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# Advanced Powder Technology

journal homepage: [www.elsevier.com/locate/apt](http://www.elsevier.com/locate/apt)



Original Research Paper

## Utilization of incineration fly ash from biomass power plants for zeolite synthesis from coal fly ash by microwave hydrothermal treatment

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### ARTICLE INFO

#### Article history:

Received 1 July 2017

Received in revised form 20 October 2017

Accepted 23 October 2017

Available online xxxxx

#### Keywords:

Biomass incineration ash

Zeolite

Microwave hydrothermal treatment

### ABSTRACT

Potassium-type zeolite (K-zeolite) was synthesized from coal fly ash and woody biomass incineration ash by microwave hydrothermal treatment. The woody biomass incineration ash was discharged from a biomass power plant, and extracted solutions of the material had a pH range of 11.5–13.0 and a high potassium concentration; therefore, it could be employed to replace the KOH solution that is typically used in the synthesis of K-zeolites. Consequently, we successfully synthesized a K-zeolite containing phillipsite phases from coal fly ash using extracted solutions obtained from biomass incineration fly ash. The ammonium adsorption capacity of the K-zeolite synthesized by microwave hydrothermal treatment was comparable to that of K-zeolite synthesized by oil-bath hydrothermal treatment (external heating). We also confirmed that the microwave heating method could shorten the K-zeolite synthesis time compared to that required when using oil-bath heating.

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### 1. Introduction

The use of renewable energy sources for the generation of electric power in Japan is being promoted by the Feed-in Tariff Scheme for Renewable Energy, which was established in 2012 [1–3]. Using woody biomass for electricity generation can give a stable supply of electricity that is not influenced by the weather while also contributing to the suppression of carbon dioxide emissions and the conservation of forests. Therefore, the idea of a boiler power plant using woody biomass as a fuel has been attracted attention in recent years [4]. In Japan, the ash generated during biomass incineration is discharged from power plants and transferred to a final disposal site as industrial waste without any further use [5]. Since the costs of conveying and landfilling is particularly high (about 20,000 JPY/t), this appears to be sufficient to inhibit the spread of boiler power plants using woody biomass as a fuel, and so the development of a suitable scheme for the utilization of biomass incineration ash is necessary [6].

It has been reported that the incineration ash discharged after the combustion of biomass could be utilized for a variety of pur-

poses, for example as a soil improving agent [7,8], a fertilizer [9,10], or an adsorbent material [11]. One potential way of utilizing biomass incineration ash is in the preparation of potassium-type zeolites (K-zeolites) from coal fly ash using extracted solutions of the biomass incineration ash, which exhibit pH values ranging from 11.5 to 13.0 and contain high concentrations of potassium [12,13]. Although a number of studies have reported zeolite formation from coal fly ash using hydrothermal treatment methods [14–21], a potential problem with these systems is that they require a large quantity of highly concentrated alkaline agent for the dissolution of the ions necessary for zeolite synthesis. Thus, aqueous solutions extracted from biomass incineration ash could potentially be employed as alkali sources to reduce the quantity of alkaline agent required. We have previously reported the synthesis of K-zeolites from coal fly ash via an external heating method using woody biomass incineration ash as an alkali source [22]. The zeolites were successfully prepared at a KOH concentration that was much lower than the concentration required to synthesize K-zeolite using a KOH solution alone as the alkaline source. However, long thermal treatment times were necessary to synthesize the zeolite. Therefore, shortening the thermal treatment time is necessary for practical use.

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85 Microwaves are capable of heating matter rapidly, directly, and  
86 selectively. They generate heat by rotating the dipole of an object.  
87 In our previous studies, we have investigated the effect of micro-  
88 wave irradiation on zeolite synthesis from coal fly ash using pure  
89 chemicals as alkali agents, and have reported that microwave heat-  
90 ing reduced the treatment time necessary for the reaction to go to  
91 completion [23–25].

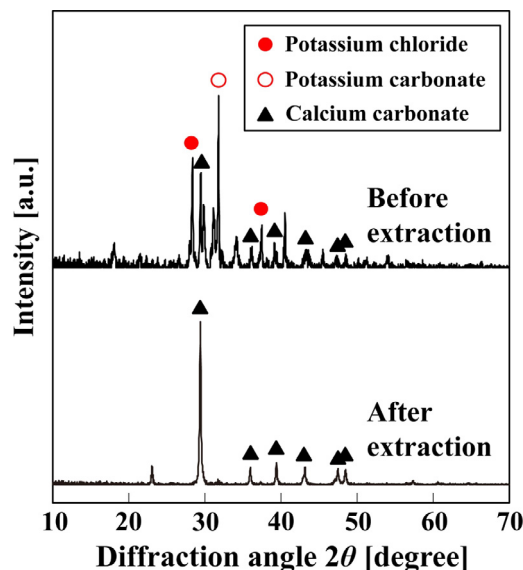
92 In this study, we investigated the effect of microwave heating  
93 on the rate of zeolite synthesis from coal fly ash in an extracted  
94 solution of biomass incineration ash. Furthermore, the zeolite crys-  
95 tal synthesis rates achieved using the microwave and external  
96 heating methods were compared based on the investigation and  
97 an empirical equation.

