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#### Review

# Review of flow boiling and critical heat flux in microgravity



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#### ABSTRACT

Space agencies worldwide are actively exploring the implementation of two-phase thermal management systems to support astronaut life onboard future space vehicles and planetary bases. Key motivations for these efforts are to increase the efficiency of power utilization and reduce overall weight and volume. These advantages are realized by orders of magnitude enhancement in heat transfer coefficient achieved with flow boiling and condensation compared to single-phase systems. This study will review published literature concerning two-phase flow and heat transfer in reduced gravity. Discussed are the different methods and platforms dedicated to exploring the influence of reduced gravity, including ground flow boiling experiments performed at different orientations relative to Earth gravity, as well as reduced gravity adiabatic two-phase flow, pool boiling, flow boiling and CHF experiments. Despite the extensive data and flow visualization results available in the literature, it is shown that there is a severe shortage of useful correlations, mechanistic models and computational models, which compromises readiness to adopt flow boiling in future space systems. Key recommendations are provided concerning platform, heater design, and operating conditions for future studies to expedite the deployment of two-phase thermal management in future space missions.

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Nomenclature							
Α	cross-sectional area of flow channel	$U_{\infty}$	bubble rise velocity				
b	ratio of wetting front length to wavelength	W	heated width of channel's cross-section				
Во	Bond number	We	Weber number				
$C_{f,i}$	interfacial friction coefficient	$\chi_e$	thermodynamic equilibrium quality				
$C_o$	distribution parameter in Drift Flux model	Z	stream-wise coordinate				
$c_p$	specific heat at constant pressure	$z_0$	distance from leading edge of heated wall to location				
D D	diameter	~0	where vapor velocity surpasses liquid velocity				
$D_h$	hydraulic diameter, 4A/P		miere raper researcy surpasses inquita researcy				
f"	friction factor	Greek sy	mhole				
Fr	Froude number	α	vapor void fraction				
G	mass velocity	$\delta$	mean thickness of vapor layer				
g	gravity	$\delta_{ m h}$	heated wall thickness				
$g_e$	Earth gravity	$\eta$	interfacial perturbation				
$g_n$	component of gravity normal to heated wall	$\eta_o$	amplitude of interfacial perturbation				
$g_{  }$	component of gravity opposite to direction of fluid flow	ηο λ	wavelength				
H	height of channel's cross-section	$\lambda_c$	critical wavelength				
h	heat transfer coefficient	$\mu$	dynamic viscosity				
$H_f$	mean thickness of liquid layer	v	kinematic viscosity				
$h_{fg}^{'}$	latent heat of vaporization	П	dimensionless group				
$H_g$	mean thickness of vapor layer	$\rho$	density				
j ຶ	superficial velocity	$\rho''$	modified density				
k	thermal conductivity; wave number $(2\pi/\lambda)$	$\sigma$	surface tension				
L	heated length	τ	shear stress				
ṁ	mass flow rate	$\theta$	flow orientation angle				
Nu	Nusselt number	Ü	now orientation ungre				
P	perimeter	Subscrin	Subscripts				
p	pressure	asymp	asymptotic				
Pr	Prandtl number	b	bulk liquid				
Q	volumetric flow rate	f	saturated liquid				
q''	wall heat flux	-	saturated riquid				
$q_m''$	critical heat flux (CHF)	g h	heated wall				
$q_w''$	wetting front lift-off heat flux	i	interface				
Re	Reynolds number	in	inlet to heated wall				
T	temperature	m	critical heat flux				
$\Delta T_{sub,o}$	outlet subcooling, $T_{sat,o} - T_{b,o}$	min	minimum				
U	mean liquid inlet velocity	max	maximum				
$U_f$	mean velocity of liquid layer	0	outlet from heated wall				
$\dot{U_g}$	mean velocity of vapor layer	sat	saturation				
$U_{g,n}$	mean vapor velocity in wetting front normal to heated	sub	subcooling				
	wall	W	wetting front; heated wall				

#### 1. Introduction

# 1.1. Importance of two-phase thermal management to future space missions

Many modern applications requiring the dissipation of large concentrated heat loads rely on two-phase thermal management systems that employ both flow boiling and condensation. Unlike single-phase systems, which rely entirely on sensible heat rise of the working fluid to remove the heat, two-phase systems capitalize upon latent heat in addition to the sensible heat, which allows them to achieve orders of magnitude enhancement in heat transfer

coefficient and much lower temperatures of the heat dissipating device compared to single-phase counterparts [1]. Associated with heat-flux controlled flow boiling, critical heat flux (CHF) is arguably the most important design parameter for two-phase thermal management systems. Since exceeding this limit can lead to catastrophic failure, a key goal in designing a two-phase thermal management system is to increase CHF in order to broaden the useful nucleate boiling heat flux range. This important goal has spurred many recent research efforts to both increase and predict CHF using a variety of boiling configurations, including pool [2,3], channel flow [4,5], mini/micro-channel [6], spray [7,8], and jet [9–11], as well as hybrid cooling configurations [12,13].

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