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# A novel theoretical approach to the temperature–viscosity relation for fluidic fuels

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## HIGHLIGHTS

- Novel theoretical approach to the viscosity of fluidic fuel was constructed.
- Equation for viscosity over temperature was derived.
- Viscosity decreased with temperature, but increased in high temperature region.
- Good agreements with the reported data from references were found.

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## ABSTRACT

Viscosity is a first and foremost function both for theory and application. By approximating the interaction potential of molecule in fluidic fuel as constant and proposing a new method to calculate the momentum transfer by means of the radius of averaged volume per molecule, an equation of viscosity versus temperature was derived, which were found in good agreement with a lot of data from gaseous to liquid fuels by the curve fit. The equation also predicted that the viscosity initially decreased with temperature and then slowly increased in the high temperature region. When using it as correlation equation for the dependence of viscosity on temperature, it was able to cover more fluids from gaseous to liquid fuels.

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## 1. Introduction

Fluidic fuel includes liquid and gaseous fuels. They are the major types of chemical fuels that cannot be replaced in industrial and daily life up to now. Knowledge of the viscosity of fluidic fuel is important since it determines the temperature for handling, the size of the centrifuges and the temperature at which the fuel is injected into the engine. In these process, the relation between viscosity and temperature plays a crucial role.

Because of the importance in theory and practice, there has long been an effort to find the equation that can be applied for more fluids in wider temperature and viscosity ranges. Since Reynolds presented the first equation correlating the viscosity and temperature [1], a lot of equations were reported subsequently, which can be classified into three forms: the early form, the Arrhenius and the log–log forms. The early formula such as Reynolds' [1] and Vogel's [2] could only cover narrow temperature and viscosity

range. The Arrhenius form included the Arrhenius equation, Williams–Landel–Ferry equation, Fulcher's [3], and improved Vogel equation. The more complicated log–log form was also used in the attempt to cover wider temperature and viscosity ranges [4,5]. Because of the importance in fuel production, transportation, storage and application, attentions have been especially paid to the temperature dependent viscosity models or correlations for fluidic fuels, such as for crude oils [6,7], for predicting natural gas viscosity [8], for biodiesel [9–16], for mixed oil [17] and waxy oils [18], for petroleum reservoir fluids [19], for lubricants [20], for hydrocarbon Fractions [21] and light hydrocarbon solvents [22]. Most equations from the mentioned references were constructed on pure experience of single or a type of fuel/crude fuel to fit the experimental data in various ranges of temperature and viscosity. As a result, they can hardly be applied to the whole fluidic fuels of both gas and liquid. It is always desired to construct an ideal equation that has theoretical background and is able to cover both liquid and gaseous fuels in wider temperature and viscosity ranges.

In present paper, the author approximated the molecular interaction in the fluidic fuel as constant potential, and derived novel

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**Nomenclature and symbols**

$A$	constant	$v_y$	y components of molecular velocity
$b$	thickness of the layer	$v_z$	z components of molecular velocity
$C$	Sutherland's constant	<i>Greek letters</i>	
$E_i$	averaged intermolecular interaction potential in J mol <sup>-1</sup>	$\dot{\gamma}$	shear rate
$F$	averaged force vector	$\varepsilon$	averaged intermolecular interaction potential
$k$	Boltzmann's constant	$\eta$	viscosity
$m$	mass of molecule	$\eta_0$	viscosity constant
$n$	molecule density or number of data points	$\tau$	shear force
$N$	total number of molecules	$\sigma$	collision cross-section of molecule
$N_A$	Avogadro constant	<i>Subscripts</i>	
$r$	radius of molecular space	$cal$	calculated value
$R$	universal gas constant	$i$	interaction
$T$	absolute temperature	$x$	x-coordinate
$T_i$	interaction temperature in kelvins	$y$	y-coordinate
$T_0$	reference temperature in kelvins	$z$	z-coordinate
$u$	potential field	$0$	constant
$U$	shear velocity		
$V$	volume		
$v_x$	x components of molecular velocity		

82 formula of viscosity versus temperature for the fluidic fuel based  
83 on statistical mechanics. Finally, comparison between the theoretic-  
84 al data and the experimental data gathered by author was given.

85 **2. Theoretical**

86 *2.1. Approximation to interaction potential inside fluidic fuel*

87 Because of the huge number of molecules, it is usually too com-  
88 plex to accurately calculate the intermolecular interaction inside  
89 the fluidic fuel. However, approximations of various degree of  
90 accuracy can be made while expressing the intermolecular interac-  
91 tion by potential function.

