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Enhanced natural convection heat transfer of nanofluids in enclosures with two adjacent walls heated and the two opposite walls cooled



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ABSTRACT

A two-phase mixture model is used to carry out a numerical study of buoyancy-driven convection in nanofluid-filled square enclosures heated laterally and underneath. The thermal performance of water-based nanofluids with suspended metal oxide nanoparticles having temperature-dependent properties is investigated in the hypothesis that Brownian diffusion and thermophoresis are the primary slip mechanisms between solid and liquid phases. The thermophoretic diffusion effects are taken into account through a correlation developed on the basis of wide sets of experimental heat transfer data available in the literature for different nanofluids. The idea upon which the present work is based originates from the main result of all the experimental studies conducted on natural convection of nanofluids in differentially-heated enclosures, whose common conclusion is that the addition of nanoparticles to a base liquid is substantially detrimental, due to the formation of two stagnant fluid layers near the top and bottom adiabatic walls. Therefore, if the horizontal walls are differentially heated instead of being perfectly insulated, the lack of stratification at the top and bottom of the enclosure, consequent to the development of two horizontal concentration boundary layers, may result in a heat transfer enhancement. A computational code based on the SIMPLE-C algorithm is used to solve the system of the mass, momentum and energy transfer governing equations. Numerical simulations are executed for three different nanofluids, using the diameter of the suspended nanoparticles and their average volume fraction, as well as the cavity width and the temperatures imposed at the walls, as independent variables. It is found that, due to the effects of the slip motion occurring between solid and liquid phases, the rate of heat transferred across the enclosure by the nanofluid is periodic and remarkably higher than that transferred by the pure base liquid. Furthermore, the heat transfer performance of the nanofluid relative to that of the pure base liquid increases with increasing the nanoparticle concentration up to an optimal particle loading at which the heat transfer rate has a smooth peak. The relative heat transfer enhancement is discovered to increase with increasing the nanofluid average temperature and the cavity width, and decreasing the nanoparticle size.

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1. Introduction

Natural convection of nanofluids in enclosures has been abundantly investigated in the last decade, both experimentally and, above all, numerically.

The main finding of the experimental works is that the addition of nanoparticles to a base liquid is substantially detrimental, which is the case of the studies performed by Putra et al. [1], Wen and Ding [2,3], Nnanna [4], Chang et al. [5], Ho et al. [6], Hu et al. [7], and Hu et al. [8], using cavities differentially heated at sides.

* Corresponding author. *E-mail address:* massimo.corcione@uniroma1.it (M. Corcione). For vertical enclosures, an interpretation of the cited heat transfer degradation was recently proposed by Aminfar and Haghgoo [9]. They found that, besides the development of two thin concentration boundary layers adjacent to the heated and cooled sides, the slip motion occurring between solid and liquid phases gives rise to the formation of two stagnant fluid layers near the top and bottom adiabatic walls, whose pronounced thickness results in a significant limitation of the heat transfer rate across the enclosure. Noticeably, the occurrence of such a marked stagnation at the top and bottom of the cavity was never pointed out before. In fact, most previous numerical works performed on this topic were based on the single-phase approach. On the other hand, the few studies based on the two-phase model typically relied on the use of the McNab-Meisen relation [10] for the calculation of the

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С	specific heat at constant pressure, J/(kg K)	x	horizontal Cartesian coordinate, m	
D_B	Brownian diffusion coefficient, m ² /s	у	vertical Cartesian coordinate, m	
D_T	thermophoretic diffusion coefficient, m ² /s			
d_p	nanoparticle diameter, m	Greek symbols		
g	gravity vector, m/s ²	${arphi}$	nanoparticle volume fraction	
Ī	unit tensor	μ	dynamic viscosity, kg/(m s)	
\mathbf{J}_{p}	nanoparticle diffusion mass flux, kg/(m ² s)	θ	period of oscillation, s	
k	thermal conductivity, W/(m K)	ho	mass density, kg/m ³	
k_B	Boltzmann constant = $1.38066 \times 10^{-23} \text{ J K}^{-1}$	τ	stress tensor, kg/(m s ²)	
Le	Lewis number			
т	nanoparticle mass fraction	Subscrij	Subscripts	
Nu	Nusselt number	av	average	
р	pressure, Pa	b	bottom wall, at the temperature of the bottom wall	
Pr	Prandtl number	С	cooled wall, at the temperature of the cooled wall	
Q	heat transfer rate, W	f	base fluid	
q	heat flux, W/m ²	h	heated wall, at the temperature of the heated wall	
Ra	Rayleigh number	in	incoming	
S_T	thermophoresis parameter	max	maximum value	
Sh	Sherwood number	min	minimum value	
Т	temperature, K	п	nanofluid	
t	time, s	opt	optimal value	
U	horizontal velocity component, m/s	out	outgoing	
V	velocity vector, m/s	S	solutal	
V	vertical velocity component, m/s	S	solid phase	
\mathbf{V}_T	thermophoretic velocity vector, m/s	Т	thermal	
W	width of the enclosure, m	t	top wall, at the temperature of the top wall	

