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# Top-down scaling methodology from the LSTF facility to a three loop PWR plant applied to a SBLOCA event – The ROSA 1.2 test



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#### ABSTRACT

The scaling methodology describes quantitatively the possible differences in the behavior between a reduced size experimental facility and a full scale commercial plant for a determined transient. Then scaling is an essential tool in the design and operation processes of a reduced size facility in order to be able to simulate the behavior of large commercial plants. Since, in this way, it is possible to advance in the development of safety systems, prediction of situations likely to produce accidental sequences, etcetera. Therefore the scaling calculations should be carried out from the earlier stages of the experimental facility conceptual design, so that its experimental data results could be directly extrapolated to a commercial plant. Evidently, the scaling analysis has to be carried out for the experimental test plans, in order to check the capacity to transpose the experimental data of the reduced size facilities to the commercial plants. Consequently, the major objective of the scaling methodology is to evaluate quantitatively the applicability of small size test facility data to predict the behavior of full size commercial plants.

The top-down scaling step of the H2TS scaling methodology, between the LSTF experimental facility and a Pressurized Water Reactor of Siemens-KWU type for the ROSA 1.2 test, has been carried out along this document to evaluate the global system behavior. In order to achieve this main purpose, the general description of both facilities, the transient scenario, and the results of the scaling analysis for a small break loss of coolant accident (SBLOCA) in the hot leg are shown. The scaling analysis methodology used is the top-down global system analysis, from which, it is intended to establish thermal–hydraulic similarity between a scaled facility and a full scale industrial plant. With this aim, the accidental sequence of the ROSA 1.2 test has been divided into its five main time phases, analyzing separately each of them. In each phase the similarity groups ( $\pi$ -monomials and  $\pi$ -monomial groups) have been defined and applied. In such a way that only a reduced number  $\pi$ -monomials are needed to develop the scaling methodology, in addition, many of these similarity groups appear in several phases.

The key aspect of this document is to show the applicability of the top-down scaling analysis methodology to a commercial plant of a different type to that of the reference NPP at which the experimental facility replicates, i.e., test carried out in a Westinghouse type experimental facility, scaling analysis applied to a Siemens-KWU type. In such a way that, it has been proved the possibility to use the measurements made in an experimental facility of different type of the reference plant for an accidental scenario, in particular, applicability of a SBLOCA test data from an experimental facility of type Westinghouse to a commercial plant of type Siemens-KWU.

#### 1. Introduction

Scaling analysis has been traditionally an issue previous to the construction of new nuclear power plants, since its design and construction processes constitutes a very complex technological challenge. Due to the almost unavoidably problem to characterize the whole system performance under the design conditions previous to the plant construction. Then, consequently, the experiments aimed to understand

this behavior are usually performed in small size prototypes. So the scaling methodologies have been traditionally of importance during the design process of these experimental facilities.

Several scaling methods has been developed and used in many technical fields from the 70 s up to nowadays, such the linear scaling, the power/volume scaling, the Ishii's scaling (Bestion, 2016). It was in the 90's when the Hierarchical Two-Tiered Scaling methodology, H2TS, appeared (Zuber, 1991). This methodology is the most widely used in

