

Accepted Manuscript



Thermo-hydrous behavior of dried un-blanching potato samples

I. Boutelba, S. Zid, P. Glouannec, S. Youcef-ali, A. Magueresse, N. Kimouche

PII: S0260-8774(18)30316-9
DOI: 10.1016/j.jfoodeng.2018.07.027
Reference: JFOE 9341
To appear in: *Journal of Food Engineering*
Received Date: 17 November 2017
Accepted Date: 23 July 2018

Please cite this article as: I. Boutelba, S. Zid, P. Glouannec, S. Youcef-ali, A. Magueresse, N. Kimouche, Thermo-hydrous behavior of dried un-blanching potato samples, *Journal of Food Engineering* (2018), doi: 10.1016/j.jfoodeng.2018.07.027

This is a PDF file of an unedited manuscript that has been accepted for publication. As a service to our customers we are providing this early version of the manuscript. The manuscript will undergo copyediting, typesetting, and review of the resulting proof before it is published in its final form. Please note that during the production process errors may be discovered which could affect the content, and all legal disclaimers that apply to the journal pertain.

1 Thermo-hydrous behavior of dried un-blanchéd potato samples

2 I. BOUTELBA¹, S. ZID¹, P.GLOUANNEC², S. YUCEF-ALI¹, A.MAGUERESSE², N. KIMOUCHE¹

3 ¹ Laboratoire du Génie Climatique Constantine -LGCC, Université Frères Mentouri Constantine 1, Ain Elbey, 25000 Constantine, Algérie

4 ² Institut de Recherche Dupuy de Lôme, Université Bretagne Sud, B.P.92116, 56321 Lorient Cedex, France

5 Abstract

6 This study concerns a purely convective drying of parallelepiped un-blanchéd potato slices. A numerical model for heat and mass transfer
7 has been developed in Lagrangian referential to overcome the structural changes. The thermo-physical properties of the slices vary with the
8 temperature and moisture content. The finite volume method combined with a typically implicit time pattern was used to solve the model
9 equations. The evaporated mass flux was calculated using the transfer surface area by which the water evaporates, and heat transfer
10 coefficient was estimated using Nusselt number; The inverse method was used in this computation. The experiments were carried out under
11 several thermo-aerualics conditions in order to determine the most influent operating variable on the drying kinetic. A good agreement
12 between experimental and simulated results was obtained with a moisture content determination coefficient (R^2) higher than 0.9980;
13 Whereas, the surface and center temperatures are higher than 0.9328 and 0.9305 respectively. The results have shown that the air temperature
14 is the most important parameter that controls the drying kinetic.

15 **Keywords:** Experiment; Convective drying; Mass and heat transfer; Numerical model; Drying rate, Potato.

16 Nomenclature

17 c_p	specific heat, J kg ⁻¹ K ⁻¹	42 Re :	Reynolds number
18 D	water diffusion coefficient, m s ⁻²	43 Greek letters	
19 DR	drying rate, kg _w kg ⁻¹ _{ds} min ⁻¹	44 ρ :	density, kg m ⁻³
20 e_p	thickness, m	45 ψ :	linear shrinkage coefficient
21 F_m	evaporation rate, kg _w m ⁻² s ⁻¹	46 ζ :	Lagrangian coordinate
22 h_c	heat convective exchange coefficient, W m ⁻² K ⁻¹	47 λ :	thermal conductivity, W m ⁻¹ K ⁻¹
23 Hr	air relative humidity, %	48 σ :	Stephan-Boltzmann constant, W m ⁻² K ⁻⁴
24 l	width, m	49 ϵ :	Emissivity
25 L	length, m	50 Subscripts	
26 L_v	latent heat of vaporization, J kg ⁻¹	51 ϕ :	initial value
27 m	mass, kg	52 a :	air
28 M_v	molecular weight, kg mol ⁻¹	53 c :	center, middle
29 P_t	atmospheric pressure, Pa	54 cr :	critical
30 P_v	water vapor pressure, Pa	55 ds :	dry solid
31 R	universal gas constant, J mol ⁻¹ K ⁻¹	56 eff :	effectif
32 S	surface, m ²	57 h :	humid
33 t	time, s	58 l :	liquid
34 T	temperature, K, °C	59 moy :	average
35 V	velocity, m/s	60 p :	wall of dryer
36 v_s	solid displacement, m s ⁻¹	61 s :	solid
37 X	moisture content, kg _w kg ⁻¹ _{ds}	62 sat :	saturated
38 Dimensionless Numbers		63 $surf$:	surface
39 Le :	Lewis number	64 v :	vapor
40 Nu :	Nusselt number	65 w :	water
41 Pr :	Prandtl number		

66 Introduction

67 The moisture content of the most agro-foodstuffs is 70-95 % (wet basis) (Kiranoudis et al., 1993), this has imperatively
68 an influence on microbiological activity (Nagwekar et al., 2017), volume and product stability (storage life). In 2016 total
69 world production of potato was more 376 million tons (FAOSTAT, 2018), two thirds are consumed by people as food, the
70 other third production is used in transformation industries (Friedman et al., 2017; Park & Yoon, 2018). However, Algeria is
71 considered as the biggest producer of potato in Africa, more than 4.78 million tons in 2016. Unfortunately, some part of the
72 harvest has to be left to the abundant because of a bad industrial or commercial orientation. The glucides are the principal
73 constituent of potato dry matter (16-25 %), mainly starch (60–80 % of the total dry matter contents) (Youcef-ali et al., 2001;
74 Levly & Rabinowitch, 2017); they are used in pharmaceuticals, cosmetics, textiles, woods and papers industries.

75 In recent years, drying consumes a lot of energy, up to 70 % for wood industry and 50% for the textile (Minea, 2013),
76 whereas the food industry consumes about 15 % (Perussello et al., 2014), although an inappropriate drying can increase this
77 consumption and decrease the final product quality. The quality concept can be characterized by microbiological activity, the
78 shrinkage, nutritional control and the sensory characteristics (Tsami et al., 2000; Chua et al., 2000; Cui et al., 2008) which are
79 directly related to product moisture content and temperature (Kalbasi et al., 2000). During drying, the product dehydrates on
80 the surface faster unlike the heart (Wang & Brennan, 1993; Srikiatden et al., 2008; Mihoubi et al., 2009). Consequently, to

Download English Version:

<https://daneshyari.com/en/article/6664366>

Download Persian Version:

<https://daneshyari.com/article/6664366>

[Daneshyari.com](https://daneshyari.com)