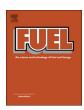


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Review article

Modeling of temperature distribution and oil displacement during thermal recovery in porous media: A critical review



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ABSTRACT

Thermal flooding is one of the most successful and widely used processes for heavy oil recovery. The memory-based fluid flow model is effective in characterizing reservoir heat transport mechanism, temperature profile, and predicting the performance of thermal recovery. Temperature has a substantial effect on the thermodynamic properties such as thermal conductivity of the formation. In addition, the influence of temperature on reservoir rock and fluid properties plays an important role in accurately predicting reservoir temperature distribution, oil displacement, and steam oil ratio. This paper presents a critical review and analyses to provide inclusive information on the state-of-the-art memory-based fluid flow modeling during the thermal displacement process. The review highlights the assumptions and limitations of the current models in the areas of thermal conductivity, temperature distribution, oil displacement, and steam oil ratio during the thermal flooding process in porous media. This paper also serves to provide an insight into future research opportunities to fill the knowledge gaps in the subject area by applying the memory concept and further improvement of the current and classical models for heavy oil recovery.

1. Introduction

1.1. Background and motivation

The current worldwide petroleum industry is facing a great challenge to produce hydrocarbon from mature reservoirs. The produced reserves from new discoveries have provided steadily declining replacement rate over the last few decades. For meeting the global energy demands by producing more oil from mature hydrocarbon reservoirs, enhanced oil recovery (EOR) is the most popular technique. EOR is accomplished by increasing the oil recovery after the primary recovery such as natural drive mechanisms, and secondary recovery such as water flooding techniques. This can be accomplished by many techniques such as thermal recovery, chemical or gas injection, ultrasonic stimulation and microbial injection. These EOR methods allow recovery of oil that was not economically recoverable earlier using conventional techniques. EOR methods involve the injection of substances and/or energy into the oil reservoir to unlock trapped oil, improve sweep and enhance production rates. Among the tertiary oil recovery methods, thermal techniques (i.e. cyclic steam stimulation, steam flooding and in-situ combustion) aim to reduce oil viscosity to increase its mobility through the application of heat into the reservoir formation. Among the EOR processes, thermal injection is the most successful and extensively

used process that is applicable to a variety of heavy oil as well as bitumen reservoirs [1]. However, the achievement of a thermal flood is entirely dependent on understanding the mechanism of heat transfer within the reservoir and the complex interactions between the reservoir rock and fluid matrices, temperature-sensitive rock and fluid parameters, which govern the evolution of the temperature profile during the thermal EOR processes [2,3].

1.2. Fluid flow modeling

It is important to predict reservoir properties and rheology through the porous media during thermal flooding. The classical constitutive equation describing fluid flow in reservoir porous media is Darcy's law [4]. This equation is based on several assumptions such as single phase, isothermal laminar flow, no chemical reaction between rock and fluid, as well as constant permeability and viscosity [4]. When heat energy is introduced, thermal alterations of reservoir rock and fluid properties induce non-Darcy flow effects, which cannot be captured accurately by the Darcy equation. This type of modeling is a complicated research task in oil and gas engineering due to the complex nature of reservoir rock and fluid properties, and geological subsurface behavior. Rheology is the study of fluid flow and its deformation, which are related to the field of physics [5]. The study of rheology focuses on materials that