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| Nomenclature                                |   | f  | liquid phase   |
|---|---|--|--|
|   |   | g  | gas phase  |
| A   | area  | in   | inlet  |
| $D_h$                                       | hydraulic diameter  | 1  | loop   |
| E   | total energy  | LSTF-ROSA ROSA 1.2 test in the LSTF Facility |  |
| f   | friction factor   | m  | two-phase mixture  |
|   | gravity constant  | m-p  | mid-point  |
| g   | • •   | -  | •  |
| G<br>1.                                     | mass flux   | net  | total  |
| h   | enthalpy  | out  | exit   |
| $H_0$                                       | total height  | prz  | pressurizer  |
| k   | form loss coefficients                                    | RCS  | reactor coolant system   |
| $\overrightarrow{k}$                        | unit vector in the z direction                            | sat  | saturation conditions  |
| L   | liquid height   | TSK-PWF                                      | R Siemens-KWU PWR type, three loop 3010 MW <sub>t</sub>        |
| $L_{i}$                                     | length of segment i                                       | Westingh                                     | nouse PWR of Westinghouse type, four loop 3423 MW <sub>t</sub> |
| M   | total mass  |  |  |
| $M_1$                                       | momentum of loop 1  | Superscrip                                   | ots  |
| t   | time  |  |  |
|   | velocity  | *  | dimensionless variable   |
| u   | · · · · · · · · · · · · · · · · · · ·                     |  | mean value   |
| U   | total internal energy                                     |  | variation per unit time t                                      |
| V   | control volume  |  |  |
| m   | mass flow rate  | $\rightarrow$                                | vector   |
| N <sub>nodes</sub>                          | total number of nodes                                     | 4  | _  |
| $\overrightarrow{n}_{\scriptscriptstyle S}$ | unit vector in the mixture velocity direction             | Acronyms                                     | S  |
| p   | pressure  |  |  |
| ġ   | heat transfer   | AIS  | Accumulator Injection System                                   |
| Q   | volumetric flow rate                                      | ATLAS  | Advanced Thermal-hydraulic Test Loop for Accident              |
| Ri  | Richardson number   |  | Simulation   |
| S   | length along the loop                                     | BD   | Blow-Down  |
| t   | time  | ECCS   | Emergency Core Cooling System                                  |
| T   | temperature   | H2TS   | Hierarchical Two Tiered Approach                               |
| u   | fluid velocity  | HPIS   | High Pressure Injection System                                 |
|   | mass flow rate of the gas-steam mixture                   | HQMD   | High Quality Mixture Discharge                                 |
| W <sub>m</sub>                              | <u> </u>  | JAERI  | Japan Atomic Energy Research Institute                         |
| $X_S$                                       | static quality  | LBLOCA                                       |  |
| C   |   | LOCA   | Loss Of Coolant Accident                                       |
| Greek symbols                               |   | LSTF   |  |
|   |   | LWR  | Large Scale Test Facility Light Water Reactor                  |
| α   | void fraction   |  | e e e e e e e e e e e e e e e e e e e                          |
| Δ   | difference (as in $\Delta T$ , difference in temperature) | NC   | Natural Circulation  |
| ε   | stored energy per unit mass                               | NEA  | Nuclear Energy Agency  |
| ф   | phase (1φ single-phase fluid, 2φ two-phase fluid)         | NPP  | Nuclear Power Plant  |
| μ   | specific internal energy                                  | NRC  | Nuclear Regulatory Commission                                  |
| $\Pi_{x}$                                   | π-monomial of a magnitude x                               | OECD   | Organisation for Economic Co-operation and Development         |
| ρ   | density   | PKL  | "Primärkreislauf", primary circuit                             |
| τ   | characteristic time                                       | PRZ  | Pressurizer  |
| ν   | specific volume   | PWR  | Pressurized Water Reactor                                      |
|   | transfer characteristic frequency of a given property     | RCS  | Reactor Coolant System   |
| $\omega_x$                                  | π-monomial group of a property, x, which is changing      | ROSA   | Rig Of Safety Assessment program (carried out in LSTF)         |
| $\Xi_{x,y}$                                 |   | RPV  | Reactor Pressure Vessel  |
| _   | caused by a property, y.                                  | RR   | Reactor Refilling  |
| $\Xi_{x,y,Z}$                               | $\pi$ -monomial group of a property, x, which is changing |  |  |
|   | caused by a property, y, in the facility, Z.              | SBLOCA                                       | Small Break Loss Of Coolant Accident                           |
|   |   | SCRAM  | Safety Control Rod Axe Man                                     |
| Subscript                                   | ts  | SG   | Steam Generator  |
|   |   | TPD  | Two-phase Discharge  |
|   | C   | TD A CE                                      | TDAC/DELAD Advanced Computational Engine (Thornal              |
| 0   | reference   | TRACE  | TRAC/RELAP Advanced Computational Engine (Thermal-             |
| 0<br>bg                                     | reference<br>begin of phase                               | TRACE  | Hydraulic code of the U.S. NRC)                                |

the industry, but over the last decade two new methodologies have been developed, the Fractional Scaling Analyses (FSA) and the Dynamical System Scaling (DSS). The FSA is quite similar to the H2TS methodology, in fact both were developed by Zuber and his coworkers (Zuber et al., 2007), and both methodologies have many similarities. As far as DSS is concerned, say that this approach examines the scale distortions over the transient duration (Reyes, 2015), but due to its

short life it has not been applied to a complex system. All these last three methods are based in the determination of a hierarchical ordering of the phenomena involved in the studied transient.

In general, thermal-hydraulics calculations constitute one of the major points for the safety design analysis of the light water nuclear reactors (LWR's). In particular, the scaling analysis is a very important tool to extrapolate the results obtained in small size test facilities to the

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