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Original Research Paper

Co-Al spinel-based nanoparticles synthesized by flame spray pyrolysis for glycerol conversion

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ABSTRACT

The catalytic properties of Co-Al spinel nanoparticles prepared by liquid-feed flame spray pyrolysis (L-F FSP) were investigated in the glycerol conversion in gas phase in an atmosphere of hydrogen. Reduction at 1123 K of the as-synthesized spinel nanoparticles induced the formation a new phase containing metallic cobalt species. Although, the reducibility of cobalt oxides is greatly decreased due to interaction with aluminium species, this strong interaction may prevent the aggregation of Co particles under the harsh reduction conditions. X-ray photoelectron spectroscopy (XPS) of the reduced spinel nanoparticles at 1123 K revealed that the Co/Al atomic ratio has decreased to Co/Al = 0.11, which may indicate a redistribution of the aluminum and cobalt species at the surface of the sample submitted to the reduction in a flow of hydrogen at 1123 K. X-ray diffraction (XRD) and high resolution electron microscopy (HRTEM) also reinforced the formation of metallic cobalt species after reduction of cobalt from the spinel nanoparticles at 1123 K. The main products obtained from the conversion of glycerol in the gas phase were hydroxyacetone, pyruvaldehyde, lactic acid and lactide. FSP successfully gave insights to ensure uniform dispersion of the active metal on a support material.

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53 1. Introduction

Glycerol is an extremely versatile building block within biore-54 fineries as it offers many opportunities for production of useful 55 chemicals. Nearly two-thirds of the world's glycerol production 56 comes as by-product from biodiesel. Furthermore, biodiesel pro-57 duction increased rapidly from 1 million tons in 2000 to 25 million 58 tons in 2015 [1–3]. Thus, the availability of glycerol is expected to 59 60 increase as the demand for biodiesel continues to rise globally. Hence, the transformation of glycerol into valued-added products 61 and commodity chemicals has been intensively studied over the 62 last decade [2]. 63

The transformation of glycerol by catalytic conversion is often 64 65 carried out using noble metal-based catalysts for hydrogen activation. Conversely, transition metal-based materials are alternative 66

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catalysts for glycerol transformation [5-7]. Despite their lower activity for hydrogenation compared to noble metals they present other advantages, such as much lower prices and higher resistance to poisoning [8].

In addition to the kind of metal for the catalyst other features must be considered when selecting a material namely, the size of the metal particle, the type and morphology of the support, and the homogeneity of the catalyst and the metal dispersion. Numerous studies have shown that particle size and dispersion of the metal play a major role in the selectivity of catalytic reactions [7]. The dispersion, defined as the fraction of the atoms in a cluster present on the catalyst surface, depends on the conditions of preparation, approaching unity when these metallic clusters are extremely small of the order of 1 nm in size [8]. The control of the size of metal nanostructures may thus provide powerful a method to enhance the catalytic activity of metal particles [9].

Cobalt is one of the most attractive transition metals used in catalytic reactions owing to its availability and relatively low cost [10]. Typically, for heterogeneous catalysis, Co/alumina particles

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86 are prepared by using either solid state reactions of their parent 87 oxides (Co₃O₄ and γ -Al₂O₃) or by wet methods (e.g. impregnation, 88 sol-gel process) followed by their thermal treatment in air [11,12]. 89 However, Co_3O_4 and γ -Al₂O₃ have isotype crystal structures that 90 enable the migration of ions from cobalt oxide into the underlying 91 alumina support, thus forming aluminate spinels (e.g., Co₂AlO₄, 92 CoAl₂O₄) when heated. It has been suggested that cobalt ions occu-93 pying surface octahedral sites of γ -Al₂O₃ are reducible while cobalt ions occupying tetrahedral sites are not reducible at least at tem-94 95 peratures \leq 900 °C [13]. Such preparation methods demand opti-96 mization of the metal dispersion on the catalyst and the degree 97 of reduction [14,15]. It is known that Co⁺³ of Co₃O₄ can be gradu-98 ally replaced by Al^{+3} to produce the series of $Co_{3-s}Al_sO_4$ (0 < s < 2) spinels. These series include CoAl₂O₄, Co₂AlO₄, Co₃O₄, and more. 99 The interaction between Co₃O₄ and alumina could result in partial 100 101 substitution of Co⁺³ ions in Co₃O₄ spinel by Al⁺³ ions, thereby hin-102 dering the reduction of cobalt species. Cobalt reducibility is known to depend on particle size [16]. The interaction of cobalt species 103 with alumina should also be considered [17]. Alternatively, gas 104 phase methods for cobalt-based catalyst preparation have been 105 106 explored [18,19].

