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Enhanced hydrogen generation by methanolysis of sodium borohydride in the presence of phosphorus modified boehmite

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HIGHLIGHTS

- Phosphorus (P) modified boehmite catalyst was prepared.
- Methanolysis of NaBH₄ was effectively accelerated by using P/boehmite catalyst.
- Catalytic activity of P/boehmite was improved by appropriate calcination treatment.
- First-order kinetic model was proved to be the suitable kinetic model.
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ABSTRACT

Phosphorus (P) modified boehmite catalysts were prepared with wet impregnation method using phosphoric acid (H_3PO_4) as the P source. The P/boehmite catalysts with different P loadings ranging from 0 to 6.4 wt% were obtained by regulating the concentration of H_3PO_4 . These catalysts were characterized by BET surface area and FTIR spectroscopy measurements and their catalytic performance for hydrogen generation by methanolysis of sodium borohydride at 0 °C was evaluated. The results show that the as-prepared non-metallic P/boehmite catalyst exhibited high catalytic activity toward the methanolysis reaction under the circumstance of low environmental temperature. Appropriate calcination treatment can enhance the catalytic activity of P/boehmite catalyst to some extent. To understand the kinetic behavior of the methanolysis reaction in the presence of these catalysts, the experimental data were fitted to both zero-order and first-order kinetic models using the integral method.

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48 **1. Introduction**

Proton exchange membrane fuel cells, also known as polymer 49 electrolyte membrane fuel cells (PEMFCs), are a type of fuel cell 50 51 being developed for transportation applications as well as for stationary and portable applications. Basically, the fuel cell technol-52 ogy converts an energy carrier, mostly hydrogen, into electricity. 53 However, its widespread use is severely limited by the lack of a 54 55 safe, convenient, efficient hydrogen storage and infrastructure system [1]. To overcome these major barriers, much effort has been 56 made to convert various fuels into hydrogen in situ [2]. 57

58 Chemical hydrides have attracted wide attentions as a novel 59 approach to provide pure hydrogen for fuel cells due to some 60 advantages including stability, nonflammable in alkaline solution, 61 convenience of H₂ release via hydrolysis at ambient conditions,

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http://dx.doi.org/10.1016/j.fuel.2014.05.071 0016-2361/© 2014 Published by Elsevier Ltd. and recyclability of byproducts [3]. During the past decade, considerable efforts have been made to generate hydrogen by the hydrolysis of NaBH₄, most of which focus on catalysts, reactors, and hydrolysis kinetics [4–7]. Although the hydrogen storage density based on this hydrolysis reaction stoichiometry is 10.8 wt%, the actual hydrolysis of NaBH₄ is typically conducted in the aqueous phase where large quantities of excess water are required to facilitate mass transfer of reactant and ensure complete dissolution of hydrated byproduct (NaBO₂ xH₂O), resulting in a significant reduction of the gravimetric hydrogen storage capacity from 10.8 to 2.9 wt% [8–10].

Recently, the reaction of methanol rather than water with NaBH₄ has been successfully demonstrated for the generation of hydrogen [11–13]. Compared to the hydrolysis system, the methanolysis system is more attractive because of some additional advantages. The rate constant for the methanolysis reaction at 273 K has been suggested to be greater than that of the hydrolysis reaction [14]. The byproduct, NaB(OCH₃)₄, has less tendency of

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plugging the reactor. In addition, the low freezing point of
methanol makes the methanol–NaBH₄ system to be suitable to
generate hydrogen at subzero temperatures. Most of all, the hydrolysis of NaB(OCH₃)₄ by-product liberate the consumed methanol
efficiently, which thus can be continuously recycled and reused
in methanolysis reaction [15].

To facilitate the application in cold weather condition, it is critical to improve the kinetics of the methanolysis reaction at low solution temperatures. Hannauer et al. [16] found that Co–TiO₂ shows higher catalytic performances than those of Ru-TiO₂ toward methanolysis of NaBH₄. Lo et al. [11] have investigated the methanolysis of NaBH₄ over 45 to $-20 \,^{\circ}$ C using metal chlorides and platinum-coated lithium cobalt oxide as catalysts. The results showed that the rate of methanolysis was enhanced by more than 110 times at $-20 \,^{\circ}$ C in the presence of 10 wt% CoCl₂ catalyst. NiCl₂, Ni₂B and RuCl₃ were also found to be effective in improving the kinetics of alcoholysis reaction in non-stabilized NaBH₄ [17].

