#page-1-3)):

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