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# <sup>2</sup> Original Research Paper

# Increasing the amorphous yield of  ${({Fe_{0.6}Co_{0.4}})_{0.75}B_{0.2}Si_{0.05}}$  $96Nb_4$  $\frac{1}{5}$  powders by hot gas atomization

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- 28

#### **ABSTRACT**

The synthesis of metallic glasses requires high cooling rates leading to product size limitations of a few 30 millimeters when using conventional casting techniques. One way to overcome these size limitations is 31 powder metallurgy. Melt atomization and the subsequent powder processing can result in larger, amor- 32 phous components as long as no crystallization takes place during powder consolidation. 33

An iron-based glass-forming alloy  ${({[Fe_{0.6}Co_{0.4}]_{0.75}B_{0.2}Si_{0.05}]_{96}}Nb_4}$  was formed through both ambient 34<br>oom and high temperature inert gas atomization at various melt flow rates (close-coupled atomization). 35 room and high temperature inert gas atomization at various melt flow rates (close-coupled atomization). The use of hot gas generally decreases the droplet size and hence leads to an increased cooling rate and 36<br>37<br>37 amorphous fraction of the atomized powders.

Hot gas atomization results in a lower gas consumption, a smaller gas-to-melt mass flow ratio (GMR), 38 smaller particles and a smaller geometric standard deviation. 39

Particles atomized in ambient temperature were fully amorphous up to a particle size fraction of 90 40 µm. Larger particle size fractions resulted in a higher crystalline fraction. According to the XRD and 41 DSC analyses, hot gas atomization has only a very small influence on the cooling rate and the amorphous 42 fraction. However, the amorphous yield is significantly increased using hot gas atomization. 43

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#### 48

# 49 1. Introduction

 Metallic glasses exhibit excellent physical and chemical proper- ties such as soft magnetic properties, good catalytic performance, 52 high strength and good corrosion resistance  $[1,2]$ . However, the properties of these amorphous materials can only be obtained when the melt is rapidly cooled. Ongoing efforts to modify glass- forming alloys and the use of rapid solidification techniques such as water quenching and copper mold casting has led to the synthe- sis of bulk metallic glasses. These methods provide the required cooling rates to avoid crystallization, but the relatively low heat conduction of these alloys generally results in dimensional restric- tions. This limits the critical casting thickness ranges from microm-61 eters to a few centimeters  $[3,4]$ . A further challenge is the required high purity of the feedstock material that can also limit the com-mercialization of metallic glasses at a large scale.

64 The combined use of melt atomization and a subsequent pow-65 der metallurgy process is an alternative way to overcome size limitations. Gas atomization is a suitable process for the generation 66 of amorphous powders  $[5,6]$ , as it provides an appropriate range of 67 cooling rates  $(10^3 - 10^5 \text{ K s}^{-1})$ . 68

Today, there is a strong tendency to process metallic glasses for 69 use in structural components. Different manufacturing techniques 70 such as selective laser melting [\[7\],](#page--1-0) warm hydrostatic extrusion  $[8]$ , 71 warm rolling [\[9\]](#page--1-0), spark plasma sintering [\[10,11\],](#page--1-0) severe plastic 72 deformation  $[12]$ , cold spraying  $[13,14]$ , and thermoplastic forming 73 [\[15–17\]](#page--1-0) have been used. These techniques require primarily amor- 74 phous powder as a base material. Consequently, generating metal- 75 lic glasses as glassy powders is essential for these technologies as it 76 avoids dimensional restrictions as long as no crystallization takes 77 place during subsequent powder processing. The matrix of  $\frac{1}{2}$  and  $\frac{1}{2}$  a

The final properties of the consolidated material are influenced 79 by particle size, particle shape, impurities, oxygen level and amor-<br>80 phous fraction. These properties are interconnected as the amor- 81 phous fraction also depends on the cooling rate and the cooling 82 rate, in turn, depends on the particle size. For instance, an 83 increased droplet size generally results in lower cooling rates as 84 the specific surface of the melt droplets decreases  $[5]$ . The design 85

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86 of appropriate cooling strategies is therefore required to achieve an 87 amorphous fraction of 100%.

 One of the most attractive possibilities to alter the cooling rate is the use of hot gas to generate smaller particles [\[18,19\]](#page--1-0). Hot gas atomization can yield smaller particles as the gas velocity increases. The cooling rate, the amorphous fraction, and the amor- phous yield hence increase due to the synthesis of smaller parti-cles. An additional benefit is a reduction of gas consumption.

