



# Bubble nucleation, growth and surface temperature oscillations on a rapidly heated microscale surface immersed in a bulk subcooled but locally superheated liquid under partial vacuum

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## ABSTRACT

The effect of ambient pressures below atmospheric, liquid subcooling and heating rate on bubble dynamics associated with rapid evaporation in highly superheated water is investigated. Platinum films of various aspect ratios are electrically heated under partial vacuum and the average metal film temperature monitored during a power pulse of duration of several tens of microseconds.

At high liquid subcooling, the surface temperature of the pulse-heated thin platinum strips is shown to oscillate with a frequency on the order of 0.5 MHz. The oscillation frequency increases with ambient pressure in the range 0.02 MPa and 0.101 MPa, and decreases with increasing ambient temperature at a fixed pressure. An unusual dynamic instability is observed in which the surface temperature is constant before relaxing into oscillations, and the delay to oscillations increases with decreasing pressure.

High speed imaging shows that the bubble growth phase of the oscillation is associated with surface heating and the collapse phase with surface cooling in the cyclic temperature history. These effects are explained by a bubble growth theory that includes a heat loss mechanism to the surrounding liquid. The nucleation temperature is unaffected by pressure in the sub-atmospheric range examined and it approaches the theoretical superheat limit for water at a heating rate of about  $10^9$  °C/s.

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## 1. Introduction

Bubble nucleation and growth on microscale surfaces<sup>1</sup> immersed in sub-cooled liquids is an important process in applications that use bubble formation as a means to push fluid through microscale structures, as in thermal ink jet printing [2,3] and bubble pump designs [4–6]. Many parameters influence the phase change dynamics on microscale surfaces including gravity, liquid subcooling, and heater size [1,7,8] and pressure. Under some conditions the surface temperature can oscillate during the phase change process. Observed in the post-nucleation regime, oscillations have been noted for 65  $\mu\text{m}$  square thin metal films immersed in water and aqueous methanol mixtures [9,10], 100  $\mu\text{m}$  diameter by 4 cm long platinum wires in organic fluids [11] and for sub-microscale surfaces [12] under atmospheric pressure conditions. The existence

of oscillations may signal an erratic bubble dynamic that influences the quality of the droplet ejection process and is therefore important to understand.

With reference to Fig. 1, five periods characterize the overall processes leading up to surface temperature oscillations for a microscale surface with a sustained constant heat input: an initial surface heating profile (1) that consists of a somewhat exponential form associated with liquid heating; a transition period (2) marked by an inflection point in the evolution of average surface temperature that signifies the state where a bubble is nucleated; a period similar to the first (3) but with an initially higher heating rate because heat transfer is now across a vapor layer (with lower thermal conductivity compared to the liquid) because the nucleated bubble expands laterally over the surface; and remaining periods where the surface temperature is constant (4) followed by an oscillatory period (5) that can sustain itself indefinitely for a constant heat input.

The present investigation is undertaken to further examine the surface temperature oscillation phenomenon and conditions that affect it. In particular, the influence of surface heating rate, ambient pressures below atmospheric, and bulk liquid subcooling are considered for heating times on the order of several tens of microseconds. By imposing sub-atmospheric pressure conditions the

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<sup>1</sup> A microscale surface is one for which the characteristic length of the heater,  $L$ , is much smaller than the Taylor wavelength [1]  $L_{\text{Tay}} = \sqrt{\frac{\sigma}{g(\rho_l - \rho_g)}}$ . For water at 403 K (the reference temperature at which properties in Table 1 are evaluated in the present study),  $L_{\text{Tay}} \approx 2$  mm, though heaters with much smaller  $L$  (order of less than 100  $\mu\text{m}$ ) are used in this study.

## Nomenclature

AR	aspect ratio of heater (length divided by width)	$t_w$	waiting time
$C_p$	Pt film specific heat ( $\text{J kg}^{-1} \text{K}^{-1}$ )	$t_L$	time for a bubble to reach size $R_{ca}$ (s)
$g$	acceleration due to gravity ( $\text{m/s}^2$ )	$T$	Platinum temperature ( $^{\circ}\text{C}$ )
$k_L$	liquid thermal conductivity ( $\text{W m}^{-1} \text{ }^{\circ}\text{C}^{-1}$ )	$T_{\infty}$	ambient fluid temperature ( $^{\circ}\text{C}$ )
$k_s$	solid thermal conductivity ( $\text{W m}^{-1} \text{ }^{\circ}\text{C}^{-1}$ )	$T_{nuc}$	bubble nucleation temperature ( $^{\circ}\text{C}$ )
$L$	length of heater (m)	$T_w$	surface temperature ( $^{\circ}\text{C}$ )
$N_s$	number density of molecules at the surface (molecules/ $\text{m}^2$ )	$V_{in}$	input voltage to bridge (V)
$N_o$	number density of molecules in the bulk (molecules/ $\text{m}^3$ )	$V_o$	voltage amplitude for pulse input (V)
$p_{in}$	input power (W)	$V_{out}$	bridge output voltage (V)
$p_o$	input power (W) for square pulse		
$P_o$	ambient pressure		
$P_{sat}$	pressure inside the bubble		
$R_c$	critical bubble radius		
$R$	bubble radius		
$R_1$	fixed wheatstone bridge resistor ( $\Omega$ )		
$R_2$	fixed wheatstone bridge resistor ( $\Omega$ )		
$R_3$	adjustable resistor ( $\Omega$ )		
$R_H$	heater resistance ( $\Omega$ )		
$R_L$	lead resistance due to electrical connections ( $\Omega$ )		
$R_T$	$R_L + R_H$ ( $\Omega$ )		
$R_{\infty}$	heater resistance at $T_{\infty} = 22^{\circ}\text{C}$		
$S$	conduction shape factor (m)		
$t$	time (s)		
$t_b$	bubble growth time		

