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<sup>2</sup> Original Research Paper

# <sup>4</sup> Co-Al spinel-based nanoparticles synthesized by flame spray pyrolysis  $\int_{5}$  for glycerol conversion

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## A B S T R A C T

The catalytic properties of Co-Al spinel nanoparticles prepared by liquid-feed flame spray pyrolysis (L-F 35 FSP) were investigated in the glycerol conversion in gas phase in an atmosphere of hydrogen. Reduction 36 at 1123 K of the as-synthesized spinel nanoparticles induced the formation a new phase containing 37<br>metallic cobalt species. Although, the reducibility of cobalt oxides is greatly decreased due to interaction 38 metallic cobalt species. Although, the reducibility of cobalt oxides is greatly decreased due to interaction 38 with aluminium species, this strong interaction may prevent the aggregation of Co particles under the 39 harsh reduction conditions. X-ray photoelectron spectroscopy (XPS) of the reduced spinel nanoparticles 40 at 1123 K revealed that the Co/Al atomic ratio has decreased to Co/Al = 0.11, which may indicate a redis- 41 tribution of the aluminum and cobalt species at the surface of the sample submitted to the reduction in a 42 flow of hydrogen at 1123 K. X-ray diffraction (XRD) and high resolution electron microscopy (HRTEM) 43 also reinforced the formation of metallic cobalt species after reduction of cobalt from the spinel nanopar- 44 ticles at 1123 K. The main products obtained from the conversion of glycerol in the gas phase were 45 hydroxyacetone, pyruvaldehyde, lactic acid and lactide. FSP successfully gave insights to ensure uniform 46 dispersion of the active metal on a support material. 47 April 2012 12:38:47

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## 53 1. Introduction

 Glycerol is an extremely versatile building block within biore- fineries as it offers many opportunities for production of useful chemicals. Nearly two-thirds of the world's glycerol production comes as by-product from biodiesel. Furthermore, biodiesel pro- duction increased rapidly from 1 million tons in 2000 to 25 million tons in 2015 [\[1–3\].](#page--1-0) Thus, the availability of glycerol is expected to increase as the demand for biodiesel continues to rise globally. Hence, the transformation of glycerol into valued-added products and commodity chemicals has been intensively studied over the last decade [\[2\]](#page--1-0).

64 The transformation of glycerol by catalytic conversion is often 65 carried out using noble metal-based catalysts for hydrogen activa-66 tion. Conversely, transition metal-based materials are alternative

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catalysts for glycerol transformation  $[5-7]$ . Despite their lower 67 activity for hydrogenation compared to noble metals they present 68 other advantages, such as much lower prices and higher resistance 69 to poisoning  $[8]$ . 70

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In addition to the kind of metal for the catalyst other features 71 must be considered when selecting a material namely, the size of 72 the metal particle, the type and morphology of the support, and 73 the homogeneity of the catalyst and the metal dispersion. Numer-<br>
74 ous studies have shown that particle size and dispersion of the 75 metal play a major role in the selectivity of catalytic reactions 76  $[7]$ . The dispersion, defined as the fraction of the atoms in a cluster  $77$ present on the catalyst surface, depends on the conditions of 78 preparation, approaching unity when these metallic clusters are 79 extremely small of the order of 1 nm in size  $[8]$ . The control of 80 the size of metal nanostructures may thus provide powerful a 81 method to enhance the catalytic activity of metal particles [\[9\].](#page--1-0) 82

Cobalt is one of the most attractive transition metals used in 83 catalytic reactions owing to its availability and relatively low cost 84 [\[10\].](#page--1-0) Typically, for heterogeneous catalysis, Co/alumina particles 85

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86 are prepared by using either solid state reactions of their parent 87 oxides ( $Co<sub>3</sub>O<sub>4</sub>$  and  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>) or by wet methods (e.g. impregnation, 88 sol-gel process) followed by their thermal treatment in air [\[11,12\].](#page--1-0) 89 However,  $Co_3O_4$  and  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> have isotype crystal structures that 90 enable the migration of ions from cobalt oxide into the underlying 91 alumina support, thus forming aluminate spinels (e.g.,  $Co<sub>2</sub>AlO<sub>4</sub>$ , 92  $COAl<sub>2</sub>O<sub>4</sub>$ ) when heated. It has been suggested that cobalt ions occu-93 pying surface octahedral sites of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> are reducible while cobalt 94 ions occupying tetrahedral sites are not reducible at least at tem-95 peratures  $\leq$  900 °C [\[13\].](#page--1-0) Such preparation methods demand opti-<br>96 mization of the metal dispersion on the catalyst and the degree mization of the metal dispersion on the catalyst and the degree 97 of reduction [\[14,15\].](#page--1-0) It is known that  $Co^{+3}$  of  $Co_3O_4$  can be gradu-<br>98 ally replaced by  $Al^{+3}$  to produce the series of  $Co_3$ , Al,  $O_4$  (0 < s < 2) 98 ally replaced by  $Al^{+3}$  to produce the series of  $Co_{3-s}Al_5O_4$  ( $0 < s < 2$ )<br>99 spinels. These series include CoAlsO<sub>4</sub>, Co<sub>2</sub>AlO<sub>4</sub>, Co<sub>2</sub>O<sub>4</sub>, and more spinels. These series include CoAl<sub>2</sub>O<sub>4</sub>, Co<sub>2</sub>AlO<sub>4</sub>, Co<sub>3</sub>O<sub>4</sub>, and more. 100 The interaction between  $Co<sub>3</sub>O<sub>4</sub>$  and alumina could result in partial 101 substitution of  $Co^{+3}$  ions in  $Co_3O_4$  spinel by  $Al^{+3}$  ions, thereby hin-102 dering the reduction of cobalt species. Cobalt reducibility is known 103 to depend on particle size  $[16]$ . The interaction of cobalt species 104 with alumina should also be considered [\[17\].](#page--1-0) Alternatively, gas 105 phase methods for cobalt-based catalyst preparation have been 106 explored [\[18,19\]](#page--1-0).