107 Gas phase approaches such as the so-called liquid-feed flame 108 spray pyrolysis (LF-FSP) method have been previously used to pre-109 pare CoO_x-Al₂O₃ particles [12]. In a FSP system, a metallorganic 110 precursor dissolved in fuel (solvent) is aerosolized into droplets 111 and ignited with a premixed methane-oxygen flame, the organic 112 fuel combusts forming carbon dioxide and water vapor. The metal-113 lorganic component forms metal oxide particles. The entire process 114 takes place in a time range of the order of miliseconds. Particles of 115 varying morphologies (solid, hollow, porous, etc.) and sizes can be 116 produced by controlling process parameters [20–22]. Particularly, the flame temperature, the residence time in the flame, and the 117 droplet evaporation time play a key role in the particle formation. 118 In a typical FSP, the droplets may undergo complete evaporation. 119 120 In such case, the metallorganic precursor's vapor reacts and trans-121 forms into metal oxide vapor, which then forms small nanoparti-122 cles by homogeneous nucleation [20–22]. Nanoparticles 123 synthesized via FSP exhibit typically small crystalline sizes and 124 high surface areas. Particularly, in the synthesis of metal catalysts, 125 aerosol methods ensure uniform dispersion of the active metal on a 126 support material, unlike conventional wet-based methods. If the size of the metal nanoparticles is sufficiently small, the fraction 127 of its surface atoms increases, thus improving catalyst 128 129 performance.

In this work, Co-Al spinel nanoparticles were readily synthe-130 131 sized by a one-step FSP method. The approach allows the produc-132 tion of oxide nanoparticles at a relatively high rate. FSP provides an 133 extremely short residence time of flame particles formation typi-134 cally in the range of miliseconds [23,24]. The particles were subse-135 quently reduced to obtain metallic cobalt species and investigated 136 in the conversion of glycerol in gas phase. Although, the reducibility of cobalt oxides is greatly decreased due to interaction with alu-137 minium species, this strong interaction may prevent the 138 aggregation of Co particles under the harsh reduction conditions. 139 140 Reduction of cobalt species is determinant for its catalytic performance in the conversion of glycerol. 141

142 **2. Experimental**

143 2.1. Catalyst preparation

144 2.1.1. Flame spray pyrolysis

Aluminium acetylacetonate (99%, Sigma-Aldrich) and cobalt
acetate (99,995%, Sigma-Aldrich) were used as received. The
precursor solution consisted of a mixture of aluminium acetylacetonate (0.078 mol/l) and cobalt acetate (0.017 mol/l) dissolved in a



Fig. 1. Schematics of the Flame Spray Pyrolysis system.

Table 1

 N_2 physisorption of the as-synthesized Co-Al spinel nanoparticles and Co-Al spinel nanoparticles reduced at 1123 K.

Sample	$S_{BET} \ (m^2/g)$	Pore volume (cm ³ /g)	Average pore diameter (nm)
As-synthesized Co-Al spinel nanoparticles	174	1.21	3.73
Co-Al spinel nanoparticles Reduced at 1123 K	112	0.68	3.69

solution containing 73%-v of methanol (J.T. Baker) in ionexchanged water. The Co:Al ratio in the precursor solution was approximately 0.22.

The flame spray pyrolysis system used for particle preparation has been described previously [25] and is shown in Fig. 1. Briefly, the precursor solution was fed through a capillary at a rate of 5 mL/min and atomized with a high-pressure dispersion gas, O₂, at a flow rate of 5 L/min. A premixed methane-oxygen flamelet with gas flow rates of 1 and 2 L/min, respectively, ignited the atomized precursor solution, resulting in the formation of a hightemperature flame, with temperatures in excess of 2000 K. The produced particles were collected on a Teflon filter (Zefluor, Pall Corporation). Finally, the resultant cobalt sample obtained by flame spry pyrolysis was submitted to reduction treatment. Two reduction temperature treatments were investigated: 723 K and 1123 K. The sample was reduced in a flow of 5% H₂/Ar gas flowing at 20 mL/min for 4 h.

2.2. Catalyst characterization

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The morphology and structure of the particles were characterized with a transmission electron microscope (TEM, JEM-2100F, JEOL Ltd.) equipped with a field emission electron source and operated at 200 kV. For the analyses, samples were dispersed in an alcohol and a drop of the suspension was placed over a TEM grid 171

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