97 Recently, Ru immobilized Al₂O₃ pellets were synthesized as a 98 catalyst for hydrogen generation from the methanolysis of NaBH₄ 99 in alkaline solution [13]. In our previous study, Co/Al₂O₃ was pro-100 ven to be an effective catalyst for the methanolysis of NaBH₄ [18]. 101 Up to now, only several supported transitional metal catalysts have 102 been demonstrated to exhibit high performance for this methanol-103 ysis reaction, and the literatures for the methanolysis of NaBH₄ 104 with non-metallic catalysts remain scarce. Boehmite (AlOOH) is 105 an important material which can be utilized industrially as the catalyst or the precursor of the catalysts. In the present work, we 106 107 report for the first time the application of boehmite and phosphorus modified boehmite as catalysts for hydrogen generation by 108 109 methanolysis of NaBH₄.

110 2. Experimental

111 2.1. Catalyst preparation

112 Commercial boehmite (Shandong Aluminium Co., Ltd. China) was used as the catalyst precursor. Different weight percentages 113 of phosphorus (0.4, 2.0, 3.9, and 6.4) were doped into boehmite 114 115 by the wetness impregnation method using phosphoric acid solution as a source of P. The phosphorus-doped boehmite was then 116 calcined in air at 300 °C for 2 h. The as-prepared catalysts are 117 118 denoted as xP/boehmite, where x indicates the nominal amount 119 of phosphorus present in the samples.

120 2.2. Catalyst characterization

121 The specific surface area (Brunauer–Emmett–Teller, BET), pore 122 size (Barrett–Joyner–Halenda, BJH), and pore volume (V_p) of the 123 catalysts were measured by the N₂ adsorption–desorption method 124 at liquid nitrogen temperature (–196 °C) using an ASAP 2010 125 apparatus (Micromeritics). Fourier transform infrared (FTIR) spec-126 tra of the samples were recorded on a TENSOR27 FTIR spectropho-127 tometer (Bruker) in the range of 400–4000 cm⁻¹.

128 2.3. Catalyst testing

Methanol (99.5% purity, Yantai Sanhe Chemical Reagent Co., Ltd, China) and sodium borohydride (NaBH₄, 98.0% purity, Sinopharm Chemical Reagent Co., Ltd, Shanghai, China) were used as received in this work. The kinetic studies were carried out with the same method and apparatus as described in [18]. The conversion of hydrogen volume into number of moles was done by applying the ideal gas law at room temperature (20 °C).

3. Results and discussion

3.1. Textural properties

Fig. 1 provides the N_2 adsorption/desorption isotherms measured at 77 K and pore-size distributions for the unmodified and phosphorus modified boehmite catalysts. As shown in Fig. 1a, the shapes of adsorption/desorption isotherms are those of typical "type IV" isotherms with H3 hysteresis loops according to the IUPAC classification. These significant hysteresis loops at relative pressure *P*/*P*₀ above 0.50 indicate the presence of non-uniform slit-like mesopores in the samples [19,20], which is parallel to the observation of pore size distributions in Fig. 1b based on the pore volumes of the BJH (Barrett–Joyner–Halenda) desorption branch in the measurement of nitrogen isotherms. As shown, these pore size distributions are broad and mainly range from 4 to 30 nm.

Table 1 summarizes the textural properties of the boehmite and P/boehmite catalysts employed in this work. As shown in Table 1, the BET surface areas and pore volumes of P/boehmite catalysts decrease with phosphorus loading, implying the progressive blockage of the boehmite pores by phosphorus oxide species. It was also suggested that the decrease in the surface areas and pore volume at higher phosphorus loadings can be ascribed to the formation of polymeric phosphorus modified H-ZSM-5 catalysts [21].

3.2. FTIR spectra

FTIR spectra of the boehmite and P/boehmite catalysts are 161 shown in Fig. 2. In the case of boehmite, the intensive peak centered at 3478 cm^{-1} and weak band centered at 1630 cm^{-1} are 163

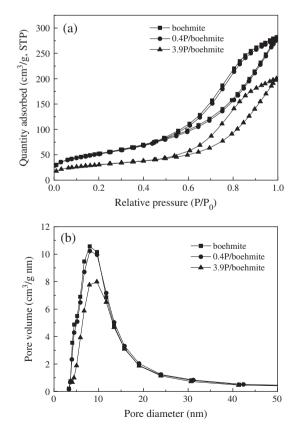


Fig. 1. N_2 adsorption/desorption isotherms (a) and BJH pore size distributions (b) of boehmite and P/boehmite samples.

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