98 **2. Experimental methods**

99 **Table 1** lists the properties of the coal fly ash and biomass incin-  
100 eration ash employed herein. Coal fly ash (JIS Z8910, No. 10) with a  
101 median diameter of 3.4  $\mu\text{m}$  was used for preparation of the zeolite  
102 framework as a source of Si and Al. Biomass incineration ash,  
103 which had a potassium concentration of 57.6 mass%, was also used.  
104 The ash was collected from the bag filter dust collector following  
105 combustion of dry sawdust, bark, and wood chips of Japanese cedar  
106 using a fluidized bed furnace in the Chugoku Mokuzai woody bio-  
107 mass power plant in Hiroshima, Japan. The X-ray diffraction (XRD)  
108 patterns of the biomass incineration ash before and after extraction  
109 with deionized water are shown in **Fig. 1**. The crystalline phases of  
110 the biomass incineration ash were KCl and  $\text{K}_2\text{CO}_3$ , both of which  
111 are readily soluble in water. The residue contained almost no  
112 potassium, rendering it suitable for use as a raw material for  
113 cement (N.B., potassium degrades the quality of cement). In addi-  
114 tion, the mass of the biomass incineration ash decreased by  
115 ~40% following the extraction process. Therefore, our reported  
116 method of using biomass incineration ash helped to both reduce  
117 the mass of biomass incineration ash and produce useful byprod-  
118 ucts while reducing the quantities of waste materials produced.  
119 Prior to zeolite synthesis, the coal fly ash and biomass incineration  
120 ash (before extraction) were dried at 100  $^\circ\text{C}$  for 24 h.

121 To confirm the effectiveness of using biomass incineration ash  
122 as an alternative to KOH, the following starting suspensions for  
123 hydrothermal treatment were prepared:

- 124 (i). Initial suspension using only KOH as a source of alkali and  
125 potassium (conventional suspension): an aqueous solution  
126 of potassium hydroxide (1.5 mol/L) was prepared by dissolv-  
127 ing KOH (4.21 g, 86.0%, Kanto Chemical Co., Inc., Japan) in  
128 deionized water (50.0 mL, SWG203, SANSYO, Japan). Coal  
129 fly ash (10.0 g) was dispersed in this KOH solution and used  
130 as the starting suspension.
- 131 (ii). Initial suspension using the extracted solution obtained  
132 from the biomass incineration ash as a source of alkali and  
133 potassium: biomass incineration ash (3.0–15.0 g) was dis-  
134 persed in deionized water (50 mL), and the resulting mixture  
135 was stirred for 10 min. A solution containing alkali and



**Fig. 1.** XRD patterns of biomass incineration ash before and after extraction.

136 potassium was obtained by filtration. **Table 2** shows the  
137 potassium ion concentration and pH of the obtained solu-  
138 tion. The potassium ion concentration and pH increased  
139 upon increasing the mass of biomass incineration ash. In  
140 our previous work, we have found that pH of more than  
141 13.5 is necessary for stable zeolite synthesis. Therefore, to  
142 adjust the pH of this solution to be more than 13.5, KOH  
143 (0.842 g, final concentration 0.3 mol/L) was dissolved in  
144 the extracted solution. Finally, coal fly ash (10.0 g) was  
145 added as a source of Si and Al.

146  
147 A schematic diagram of the microwave heating equipment is  
148 shown in **Fig. 2a**. Microwaves (2.45 GHz) generated by a mag-  
149 netron reach the vessel via a waveguide. The prepared starting sus-  
150 pension was irradiated and heated by the microwaves. The  
151 temperature of the suspension was held at 413 K, and was con-  
152 trolled by varying the output of the microwaves with a propor-  
153 tional-integral-derivative (PID) controller. The thermal treatment  
154 time was 2–32 h. The treatment pressure was maintained at atmo-  
155 spheric pressure ( $1.013 \times 10^5$  Pa), and the rotational speed of the  
156 stirrer was set to 100 rpm. After the hydrothermal treatment, the  
157 desired product was isolated by filtration (Büchner funnel), and  
158 washed with deionized water thoroughly prior to drying at 373 K  
159 for 24 h to give the powdered product.

160 As a control experiment, the prepared starting suspension was  
161 treated hydrothermally under the same conditions using a conven-  
162 tional electric heater, shown in **Fig. 2b**. The prepared starting sus-  
163 pensions were then loaded into a 100 mL Teflon reaction vessel,  
164 and the suspensions were heated in an oil bath (OHB-1000G,

**Table 1**  
Properties of coal fly ash and biomass incineration ash.

	Coal fly ash		Biomass incineration ash	
Component [mass%]	$\text{SiO}_2$	52.1	$\text{SiO}_2$	1.8
	$\text{Al}_2\text{O}_3$	22.3	$\text{Al}_2\text{O}_3$	1.5
	CaO	2.3	CaO	32.4
	$\text{K}_2\text{O}$	<1	$\text{K}_2\text{O}$	57.6
	$\text{Fe}_2\text{O}_3$	5.2	$\text{Fe}_2\text{O}_3$	<1
	Others	18.1	Others	6.7
Median diameter [ $\mu\text{m}$ ]	3.36		4.40	

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