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Data Article

Hydrogenation and hydrodeoxygenation of biomass-derived oxygenates to liquid alkanes for transportation fuels

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ARTICLE INFO

ABSTRACT

Article history: Received 10 June 2017 Received in revised for 17 January 2018 Accepted 22 January 20	An attractive approach for the production of transportation fuels from renewable biomass resources is to convert oxygenates into alkanes. In this paper, C ₅ –C ₂₀ alkanes formed via the hydrogenation and hydrodeoxygenation of the oligomers of furfuryl alcohol(FA) can be used as gasoline, diesel and jet fuel fraction. The first step of the process is the oligomers of FA convert into hydrogenated pro- ducts over Raney Ni catalyst in a batch reactor. The second step of the process converts hydrogenated products to alkanes via hydro- deoxygenation over different bi-functional catalysts include hydro- genation and acidic deoxidization active sites. After this process, the oxygen content decreased from 22.1 wt% in the oligomers of FA to 0.58 wt% in the hydrodeoxygenation products. © 2018 The Authors. Published by Elsevier Inc. This is an open access article under the CC BY license (http://creativecommons.org/licenses/by/4.0/).
Specifications ⁷	Table
Subject area	Biomass
More specific subject area	Bioenergy
Type of data	Table, figure
DOI of original artic * Corresponding auth <i>E-mail address:</i> sha http://dx.doi.org/10.101 2352-3409/© 2018 The (http://creativecommon	le: http://dx.doi.org/10.1016/j.energy.2017.06.052 ior. ohui99@zzu.edu.cn (S. Sun). 6/j.dib.2018.01.069 Authors. Published by Elsevier Inc. This is an open access article under the CC BY license ns.org/licenses/by/4.0/).
Please cite this ar	ticle as: S. Sun, et al., Hydrogenation and hydrodeoxygenation of biomass-derived

oxygenates to liquid alkanes for transportation fuels, Data in Brief (2018), http://dx.doi.org/ 10.1016/j.dib.2018.01.069

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How data was acquired	Gas chromatography-mass spectrometry (GC–MS), gas chromatography (GC), Fourier Transform infrared spectroscopy(FTIR), X-ray diffraction (XRD).
Data format	Analyzed
Experimental	Prepared long chain alkanes with FA condensate as raw materials.
factors	
Experimental features	Content data gathered after the run of the reaction
Data source location	Zhengzhou, China
Data accessibility	The data are with this article
Value of the data	a
• This data shows the bydrogenation pro-	a he theoretical content of C, H, O in the oligomers of FA and elemental analysis of
Value of the data • This data shows th hydrogenation pro • This data provides spectra, structural	a he theoretical content of C, H, O in the oligomers of FA and elemental analysis of oducts. the result of the hydrogenation products and hydrodeoxygenation products GC-MS formula and peak flowing out time.
 Value of the data This data shows the hydrogenation process of the second s	a he theoretical content of C, H, O in the oligomers of FA and elemental analysis of oducts. the result of the hydrogenation products and hydrodeoxygenation products GC–MS formula and peak flowing out time. he power X-ray diffraction (XRD) patterns of fresh catalysts and there average netal site.

1. Data

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83 The data in this data article has been gathered under a "The study of carbon-carbon bond forming 84 of biomass-derived furfuryl alcohol by self-condensation and subsequent hydrogenation 21376226" 85 run under the National Natural Science Foundation of China program funded by the state government 86 of China. Table 1 shows the result analysis of hydrogenation products over different reaction tem-87 perature. Table 2 shows the result of hydrogenation products by GC–MS analysis. Table 3 shows the 88 theoretical content of C, H, O in the oligomers of FA and elemental analysis of hydrogenation products. 89 Table 4 shows the alkane carbon yield and TOF under different catalysts. Fig. 1 shows the GC-MS 90 chromatogram of hydrogenation products in reaction conditions of 12 g oligomers of FA, 5 g Raney Ni, 91 60 g THF, 6 MPa H₂, reaction 4 h. Fig. 2 shows FT-IR spectra of the oligomers of FA and hydrogenation 92 93 products in reaction conditions of 12 g oligomers of FA, 5 g Raney Ni, 60 g THF, 6 MPa H₂, reaction 4 h 94 at different temperatures,(a)the oligomers of FA; (b)110 °C; (c)130 °C; (d)150 °C. Fig. 3 shows power 95 02 X-ray diffraction patterns of fresh catalysts. Table 5 shows average particle sizes of metal site in 96 different catalysts (Figs. 4-8 and Table 6).

98 Table 1

99 The result of hydrogenation products over different reaction temperature.^a

Reaction temperature (°C)	The H ₂ consumption (mol)	The mass of hydrogenation products (g)	Carbons distribution C_5-C_{20} (%) ^b			
			C ₅	C ₆ -C ₁₀	C ₁₁ -C ₁₅	C ₁₆ -C ₂₀
130	0.17	9.27	4.27	30.01	32.18	33.54
150	0.24	8.57	4.94	38.32	34.21	22.53

^a Conditions: 12 g oligomers of FA, 5 g Raney Ni, 60 g tetrahydrofuran (THF), 6 MPa H₂, reaction 4 h in a batch reactor of 300 mL. ^b Relative peak area.

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