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Hasan Uslu, Dipaloy Datta, Dheiver Santos, Hisham S. Bamufleh, Cuma Bayat

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**Separation of 2,4,6-Trinitrophenol from Aqueous Solution by Liquid-Liquid Extraction
Method : Equilibrium, Kinetics, Thermodynamics and Molecular Dynamic Simulation**

Hasan Uslu^{a,d,e,*}, Dipaloy Datta^b, Dheiver Santos^c, Hisham S. Bamufleh^c, Cuma Bayat^e

^aBeykent University, Engineering and Architecture Faculty, Chemical Engineering Department,
Ayazağa, İstanbul, Turkey. E-mail: hasanuslu@gmail.com.

^bMalaviya National Institute of Technology (MNIT), Department of Chemical Engineering,
Jaipur, Rajasthan, India.

^cChemical and Materials Engineering Department, Faculty of Engineering, King
Abdulaziz University, Jeddah, Saudi Arabia.

^dDepartment of Chemical Engineering, Polytechnic School, Federal University of Bahia
(UFBA), Salvador, Brazil.

^e İstanbul Esenyurt University, Engineering and Architecture Faculty, Industrial Engineering
Department, Esenyurt, İstanbul, Turkey.

ABSTRACT

In this paper, the equilibrium and kinetic studies on the extraction of 2,4,6-Trinitrophenol (picric acid) ($0.021 - 0.061 \text{ kmol}\cdot\text{m}^{-3}$) using Amberlite LA2, a secondary amine (ALA2: $0.118 - 0.588 \text{ kmol}\cdot\text{m}^{-3}$) dissolved in a polar active solvent, methyl-iso-butyl ketone (MIBK) are performed. Also, the temperature effect ($293.2 \pm 1 \text{ K}$, $303.2 \pm 1 \text{ K}$ and $313.2 \pm 1 \text{ K}$) on the extraction mechanism and efficiency is evaluated. Thermodynamic parameters like the change in entropy and enthalpy are determined. From the values of loading ratio ($Z < 0.5$), it is inferred that the amine molecule form 1:1 complex with the acid molecule in the organic phase. The mass transfer coefficient ($k_L = 3.1 \times 10^{-5} \text{ m}\cdot\text{s}^{-1}$) of picric acid in MIBK is determined. The *Hatta* number is calculated, and observed to vary in the range of 0.0032 to 0.0054, indicating that there is a very slow chemical reaction taking place between the acid and the amine molecule in the bulk of the organic phase. The reaction order is estimated to be 0.9 w.r.t picric acid, and 0.6 w.r.t ALA2 with rate constants of $14.95 \times 10^{-6} (\text{kmol}\cdot\text{m}^{-3})^{-0.5} \text{ s}^{-1}$, and $8.94 \times 10^{-7} (\text{kmol}\cdot\text{m}^{-3})^{-0.5} \text{ s}^{-1}$, for forward and backward reaction, respectively. Kinetic and potential energies of components during reactive extraction have been determined by molecular dynamic modeling.

Keywords: Picric acid; extraction; equilibrium; kinetics; thermodynamics; molecular modeling.

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