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| Nomenclature List of symbols | | Greek letters | |
|-------------------------------|--|------------------------|--|
| | | ∇P | pressure gradient [Pa/m] |
| 2.000 0) | ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,, | ΔS_o | change in oil saturation before/after steam front passage |
| A_{cD} | dimensionless steam zone size [fraction] | □50 | [fraction] |
| A (t) | cumulative heated area function of time [m ²] | Δx | size of grid block in x direction |
| a | Corey coefficient of the oil relative permeability curve | VØ | fluid potential gradient [N] |
| | oil formation volume factor [rm ³ /sm ³] | | a dummy variable for time i.e., real part in the plane of the |
| B_o | specific heat capacity of fluid $[J Kg^{-1} K^{-1}]$ | ξ | |
| C_f | | ۲۱ | integral [s] distance measured ahead of the front into the coder zone |
| CSS | cyclic steam stimulation | ξ' | |
| C_o | specific heat capacity of oil [J Kg ⁻¹ K ⁻¹] | 1.0 | [m] |
| CSOR | cumulative steam oil ratio (fraction) | dξ | dummy time step [s] |
| C_w | specific heat capacity of water [J Kg ⁻¹ K ⁻¹] | ϕ | porosity of fluid media [fraction] |
| C_r | specific heat capacity of rock [J Kg ⁻¹ K ⁻¹] | μ | fluid dynamic viscosity at any temperature [Pa-s] |
| c_F | non-dimensional form-drag constant | μ_o | oil (dynamic) viscosity [Pa-s] |
| c_t | total compressibility in porous medium [1/Pa] | μ_w | water (dynamic) viscosity [Pa-s] |
| D | thermal diffusivity [m ² /s] | ρ_c | condensate density [kg/m³] |
| dt | time step [s] | ρ_f | fluid density [kg/m ³] |
| E_H | heating efficiency [percentage] | ρ_o | oil density [kg/m³] |
| $E_{h,s}$ | overall reservoir thermal efficiency [percentage] | ρ_r | dry rock density [kg/m³] |
| EOR | enhanced oil recovery | ρ_w | dry rock density [kg/m³] |
| G | the body force term due to gravity [N] | λ | thermal conductivity [Wm ⁻¹ K ⁻¹] |
| g | acceleration due to gravitation force [N] | $\lambda_h(T)$ | effective thermal conductivity function of temperature |
| H_o | heat injection rate [J/s] | , | $[Wm^{-1}K^{-1}]$ |
| H_m | hermite polynomial of order m | λ_{hf} | thermal conductivity of fluid or formation [Wm ⁻¹ K ⁻¹] |
| h | reservoir thickness [m] | λ_{hR} | effective thermal conductivity of oil sand [Wm ⁻¹ K ⁻¹] |
| k | reservoir permeability [m ²] | λ_r | reservoir thermal conductivity [Wm ⁻¹ K ⁻¹] |
| M | volumetric (overall) heat capacity [JK ⁻¹ m ⁻³] | $\lambda_{h,s}$ | thermal conductivity of steam [Wm ⁻¹ K ⁻¹] |
| m | temperature/viscosity parameter | | ratio of the pseudo-permeability of the medium with |
| P | pressure of condensate [Pa] | η | memory to fluid viscosity [$m^3s^{1+\alpha}/kg$] |
| | | / | |
| P_r | reservoir pressure [Pa] | η' | scaled dimensionless space variable |
| P_s | pressure of the system [Pa] | α | fractional order of differentiation (related to the time and |
| P_{st} | steam temperature [Pa] | | space), dimensionless |
| Q_o | cumulative oil production rate [m ³ /s] | $\alpha_1, \ \alpha_2$ | derived variable for dimensionless thickness |
| q | oil flow (drainage) rate [m ³ /s] | α_c | simplified condensate (water) or convective diffusivity |
| q_{ν} | convective heat flux [W/m ²] | $\alpha_{c'}$ | volumetric conversion factor |
| r | radial distance of reservoir in Eq. (1) [m] | β | coefficient of the classical darcy's law |
| SAGD | steam-assisted gravity drainage | eta_c | transmissibility conversion factor |
| SF | steam flooding | γ | fractional order derivative |
| S_o | oil saturation [fraction] | Γ | euler gamma function |
| S_g | gas saturation [fraction] | ξ | normal distance to the advancing front of the steam |
| S_w | water saturation [fraction] | | chamber [m] |
| T | reservoir temperature [K] | θ | inclination of the draining surface from the horizontal |
| T_{inj} | injection temperature [K] | | plane [angle] |
| T_{st} | steam temperature [K] | ω | dummy integral variable |
| T* | temperature gradient [K/m] | | , |
| T_D^* | dimensionless temperature distribution [dimensionless] | Subscrip | ts |
| dt/dx | temperature gradient along direction of heat transfer [K/ | · · · | |
| , w | m] | e | effective |
| t | time [s] | erfc | complementary error function |
| | dimensionless time [dimensionless] | f | fluid |
| t_D | dimensionless time [dimensionless] dimensionless critical time [dimensionless] | - | |
| t_{cD} | | g | gas confining layer |
| $U_x \rightarrow$ | velocity of the advancing front of steam chamber (m/s) | m | confining layer |
| \overrightarrow{u} | velocity vector [m/s] | 0 | oil |
| V_{oD} | volume of displaced oil produce [fraction] | r | rock (matrix) |
| V_{pD} | initial pore void filled with steam as water [fraction] | ν | convection |
| v_s | linear velocity of steam front [m/s] | w | water |
| W_k | a weighting function for the numerical integration | | |
| w_s | Steam zone half width [m] | | |

possess both viscous and elastic properties. Most underground reservoir fluids do not follow the Newtonian behavior [6]. Heavy crude oil is a non-Newtonian fluid at low temperatures [7]. Fluid rheology is an important issue for the prediction of rock-fluid interactions within a

complex oil reservoir or any formation management. The subsurface structure and reservoir rock properties of a formation are not only dependent on the deposition, but also on the sedimentation process within the earth's interior with respect to geological age [8]. This subsurface

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