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The role of steam in silica vaporization and ultrafine particulate matter formation during wet oxy-coal combustion



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HIGHLIGHTS

• H₂O enhances the vaporization of silica in wet oxy-coal combustion.

Improved model for SiO₂ vaporization was developed to analysis the effect of H₂O.

• Changes of char combustion characteristic caused by H₂O are the primary factors.

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ABSTRACT

Oxy-coal combustion produces a combustion environment that contains large amounts of CO_2 , H_2O compared to conventional air combustion. Silica (SiO₂) is a major component of the mineral impurities in coal and the vaporization of silicon containing species controls the initial phase of formation of ultrafine particulate matter (ultrafine PM) via vaporization–condensation mechanism. To investigate the vaporization behavior of silica in wet recycle oxy-coal combustion conditions, synthetic chars with SiO₂ inclusions were burned at 1873 K in the $O_2/CO_2/H_2O$ environments with steam of up to 10 vol.%. Experiments were carried out with a high temperature drop tube furnace (HDTF) system and ultrafine PM was collected with a low pressure impactor (LPI). Meanwhile, modeling work was carried out for further investigation of the effect of H_2O on the vaporization conditions, H_2O in combustion atmosphere significantly enhanced the vaporization of SiO₂ and considerably increased the yield of the ultrafine PM. The variation of char combustion characteristics such as burning temperature and gas properties surrounding the mineral inclusions caused by H_2O seemed to be the primary cause. Especially, effect of H_2 inside the char particle cannot be ignored.

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1. Introduction

Ultrafine particulate matter (ultrafine PM, particles with aerodynamic diameters of <0.3 μ m) is one of the most critical air pollutants in China [1]. A considerable part of the particles is believed to be derived from coal combustion. Ultrafine PM is generally rich in hazardous materials such as heavy metals and polycyclic aromatic hydrocarbons (PAHs), which are seriously harmful to public health. Unfortunately, there is currently no effective technology to control the emissions of ultrafine PM from combustion systems [1,2]. Understanding the formation of ultrafine PM is essential for developing technology for PM emission control.

Si is well known to be one of the major refractory elements in the ultrafine PM emitted from the combustion of coals [1-5]. Moreover, silica (SiO₂) plays an important role in the formation of ultrafine PM, as the condensation of SiO₂ vapor provides the initial nuclei [4,6]. Generally, the vaporization of SiO₂ dominates the initial phase of formation of ultrafine PM via the vaporization-condensation mechanism [4,6]. Therefore, it is of particular importance and has attracted extensive investigation [2,4,7–9]. During the combustion of coal particles, SiO₂ inclusions undergo reduction reactions and vaporize as volatile SiO in the local reducing atmosphere [4,8]. In the early 1980s, Quann [4] systematically investigated the vaporization behavior of refractory minerals by burning various coals in air-combustion conditions on a drop tube furnace (DTF) and proposed a model to describe the reduction reaction of SiO₂ and the transportation of the generated SiO in char pores [10]. They pointed out that combustion



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Nomenclature			
$ \begin{aligned} & \varepsilon \\ & \theta \\ & \rho \\ & \tau \\ & \Phi \\ & a \\ & c \\ & d \\ & f \\ & r \\ & t \end{aligned} $	stefan flow factor porosity volume fraction of mineral inclusions in coal particle density tortuosity thiele modulus reaction activity factor concentration pore diameter vaporization fraction radius burnout time	T V Subscriț a e i k o p m	temperature vaporization rate of each mineral inclusion ot apparent effective initial Knudsen oxygen coal particle mineral inclusions
x A D Ke M P	molar fraction ash content diffusivity equilibrium constant of reaction relative molecular mass partial pressure	Supersc b e s	ript bulk gas equilibrium surface

conditions, especially the combustion atmosphere, have a great impact on the vaporization of SiO₂, which is consistent with the studies by Lee et al. [11] and Sui et al. in our group [12]. Buhre et al. [7] investigated the factors governing the vaporization of silica based on experiments with five bituminous coals, and concluded that the occurrence of silica in coal as well as the char burning temperature significantly affects the vaporization behavior. Because the vaporization processes of SiO₂ and the factors governing vaporization are complicated, the evaporation and related ultrafine PM formation are not fully understood. More fundamental research is still required particularly for those in coal combustion processes involving emerging technologies.