thermophoretic velocity of the suspended nanoparticles, which implied an underestimation of the thermophoretic diffusion coefficient, as debated by Giddings et al. [11]. These are the main reasons why many authors, against any experimental evidence, concluded that the dispersion of nanoparticles into a base liquid produces almost always a heat transfer increase rather than a diminution - see, e.g., the compilation of selected papers collected by Corcione et al. [12]. Conversely, with the scope to overcome the disagreement between numerical results and experimental data, Aminfar and Haghgoo [9] adapted the value of the thermophoretic diffusion coefficient so as to fit a set of heat transfer measurements executed by Ho et al. [6] using a square cavity of side length 25 mm containing water suspensions of alumina nanoparticles with an average diameter of 33 nm and an average volume fraction of 0.01 and 0.03, which allowed them to properly account for the effects of the slip motion occurring between solid and liquid phases, and discover the mentioned stagnation occurrence.

Nomenclature

According to what has been discussed earlier, we can assert that if the horizontal walls of the enclosure are differentially heated instead of being insulated, the lack of stratification at the top and bottom of the enclosure, consequent to the development of two horizontal concentration boundary layers, may result in an increase rather than a decrease in the heat transfer performance associated with the dispersion of a given concentration of solid nanoparticles into the base liquid.

Framed in this background, a numerical study on natural convection of nanofluids in square enclosures differentially heated at sides, and simultaneously heated at the bottom wall and cooled at the top wall, is carried out using a two-phase model based on the double-diffusive approach, in the hypothesis of temperature-dependent physical properties, assuming that Brownian diffusion and thermophoresis are the primary slip mechanisms between suspended nanoparticles and base liquid. In particular, the effects of the thermophoretic diffusion are taken into account through a specifically-developed correlation based on

wide sets of experimental heat transfer data available in the literature for different nanofluids. Primary scope of the paper is to determine in what measure the thermal activity of the four boundary walls of the cavity results in an enhanced heat transfer rate when a nanofluid is used instead of the corresponding base liquid, and to discuss the main heat and momentum transfer features. Further aim of the present investigation is to evaluate the effects of the nature, size and average volume fraction of the suspended nanoparticles, as well as the effects of the cavity width and the temperatures imposed at the walls, on the nanofluid heat transfer performance relative to that of the pure base fluid.

2. Mathematical formulation

A square cavity of width W, filled with a water-based nanofluid containing metal oxide nanoparticles, is considered. The reference Cartesian coordinate system is defined so that the x axis is horizontal, while the y axis is vertical and pointing upwards in the direction opposite to gravity. The cavity is heated at one side, kept at a uniform temperature T_h , and cooled at the opposite side, kept at a uniform temperature T_c . As far as the horizontal boundary walls are concerned, the following couple of thermal configurations are considered: (a) both the bottom and top walls are adiabatic, denoted as configuration AA; and (b) the bottom wall is heated at temperature T_h and the top wall is cooled at temperature T_{c} , denoted as configuration HC. A sketch of the cavity is depicted in Fig. 1, where the coordinate system and the thermal states of the four boundary walls are also displayed. The buoyancy-induced flow is considered to be two-dimensional, laminar and incompressible, with negligible viscous dissipation and pressure work. It is assumed that the suspended nanoparticles and the base liquid are in local thermal equilibrium, and that Brownian diffusion and thermophoresis are the only slip mechanisms by which the nanoparticles can develop a significant relative Download English Version:

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