92 Inside a liquid fuel, and away from the boundary, molecules are  
93 surrounded by other molecules of the same type and are thus  
94 attracted in all directions equally. This is saying that there is no  
95 net force on molecules inside the liquid fuel. This feature is  
96 mathematically expressed as  $F = -\nabla u \approx 0$ , here  $u$  denotes the  
97 potential a molecule feels. The solution of this equation is  $u =$  con-  
98 stant, which presents a constant potential inside the liquid fuel.

99 Since the gaseous fuel molecule almost moves freely, its  
100 amount of potential can be considered as a constant that  
101 approximately equal to zero ( $u \approx 0$ ). Mathematically, the constant  
102 potential inside fluidic fuel can be simply derived by taking the  
103 zeroth-order approximation in the Taylor expansion of the poten-  
104 tial function.

105 *2.2. A distribution function for fluidic fuel*

106 According to statistical mechanics, the distribution function is  
107 applicable to describe the molecules inside fluidic fuel. Upon the  
108 above approximation and presenting the constant potential of  
109 interaction as  $\varepsilon$ , the following formula of distribution function for  
110 the molecule in fluidic fuel in thermal equilibrium was proposed,  
111

$$f = n \exp\left(\frac{\varepsilon}{kT}\right) \left(\frac{m}{2\pi kT}\right)^{\frac{3}{2}} \exp\left[-\frac{m(v_x^2 + v_y^2 + v_z^2)}{2kT}\right] \quad (1)$$

114 where  $n = N/V$  denotes the molecule density of the fluid,  $N$  is the  
115 total number of molecules restricted in volume  $V$ .  $k$  is  
116 Boltzmann's constant,  $T$  is absolute temperature.  $m$  is the mass of  
117 molecule,  $v_x, v_y, v_z$  are the x, y, z components of molecular velocity.

118 *2.3. The temperature dependence of viscosity for fluidic fuel*

119 In order to calculate the viscosity of fluidic fuel, formula for the  
120 shear stress should be obtained first. As an approximation, the  
121 shear stress in a fluid is calculated by the momentum transfer  
122 across shear surface. In liquid, the steric resistance forbids most  
123 molecules to get across the shear surface through Brownian ran-  
124 dom motion except the ones nearby the shear surface. In gas, the  
125 collision changes the direction of most molecules moving toward  
126 the shear surface before it gets across the shear surface, except  
127 the ones nearby the shear surface in the range of mean free path.  
128 Therefore, only the part of molecules in fluidic fuel nearest the  
129 shear surface interchanges molecular momentum through random  
130 motion in the y-direction (Fig. 1). Upon this consideration, the net  
131 shear stress from the momentum transfer is expressed as  
132

$$\tau \approx \frac{2r}{b} \int_0^\infty mUv_y f dv_x dv_y dv_z = n \exp\left(\frac{\varepsilon}{kT}\right) \sqrt{\frac{mkT}{2\pi}} \frac{Ur}{b} \quad (2)$$

135 Here,  $U$  denotes the shear velocity to the fluid layer considered,  
136  $b$  the thickness of the layer,  $r$  the radius of the averaged volume per  
137 molecule, which presents the linear dimension of the effective  
138 space occupied by a molecule in the fluidic fuel. In liquid  $r$   
139 approaches the radius of a real molecule. In gas  $2r$  denotes the  
140 mean free path. If a gaseous fuel were sufficiently compressed,  $r$   
141 should reduce to the real radius of the gas molecule.

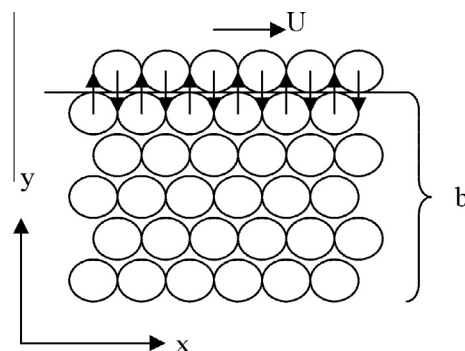


Fig. 1. The momentum transfer from the molecular exchange between nearby molecules in a fluid.  $b$  = thickness of a layer,  $U$  = the shear velocity to the fluid layer at shear surface. Sphere notes a model of the averaged volume occupied by a molecule.

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