Recently, with the rapid development of oxy-coal combustion $(O_2/CO_2$ combustion) technology, more and more attention is focused on the formation of ash particles in the O₂/CO₂ atmospheres [3,9,13]. The variation of the vaporization of SiO₂ appears to be a significant cause of the change in the ultrafine PM generated from the O_2/CO_2 combustion compared with that from the conventional air combustion [3,9]. Kazanc et al. [3] comprehensively investigated the vaporization of SiO₂ in the O₂/CO₂ combustion condition, based on experiments and a model modified from Quann et al.'s model. They concluded that the vaporization of SiO₂ decreases as the result of the lower char burning temperatures and the change of the gas properties, and their results confirm the reports of Suriyawong et al. [9]. While previous studies on the vaporization of SiO₂ were limited in dry $(O_2/N_2 \text{ or } O_2/CO_2)$ combustion conditions; there have been no studies on the vaporization behavior of SiO₂ in wet oxy-coal (O₂/CO₂/H₂O) combustion conditions. In the wet recycle mode there is a high content of H₂O in addition to CO₂ [13–17], and the effect of H₂O on coal combustion and direct sulfation of limestone cannot be ignored as reported by Hecht et al. [18], Duan et al. [19] and Hu et al. [20]. Therefore, it is essential to clarify the effect of H₂O on the vaporization of SiO₂ and the formation of ultrafine PM in oxy-coal combustion conditions, especially for wet oxy-coal combustion conditions.

In this study, the vaporization behavior of SiO₂ and the formation of ultrafine PM in $O_2/CO_2/H_2O$ environments were studied based on combustion experiments using synthetic chars with SiO₂. Moreover, an improved model that considers the effect of H₂O in the atmosphere to describe the vaporization of SiO₂ was developed based on Quann et al.'s model. The effect of CO₂ and especially H₂O on the vaporization behavior of SiO₂ and the formation of ultrafine PM during char combustion are discussed.

2. Experimental

2.1. Material

Synthetic char containing SiO₂ inclusions was used for combustion experiments. This model material was prepared with furfur alcohol (chemically pure) and SiO₂ powder (5 μ m) with carbon black (20 nm) as a pore former following the procedure of Senior [21]. The proximate and ultimate analyses and heating values are shown in Table 1 and are similar to that of bituminous coal. As reported by Senior et al. [21,22], this model material has combustion characteristics similar to coal, especially in the char burning phase. The ash composition of the char was analyzed with X-ray fluorescence (XRF, EDAX EAGLE III), which is also shown in Table 1. The pore structure was analyzed by N₂ absorption (BET method) (ASAP2020) and mercury penetration (AutoPore IV 9500). The results are listed in Table 2.

Synthetic char is a type of well-defined model material of coals, which has been successfully used in various studies, such as those of char combustion, gaseous pollutant formation and mineral transformation [21,23]. Pulverized synthetic char particles of 45–75 μ m were burned in experiments. It can be seen in Table 1 that the ash content of the synthetic char was 6.7%, and 90.9% of which was SiO₂. The unique composition allows this study to focus on the vaporization behavior of SiO₂ while minimizing interferences from impurities (Na, Al, Ca, etc.). Moreover, the mineral inclusions added to the synthetic char were well controlled, which provided accurate parameters for the modeling work, especially the mineral particle size.

2.2. Combustion conditions

Combustion experiments of the synthetic char were carried out on a high temperature drop tube furnace (HDTF). The HDTF consists of a material feeding system, gas delivery system, high temperature furnace and sampling system, as reported elsewhere in detail [24]. Synthetic char was fed into the furnace at a rate of 0.1 g/min by a SANKI piezo bowl vibratory feeder, and then burned in a simulated atmosphere at a furnace wall temperature of 1873 K. O₂ concentrations in the simulated air combustion (ON21), dry recycle oxy-coal combustion (OC31) and wet recycle oxy-coal combustion (OC31 + 10H₂O) conditions were 21%, 31% and 31% by volume, respectively. In the OC31 + 10H₂O conditions, Download English Version:

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