94 The applicability of hot gas atomization poses the question: 95 does hot gas atomization decrease the cooling rate and the amor-96 phous fraction even though smaller particles are being generated?

## 97 2. Experimental procedure

### 98 2.1. Sample synthesis

99 The iron-based glass-forming alloy  ${[Fe_{0.6}Co_{0.4}]_{0.75}B_{0.2}Si_{0.05}]_{96}$  Nb4 (at.%) was chosen due to its economical relevance that results from its unique mechanical properties, high availability, and rela- tively moderate feedstock costs. Iron-boron (81.43 wt% of Fe and 17.94 wt% of B), FeNb (31.40 wt% of Fe and 65.20 wt% of Nb), pure Fe (99.99 wt%), Co (99.0 wt%) and Si (99.9 wt%) were melted in an Al<sub>2</sub>O<sub>3</sub> crucible under an argon atmosphere. The total weight of the feedstock material was 2000 g. The melt temperature of 1833 K was constant for 20 min before atomization started.

#### 108 2.2. Atomization

 The schematic layout of the gas-atomization facility is shown in Fig. 1a. The system consists of three main components: a vacuum vessel including the inductive melting system, a spray chamber with a total height of 4.80 m and the nozzle system (close-coupled atomization) as seen in Fig. 1b.

114 An Al<sub>2</sub>O<sub>3</sub> crucible with a capacity of 1000 ml was placed into the vessel. Twenty minutes after the atomization temperature (1833 K) was kept constant, a stopper rod was pulled to start the atomization process (the feedstock material was melted 350 K above the liquidus temperature). Three different nozzle outlet diameters were used (1.5 mm; 2 mm; 3 mm) leading to different melt mass flow

rates ranging from 81 to 313 kg  $h^{-1}$ . The gas temperature was 120 heated with a heat exchanger to temperatures in the range of 121 293–600 K. 122

A novel convergent-divergent close-coupled atomizer with an 123 annular slit of 0.8 mm (CD-CCA-0.8) was used  $[20]$ . The new nozzle 124 configuration design allows the stable atomization at low pres- 125 sures of 0.8 MPa as well as higher gas pressures. 126

The high velocity gas stream impinged on the melt stream 127 which resulted in the disintegration of the melt into droplets. 128 The droplets then solidify in the presence of an inert gas during 129 their flight inside the spray chamber. Liquid Ar  $\geq$  99.996 with an 130 oxygen impurity  $O_2$  < 4 ppm was used. The powder vield was oxygen impurity  $O_2 \leq 4$  ppm was used. The powder yield was 131<br>above 95% (the remaining five percent corresponded to residues 132 above 95% (the remaining five percent corresponded to residues of the melt in the crucible and flakes or fibres due to the collision 133 of semi-solidified droplets with the chamber wall – flakes and 134 fibres were subsequently removed during sieving). 135

[Table 1](#page--1-0) summarizes parameters and characteristics of the 136 atomization process including the gas-to-melt-mass flow ratio 137 (GMR), mass median particle diameter  $d_{50,3}$ , and geometric stan- 138 dard deviation  $\sigma$ . The geometric standard deviation was calculated 139<br>from the cumulative mass distribution according to 140 from the cumulative mass distribution according to 140  $\sigma = (d_{84,3}/d_{16,3})^{1/2}$ .

A reference powder was synthesized with the Nanoval process 142 [\[21,22\]](#page--1-0) in order to calculate the amorphous fraction from differen-<br>143 tial scanning calorimetry (DSC) measurements. The feedstock was 144 melted in an argon atmosphere and subsequently atomized in a 145 nitrogen atmosphere at 1770 K (oxygen content < 200 ppm). The 146 GMR was 3.0 (nitrogen (kg)/melt (kg)). The obtained reference 147 powder had a particle mass median diameter of  $d_{50,3} = 23.2 \text{ }\mu \text{m}$  148 and a geometric standard deviation of 2.0. The manufacture of  $149$ 

# 2.3. Analyses 150

A laser diffraction instrument (Malvern Mastersizer 2000) with 151 a wet dispersion unit was used to measure the mass median parti-<br>152 cle diameter d<sub>50,3</sub> and the geometric standard deviation  $\sigma$  (nine 153 measurements were conducted and averaged). 154

XRD measurements were performed with a Bruker D8 equipped 155 with a CuK $\alpha$  source. The powder samples were run from 10 – 80 $^{\circ}$  156



Fig. 1. Schematic illustration of the gas-atomization set-up (a) including the close-coupled atomizer (b).

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