## Greek letters

$\alpha$	thermal diffusivity ( $\text{m}^2 \text{s}^{-1}$ )
$\delta$	separation of the equimolar surface from the surface of tension (m)
$\theta$	contact angle
$\gamma$	voltage ramp rate (V/s)
$\rho_L$	density liquid ( $\text{kg m}^{-3}$ )
$\rho_g$	density gas ( $\text{kg m}^{-3}$ )
$\rho_s$	density of metal film ( $\text{kg m}^{-3}$ )
$\sigma$	surface tension
$\tau$	$\equiv t_b/t_w$
$v$	volume of Pt film ( $\text{m}^3$ )

nucleation temperature will be constant. In saturated or superheated liquids, bubbles should always grow and not collapse and temperature oscillations should not occur. Thin metal films of high aspect ratio (AR) are employed to promote uniform surface temperatures during power pulses so that bulk subcooling will provide the primary mechanism for the collapse process that leads to surface quenching and an oscillating temperature history.

Water is selected as the working fluid because of the extensive property database available for it and familiarity with related experiments of rapid evaporation at the superheat limit [9,10,13–16]. Since surface temperature oscillations are speculated to track with bubble growth and collapse cycles as suggested by the schematics of Fig 1b and c, some visualizations of bubble morphology are also included using a laser flash method described previously [13]. For these visualizations, ethanol proved to have a more repeatable bubble morphology for the long pulse times investigated compared to water so some results on bubble dynamics are shown for ethanol and correlated to the temperature cycle.

## 2. Experiment

The heaters employed in the present investigation are layered structures consisting of a 300  $\mu\text{m}$  thick Si wafer substrate, a 200 nm thick  $\text{SiO}_2$  insulating layer, a 30-nm-thick titanium adhesion layer and a 200 nm thick Pt film on which the boiling process occurred. Fig. 2 is a cross-sectional schematic of the heater structure. Experiments were carried on platinum (Pt) films fabricated into several different ARs to facilitate measurements of the inflection point, delay time and oscillation frequency and photographing bubble shapes by high speed imaging. No single AR could allow for all such information.

Three ARs were examined. A 3  $\mu\text{m} \times 200 \mu\text{m}$  ( $\text{AR} = 67$ ) Pt film was used for measurements of  $T_{nuc}$  because temperature is uniform along the length of such films. This device is essentially the same as used in a previous study [14]. Fig. 3 shows a photomicrograph of a representative heater. High AR films are not suitable for

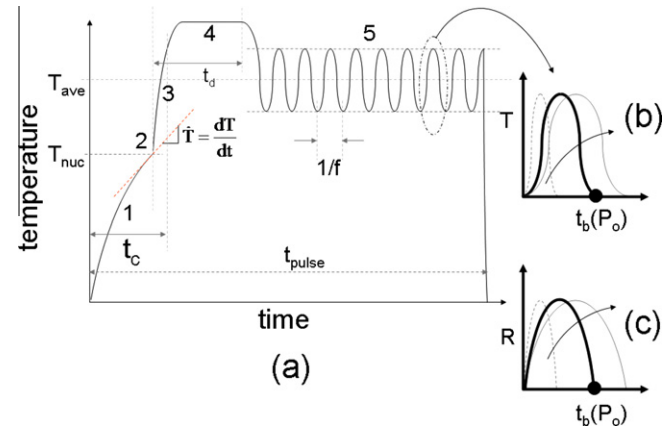


Fig. 1. (a) Illustration of temperature history for a pulse-heated microheater showing the stages prior to temperature oscillations. (b) Representation of one cycle of a temperature oscillation. (c) Suggested correspondence of one bubble growth and collapse cycle with a temperature cycle. Arrows in (b) and (c) show decreasing  $P_o$  or increasing  $T_{\infty}$ .

temperature oscillation studies because different boiling modes can co-exist over long surfaces, as shown in some visualizations of explosive bubble growth on 1.91 cm by 3.81 cm gold films in R-113 ( $\text{CCl}_2\text{FCClF}_2$ ) [17]. Reducing the heater area appears to make the bubble morphology slightly more uniform by confining the bubble to a smaller footprint, which also facilitates photographing the bubble during its growth/collapse cycle. A 4  $\mu\text{m} \times 40 \mu\text{m}$  ( $\text{AR} = 10$ ) Pt film and a 7  $\mu\text{m} \times 46 \mu\text{m}$  ( $\text{AR} = 6.6$ ) Pt film were used for recording surface temperature oscillations and for photographing bubbles, respectively. Voltage pulses ranged from 30  $\mu\text{s}$  to 90  $\mu\text{s}$  for the detailed observations reported here.

The metal films were heated by passing a current through them. The films formed one leg of a Wheatstone bridge circuit as illustrated in Fig. 4. The arrangement is similar to that described previously [14]. The bridge consists of the Pt film heater (resistance

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