 Gas phase approaches such as the so-called liquid-feed flame spray pyrolysis (LF-FSP) method have been previously used to pre-109 pare  $CoO<sub>x</sub>-Al<sub>2</sub>O<sub>3</sub>$  particles [\[12\].](#page--1-0) In a FSP system, a metallorganic precursor dissolved in fuel (solvent) is aerosolized into droplets and ignited with a premixed methane-oxygen flame, the organic fuel combusts forming carbon dioxide and water vapor. The metal-113 lorganic component forms metal oxide particles. The entire process takes place in a time range of the order of miliseconds. Particles of varying morphologies (solid, hollow, porous, etc.) and sizes can be 116 produced by controlling process parameters  $[20-22]$ . Particularly, the flame temperature, the residence time in the flame, and the droplet evaporation time play a key role in the particle formation. In a typical FSP, the droplets may undergo complete evaporation. In such case, the metallorganic precursor's vapor reacts and trans- forms into metal oxide vapor, which then forms small nanoparti- cles by homogeneous nucleation [\[20–22\].](#page--1-0) Nanoparticles synthesized via FSP exhibit typically small crystalline sizes and high surface areas. Particularly, in the synthesis of metal catalysts, aerosol methods ensure uniform dispersion of the active metal on a support material, unlike conventional wet-based methods. If the size of the metal nanoparticles is sufficiently small, the fraction of its surface atoms increases, thus improving catalyst performance.

 In this work, Co-Al spinel nanoparticles were readily synthe- sized by a one-step FSP method. The approach allows the produc- tion of oxide nanoparticles at a relatively high rate. FSP provides an extremely short residence time of flame particles formation typi- cally in the range of miliseconds [\[23,24\].](#page--1-0) The particles were subse- quently reduced to obtain metallic cobalt species and investigated in the conversion of glycerol in gas phase. Although, the reducibil- ity of cobalt oxides is greatly decreased due to interaction with alu- minium species, this strong interaction may prevent the aggregation of Co particles under the harsh reduction conditions. Reduction of cobalt species is determinant for its catalytic perfor-mance in the conversion of glycerol.

#### 142 2. Experimental

#### 143 2.1. Catalyst preparation

### 144 2.1.1. Flame spray pyrolysis

 Aluminium acetylacetonate (99%, Sigma-Aldrich) and cobalt acetate (99,995%, Sigma-Aldrich) were used as received. The precursor solution consisted of a mixture of aluminium acetylace-tonate (0.078 mol/l) and cobalt acetate (0.017 mol/l) dissolved in a



Fig. 1. Schematics of the Flame Spray Pyrolysis system.

Table 1

 $N_2$  physisorption of the as-synthesized Co-Al spinel nanoparticles and Co-Al spinel nanoparticles reduced at 1123 K.

Sample	$S_{BFT}$ $(m^2/g)$	Pore volume $(cm^3/g)$	Average pore diameter (nm)
As-synthesized Co-Al spinel nanoparticles	174	1 21	3.73
Co-Al spinel nanoparticles Reduced at 1123 K	112	0.68	3.69

solution containing 73%-v of methanol (J.T. Baker) in ion- 149 exchanged water. The Co:Al ratio in the precursor solution was 150 approximately 0.22. 151

The flame spray pyrolysis system used for particle preparation 152 has been described previously  $[25]$  and is shown in Fig. 1. Briefly, 153 the precursor solution was fed through a capillary at a rate of  $5 \times 154$ mL/min and atomized with a high-pressure dispersion gas,  $O_2$ , at 155 a flow rate of 5 L/min. A premixed methane-oxygen flamelet with 156 gas flow rates of 1 and 2 L/min, respectively, ignited the atomized 157 precursor solution, resulting in the formation of a high- 158 temperature flame, with temperatures in excess of 2000 K. The 159 produced particles were collected on a Teflon filter (Zefluor, Pall 160 Corporation). Finally, the resultant cobalt sample obtained by 161 flame spry pyrolysis was submitted to reduction treatment. Two 162 reduction temperature treatments were investigated: 723 K and 163 1123 K. The sample was reduced in a flow of  $5\%$  H<sub>2</sub>/Ar gas flowing 164 at  $20 \text{ mL/min}$  for  $4 \text{ h.}$  165

#### 2.2. Catalyst characterization 166

The morphology and structure of the particles were character- 167 ized with a transmission electron microscope (TEM, JEM-2100F, 168 JEOL Ltd.) equipped with a field emission electron source and oper- 169 ated at 200 kV. For the analyses, samples were dispersed in an 170 alcohol and a drop of the suspension was placed over a TEM grid 171

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