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# Effects of CO<sub>2</sub> on sulfur removal and its release behavior during coal pyrolysis



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#### ARTICLE INFO

Article history:
Received 11 April 2015
Received in revised form 11 October 2015
Accepted 14 October 2015
Available online 23 October 2015

Keywords: Sulfur removal Sulfur release Coal pyrolysis CO<sub>2</sub> atmosphere Py-MS Py-GC

#### ABSTRACT

In this study, two Chinese coals, Jiexiu (JX) and Yanzhou (YZ) raw coals, their deashed coals and depyrited coals, were used to investigate the effects of  $CO_2$  on sulfur removal and its release behavior during coal pyrolysis by pyrolysis with mass spectrometer (Py-MS) and pyrolysis connected with gas chromatogram (Py-GC). It is found that the sulfur removal ratio of YZ and JX coals under  $CO_2$  atmosphere is higher than that under Ar atmosphere. Most sulfur removal of JX coal is distributed in tar under Ar atmosphere, while it is distributed in gas phase under  $CO_2$  atmosphere. The  $CO_2$  atmosphere is very beneficial to  $H_2S$ , COS and  $SO_2$  release into gas phase. That is the maximum evolution peak temperature of  $H_2S$  and  $SO_2$  decreases, and their evolution amount all increase remarkably, especially for COS evolution. The COS evolution of each coal increases with temperature increasing after 850 °C under  $CO_2$  atmosphere. This further validates COS formation is related to CO at higher temperatures, while it is unrelated to CO at lower temperatures.

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#### 1. Introduction

Coal, main energy and chemical raw materials, plays an important role in the energy structure of China. In recent years, there is an increasing demand for clean coals [1–3]. But large-quantity use of coal in China has caused great damage to the environment [4]. The  $SO_2$  and  $CO_2$  release from coal combustion has led to a series of air pollution related problems, such as acid rain and global warming [5,6]. Therefore, the clean coal utilization has become the urgent topic.

Sulfur in coal occurs in both inorganic and organic forms [7–9]. The inorganic sulfur is mostly pyrite and small amounts of sulfates. The organic sulfur is usually categorized as mercaptans, sulfones, aliphatic and aryl sulfides, sulfoxides, disulfides and thiophenes [6,10]. Pyrolysis is a frequent step in various conversion processes, and it is also a simple and effective way for rational utilization of coal and environmental protection [11]. During pyrolysis, both pyrite sulfur and partial organic sulfurs can be removed, a part of sulfurs goes into the gas phase in the form of H<sub>2</sub>S, COS, SO<sub>2</sub>, etc., which can be easily recovered [12]. During pyrolysis, sulfurs and minerals or sulfurs and organic matter can interact each other,

the sulfur-containing gases also can react with char and retain in the char [13,14]. The interaction between organic matter and pyrite shows that the behavior of sulfur evolution during pyrolysis may be different in raw coal, deashed coal and pyrite-free coal [15,16]. Therefore, the behavior of sulfur evolution during pyrolysis should be discussed separately.

Previous studies have mainly paid attention to desulfurization under inert atmospheres and hydrogen atmosphere, however desulfurization under inert atmospheres during pyrolysis is very low, and hydro-desulfurization still needs higher cost [4,17,18]. Semra's study [15] shows that pyrolysis under CO<sub>2</sub> atmosphere has higher organic sulfur removal ratio at higher temperatures. Pyrolysis under CO<sub>2</sub> atmosphere can not only effectively improve desulfurization ratio, but reduce the release of CO<sub>2</sub>.

Due to the very complex presence of sulfur forms in coal, the mechanism of sulfur release and its transformation behavior are still not very clear under CO<sub>2</sub> atmosphere, as well the effect of pyrite and mineral matter on them. In this study, the sulfur release and transformation behavior during pyrolysis of two Chinese raw coals, their deashed coals and pyrite-free coals were investigated by Py-MS and with Py-GC under Ar and CO<sub>2</sub>. This can provide theoretical basis for comprehensive use of coal by pyrolysis connected with pre-desulfurization.

