Accepted Manuscript

Catalytic Steam Gasification of Biomass Surrogates: Thermodynamics and Effect of Operating Conditions

Jahirul Mazumder, Hugo I. de Lasa

PII: S1385-8947(16)30135-8

DOI: http://dx.doi.org/10.1016/j.cej.2016.02.034

Reference: CEJ 14767

To appear in: Chemical Engineering Journal

Received Date: 21 November 2015 Revised Date: 8 February 2016 Accepted Date: 10 February 2016



Please cite this article as: J. Mazumder, H.I. de Lasa, Catalytic Steam Gasification of Biomass Surrogates: Thermodynamics and Effect of Operating Conditions, *Chemical Engineering Journal* (2016), doi: http://dx.doi.org/10.1016/j.cej.2016.02.034

This is a PDF file of an unedited manuscript that has been accepted for publication. As a service to our customers we are providing this early version of the manuscript. The manuscript will undergo copyediting, typesetting, and review of the resulting proof before it is published in its final form. Please note that during the production process errors may be discovered which could affect the content, and all legal disclaimers that apply to the journal pertain.

ACCEPTED MANUSCRIPT

Catalytic Steam Gasification of Biomass Surrogates: Thermodynamics and Effect of Operating Conditions

Jahirul Mazumder and Hugo I. de Lasa*

Chemical Reactor Engineering Centre, Department of Chemical and Biochemical Engineering, The University of Western Ontario, London, Ontario N6A 5B9

ABSTRACT

Thermodynamic chemical equilibrium of biomass steam gasification is considered using both stoichiometric and non-stoichiometric analyses. These thermodynamic analyses include gaseous products, tars and coke, as well as consider a wide range of operating conditions. It is shown that both stoichiometric and non-stoichiometric approaches provide close results. Catalytic steam gasification of biomass surrogate species (glucose and 2-methoxy-4-methylphenol) is developed in a CREC Riser Simulator under the expected conditions of a circulating fluidized bed gasifier. A highly active and stable fluidizable Ni/La₂O₃-γ-Al₂O₃ catalyst is employed in this study, to investigate the effects of gasifier operating conditions. This catalyst yields 98% carbon conversion of glucose to permanent gases with no tar formation and negligible coke deposition at 700 °C.

Catalytic gasification results with the variation of temperature and steam/biomass ratio show limited deviation from equilibrium predictions. The deviation between

Download English Version:

https://daneshyari.com/en/article/6581955

Download Persian Version:

https://daneshyari.com/article/6581955

<u>Daneshyari.com</u>