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Transient thermo-mechanical analysis of steam generators for solar tower plants



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HIGHLIGHTS

- Thermal-stress modeling of the steam-generator dynamic behavior for a solar tower plant.
- The highest stresses occur in the superheater tubesheet junction.
- High stresses were found under part-load conditions instead of nominal conditions.
- Start-up takes between 50 min and 110 min, depending on the steam-generator initial-condition.
- Between 600 tons and 716 tons of hot salt are needed for the start-up procedure.

ARTICLE INFO

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ABSTRACT

In solar power tower plants, fast start-ups and/or load changes are mandatory to increase the power plant dispatchability. The high temperatures of the working fluids and the partial-load operation will reduce the lifetime of the thick-walled components at the steam generator. Therefore, a proper heat exchanger design should consider the stress evolution during the transient operation of the plant.

This work addresses, for the first time, a methodology to determine the dynamic behavior of all heat exchangers of a steam generator train. The methodology proposed here is a powerful tool for the design of solar power plants. The stress analysis model identifies the most important components of the steam generation train during transient operation. The methodology consists of the combination of analytical models to obtain the coupled response of the steam generation train from the following dynamic variables: temperature, pressure and stress.

An example of this methodology is presented for two start-up initial conditions: the assumption of non-isothermal and isothermal temperature profiles of the heat exchangers. A steam generator train based on conventional shell and tube heat exchangers is analyzed. The analysis shows that the non-isothermal condition takes approximately 50 min to reach nominal conditions, whereas the isothermal condition takes approximately 110 min, requiring 600 tons and 716 tons of hot salt to perform the start-up procedure, respectively.

1. Introduction

In recent years, significant effort has been made to reduce the operation and investment costs of concentrating solar power (CSP) plants. One of the main differential features with respect to other renewable technologies, such as photovoltaics or wind, is the flexibility provided by CSP when integrated with a thermal energy storage (TES) system. This increases the economic competitiveness of these power plants. On the one hand, the increase of the capacity factor diminishes the cost per unit of energy produced. On the other hand, the instantaneous solar source is decoupled from the electricity generation and therefore can be

delivered on demand. Then, CSP with a TES system enhances the possibility of participating in grid balancing services [1]. In this manner, these plants may be considered as dispatchable, and therefore, improvements in the flexibility by means of fast start-ups and/or load changes may lead to additional revenue [2]. Moreover, fast start-ups are especially interesting for CSP plants due to the increase of the annual electricity production [3,4]. However, the start-up and/or load change ramps are limited by the thermal stresses in thick-walled parts of the steam generator (SG) and/or steam turbine. These thermal changes may produce fatigue and/or creep damage in the SG [5]. For this reason, considerable effort should be made to develop dynamic

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Nomenclature		а	thermal diffusivity (m/s²)
		h	convective coefficient (W/m ² °C)
Abbrevia	tions	i	specific enthalpy (J/kg)
		l_{ts}	tubesheet thickness (mm)
CCPs	combined-cycle plants	ṁ	mass flow rate (kg/s).
CSP	concentrating solar plants	t	time (s)
EV	evaporator	t_j	thickness of component j (m)
FEA	finite element analysis	t	dimensionless time (-).
FW	feed water	r	radial coordinate (-)
HP	high pressure	и	specific internal energy (kJ/kg)
HPT	high-pressure turbine	y	vertical displacement (m)
HRSG	heat recovery steam generator	Z	axial coordinate (-)
HTF	heat transfer fluid		
HT	hot tank	Greek symbols	
Нх	heat exchanger	-	
LP	low pressure	α_t	thermal stress concentration factor (-)
LPT	low-pressure turbine	α_m	pressure stress concentration factor (-)
PH	preheater	β_t	linear thermal expansion coefficient (1/K)
R	receiver	θ	rotation angle (°)
RH	reheater	ν	Poisson's ratio (-)
SG	steam generator	ρ	density (kg/m ³)
SH	superheater	σ	stress (MPa)
SPTP	solar power tower plant	ψ	U-tube stress concentration factor (-)
TES	thermal energy storage	,	
UTS	ultimate tensile strength	Subscrip	ts
G 1 - 1 -	Ç .	0	nominal conditions
Symbols		ave	
	1 6 2		average
A	heat transfer area (m ²)	atemp	attemperator
A_c	cross-section area (m ²)	b !	bending
C	specific heat capacity (kJ/kg K)	cyl	cylinder
C_m	dimensionless thermal capacitance of a metal wall (-)	d	drum
D	diameter (m), characteristic time constant (-)	dc	downcomer
E	modulus of elasticity (MPa)	h	head
F	force (N)	i	inlet, inner
I	moment of inertia (m ⁴)	m	metal
K	stiffness (N/m)	i	inlet
K'	inverse of stiffness (m/N)	0	outlet, outer
L	length (m), characteristic length constant (-), level (m)	r	riser
L_{tp}	tube pitch (mm)	rec	recirculated
L_{ts}	tubesheet thickness (m)	S	shell
M	mass (kg), moment (N m)	sa	salt
P	pressure (Pa)	sat	saturated
R	radius (m)	st	steam
R_{otl}	radius of a circle circumscribed to the outermost tube of a	su	surface
	bundle (m)	t	tube
T	temperature (°C)	tp	tube pitch
T	dimensionless temperature (-)	ts	tubesheet
	volume (m ³), vertical force (N)	w	water
V	turbine power (MWe)	**	

models that consider the lifetime of the heat exchangers. These models allow the study of different strategies for operating the plant on the safety-side while saving energy during the start-up and shutdown processes.

One of the main features of solar power tower plants (SPTPs) is their higher operating temperatures compared to parabolic trough and linear Fresnel plants [2]. This leads to an increase in the thermal efficiency of the power block, which also reduces the specific costs. Examples of the feasibility of CSP technology are Gemasolar [6], Crescent Dunes [6] and Suncan Dunhuang [6], the three large-scale SPTPs currently in operation. However, other technologies, such as fire-boilers or combined-cycle plants (CCPs), work at similar temperatures to CSP plants. One of the main differences between conventional and CSP plants appears in

the SG. The heat exchangers of the SG are based on conventional shell and tube designs. These heat exchangers are sized by means of analytical methods proposed by TEMA standards [7] and/or ASME code Section VIII-Div1 [8] considering the operation at nominal conditions [9]. Then, because the SG will be operated with daily start-ups, load changes and shutdowns, a transient stress analysis is required. Moreover, no specific guidelines are proposed in the TEMA standards and/or ASME code for complex zones, such as the tubesheet, when: transients thermal loadings occur [10], temperature gradients on the junction appear [11] or the tubesheet has a non-standard design [12]. Therefore, these issues must be accomplished by finite element analysis or by complex analytical methods to obtain accurate results.

Start-up and shutdown operations become critical to the creation of

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