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#### 2. Experimental

#### 2.1. Coal samples

Jiexiu (JX) and Yanzhou (YZ) raw coals, their deashed coals and pyrite-free coals were used in this study. Organic sulfur content of JX coal is the highest compared with its sulfate sulfur and pyrite, about 92.11%. Pyrite of YZ coal is higher than that in the JX coal, about 34.21%. The deashed coal and pyrite-free coal (thus depyrited dashed coal) were obtained according to the procedures described in literature [14], respectively. Their proximate and element analyses, sulfur forms and ash analyses are shown in Tables 1–3, respectively. The ratio of basic oxides to acid oxide is obtained according to the formula:  $R_{B/A} = \frac{Al_2O_3 + Fe_2O_3 + CaO_4 + MgO_7 + TiO_2 + K_2O_7 + Na_2O}{SO_3 + P_2O_5 + SiO_7}$ .

#### 2.2. Py-MS equipment

Py-MS equipment can be seen elsewhere [19]. About 1.5 g coal sample was placed into a quartz tube fixed-bed reactor (i.d. 30 mm, length 610 mm) and heated from room temperature to  $1000\,^{\circ}\text{C}$  at a heating rate of  $10\,^{\circ}\text{C/min}$  in a continuous flow of pure Ar or pure  $\text{CO}_2$  atmosphere at a flow rate of  $300\,\text{mL/min}$ . A mass spectrometer (QIC-20) was used to measure  $\text{H}_2\text{S}$ , COS, SO<sub>2</sub>, CO, etc. online, about once every 1 min.

## 2.3. Py-GC equipment

Pyrolysis experiments were carried out in quartz tube fixed bed reactor (i.d. 35 mm, length 700 mm). About 1.0 g coal was pyrolyzed under pure Ar or pure  $CO_2$  atmosphere at the temperature range from room temperature to  $1000\,^{\circ}\text{C}$  at a flow rate of  $180\,\text{mL/min}$  at heating rate of  $10\,^{\circ}\text{C/min}$ .  $H_2S$ , COS and  $SO_2$  contents (ppm) were analyzed by gas chromatography (GC) with flame photometric detector (FPD) every  $50\,^{\circ}\text{C}$  from  $50\,^{\circ}\text{C}$  to  $1000\,^{\circ}\text{C}$ , offline (SP-7800). The column and detector temperatures were  $80\,^{\circ}\text{C}$  and  $250\,^{\circ}\text{C}$ , respectively. After pyrolysis, the sample was cooled and collected for further analyzing its weight and sulfur content. And the sulfur content in coal char was measured by automatic sulfur determination analyzer (XK-5000).

## 2.4. Calculating methods

The char yield (Y) was obtained according to the following formula:  $Y = \frac{W_{\text{char}}}{W_{\text{coal}}} \times 100\%$ , where  $W_{\text{char}}$  is the weight of char after pyrolysis and  $W_{\text{coal}}$  is the weight of raw sample. The desulfurization ratio (DR) can be obtained according to the formula:  $DR\% = \frac{W_{\text{s.coal}} - W_{\text{s.coal}}}{W_{\text{s.coal}}} \times 100\%$ , where  $W_{\text{s.coal}}$  and  $W_{\text{s.char}}$  is the sulfur content in the raw coal and char, respectively [20], the desulfurization ratio and char yield are shown in Table 4.

The sulfur weight in the form of COS  $(m_{s,COS})$  obtained according to the formula:  $m_{s,COS} = \frac{V \times A_{COS}}{R \times 22.4 \times 10^6} \times M_s$ , where R is the heating rate

**Table 2**Sulfur forms analysis of coal samples.

Sample	Sulfur forms in coal (wt%)				Sulfur form ratio in total S (%)			
	$S_{t,ad}$	$S_{s,ad}$	$S_{p,ad}$	$S_{o,ad}^{a}$	$S_{s}$	$S_{\rm p}$	$S_o^a$	
YZ raw coal	3.04	0.08	1.04	1.92	2.63	34.21	63.16	
YZ deashed	2.48	0.06	0.69	1.73	2.42	27.82	69.76	
YZ pyrite-free	1.67	0.04	0.02	1.61	2.40	1.20	96.40	
JX raw coal	2.28	0.07	0.11	2.10	3.07	4.82	92.11	
JX deashed	2.27	0.04	0.21	2.02	1.76	9.25	88.99	
JX pyrite-free	2.19	0.03	0.03	2.13	1.37	1.37	97.26	

Note:  $S_t$  is the total sulfur;  $S_s$  is the sulfate sulfur;  $S_p$  is the pyrite sulfur;  $S_o$  is the organic sulfur.

10 °C/min, V is the flow rate of 180 mL/min,  $M_s$  is the atomic weight of sulfur, and  $A_{COS}$  is integrated area of COS. And  $m_{S,H_2S}$ and  $m_{SSO_2}$  can also be obtained according to the formula. For example, Fig. 1 shows the COS evolution content (ppm) of IX raw coal obtained by Pv-GC under CO<sub>2</sub> atmosphere. After integration with temperature, the integrated area can be obtained from this figure as A<sub>COS</sub>. A<sub>H2S</sub> for H<sub>2</sub>S and A<sub>SO2</sub> for SO<sub>2</sub> can be also obtained accordingly. The sulfur weight in different form of sulfur-containing gases is shown in Table 6. The sulfur presence in the gas  $(S_{gas})$  is the sum of the sulfur weight in the form of H<sub>2</sub>S, COS and SO<sub>2</sub> to the one of the raw coal, the formula  $S_{\text{gas}}\% = \frac{m_{\text{S,H}_2} s + m_{\text{S,COS}} + m_{\text{S,SO}_2}}{W_{\text{s,coal}}} \times 100\%$ ; the sulfur presence in the char  $(S_{\rm char})$  was obtained by the formula:  $S_{\rm char}\% = 100\% - DR(\%)$ ; the sulfur presence in the tar  $(S_{tar})$  was obtained by the following formula:  $S_{tar}\% = 100\% - S_{gas}\% - S_{char}\%$ .

#### 3. Results and discussion

#### 3.1. Effects of CO<sub>2</sub> on sulfur removal during pyrolysis

Table 4 shows the desulfurization ratio of different coals and their char yield during pyrolysis under Ar and CO<sub>2</sub> atmospheres. Generally speaking, under Ar atmosphere sulfur removal ratio is related to the volatile content and the stability of organic sulfur in the coal. That is the higher the volatile content is, and the less stable the organic sulfur is, thus the higher sulfur removal ratio is. Under Ar atmosphere, for those two raw coals, the sulfur removal ratio is YZ > JX. This order is very consistent with the volatile content shown in Table 1. This indicates, for JX coal, the organic sulfur is very stable, which can hardly decompose during pyrolysis. For YZ coal with higher pyrite, the desulfurization ratio is deashed coal > depyrited coal > raw coal, this suggests that the deashed treatment and depyrited treatment is helpful for sulfur removal. The reason may be that heat transfer and mass transfer can increase sharply for their deashed and depyrited coals during pyrolysis. This may be also caused by the basic mineral of raw coals

**Table 1**Proximate and ultimate analyses of coal samples (wt%).

Sample	Proximate analyses				Ultimate analyses				
	$M_{\rm ad}$	$A_{\mathrm{ad}}$	$V_{ m daf}$	$FC_{daf}$	$C_{\rm ad}$	$H_{\rm ad}$	$O_{\mathrm{ad}}^{a}$	$N_{\mathrm{ad}}$	$S_{ad}$
YZ raw coal	3.19	12.09	42.85	57.15	67.03	4.63	7.98	1.32	3.76
YZ deashed	3.40	2.02	38.92	61.08	73.80	4.83	11.96	1.51	2.48
YZ pyrite-free	3.55	0.93	39.71	60.29	75.05	4.94	12.33	1.53	1.67
JX raw coal	0.55	10.25	20.75	79.25	76.52	4.04	5.04	1.32	2.28
JX deashed	0.90	0.33	19.82	80.18	84.39	4.33	6.34	1.44	2.27
JX pyrite-free	0.99	0.15	20.39	9.61	84.26	4.35	6.64	1.42	2.19

Note: ad is air-dried basis; daf is dried and ash-free basis.

a By difference.

<sup>&</sup>lt;sup>a</sup> By difference.

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