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II. Economic assessment for first generation green biorefinery

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ABSTRACT

Green biorefinery (GBR) is an alternative use of grassland biomass. GBR involves applying technology to chemically and physically fractionate (split) biomass such as grass and grass silage to produce marketable products. Three GBR system models were developed in a companion paper to determine, using scenario analysis, the most technically feasible scenario for the development of a blueprint Irish GBR system. The three GBR system models were a combination of feedstock system and biorefinery technology: Grass/silage basic technology (GS), Silage - basic technology (S) and Silage - advanced technology (AT). The models were then assessed at different input volumes. The focus of this paper is on the development of the economic modelling component of the three GBR system models in order to identify which of the previously selected GBR scenarios is the most technically and economically viable to develop a blueprint for a first generation GBR. Six scenarios were assessed in this paper. The GS, S and AT GBR systems, at two input volume rates: medium volume and low volume. Additional scenario analyses were also carried out to investigate two possible production scenarios "No Prot" (fibre product only), and "Prot" (includes proteinaceous secondary product). Both the economic and technical scenario analyses of this paper and its companion paper suggest the most appropriate GBR systems for a first generation Irish blueprint are the combination of Silage feedstock - basic biorefinery technology (S), at the medium input volume and both "Prot" and "No Prot" systems.

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BIOMASS & BIOENERGY

Introduction 1.

1.1. Alternative use of grassland biomass

Grasslands play an important role in global agriculture, covering about 69% of the world's agricultural area [1]. Interest in alternative uses of grasslands has been gaining momentum over the last decade or so, particularly in Europe [2]. Green biorefinery (GBR) is such an alternative use of

grassland biomass. GBR involves applying technology to chemically and physically fractionate (split) biomass such as grass and grass silage [3] into two streams, press cake (the solid fibre fraction) and press juice (the liquid fraction). The press cake can be utilised for products such as insulation materials for building [4]. From the press juice the proteinaceous fraction (proteins, peptides, amino acids) can be extracted for applications such as animal feed or cosmetics. There is also great potential for extracting high value

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NDF

neutral detergent fibre fraction of feedstock

Nomenclature

Nomeno	clature	NDF	neutral detergent fibre fraction of feedstock
а	annum		(kgt ⁻¹ DM)
А	area supplying green biorefinery facility (ha)	NO PRO	Γ production scenario which produces fibre
AD	anaerobic digester		products alone as insulation material
AT	advanced biorefinery technology scenario	NPV	net present value
	ED bipolar membrane electrodialysis	min	minute (60 s)
BT	basic biorefinery technology scenario	ODM	organic dry matter $=$ a term to group compounds
CF	cash flow		such as water soluble components e.g. sugars,
CHP	combined heat and power plant		VFA (butyric acid, acetic acid, propionic acid), as
CP	proteinaceous fraction (e.g. proteins, peptides,		well as the insoluble components fats, oils and
CI	amino acids, nitrate) of feedstock (kg t^{-1} DM)		smaller fibre fractions of the grass/silage
CSO	Central Statistics Office (Ireland)		feedstock (kgt ⁻¹ DM)
		Р	phosphorus fertiliser (kg $ha^{-1}a^{-1}$)
d	distance dependent part of transport costs $(c_1)^{-1} = 1$ (c_2)	PC	press cake – solid fraction of the refined grass or
DI	$(\in \mathrm{km}^{-1} \mathrm{t}^{-1} \mathrm{DM})$		silage feedstock
DM	dry matter	Prot	production scenario which includes a secondary
	ent dry matter fraction (kg t ^{-1} fresh matter)		proteinaceous product as an animal feed
FM	fresh matter	РJ	press juice – liquid fraction of the refined grass or
GBR	green biorefinery		silage feedstock
GS	grass feedstock system – processing grass	Q	feedstock quantity required for the 46 weeks of
	feedstock during summer (4 months) and silage		biorefinery operation (t DM a^{-1})
1.	for the rest of the year	S	silage only system – processing silage feedstock
h	hour hectares		for the 46 weeks of operation
ha HV	high volume input (or throughput) of feedstock	t	tonne (1000 kg)
пv	processed by the green biorefinery (5 t DM h^{-1})	Т	total transport costs (€)
:	interest rate (or discount rate) which reflects the	TS	total solid content of the waste stream (%)
ir	risk associated with the investment (%)	VDS	volatile dry solids (kg t^{-1} DM). It is the volatile
IRR	the ir which results in an NPV $= 0$		solids expressed as a fraction of the stillage
K	potassium fertiliser (kg ha ^{-1} a ^{-1})		DM. It is the collective term for the organic matter
ĸ kWh	kilowatt hour		in the sample (minus ash), that is readily used
kWn kWe	kilowatts of electrical energy		during anaerobic digestion
kvv _e L	distance independent part of transport costs for	UF	ultra filtration membrane purification technology
Г	unloading ($\in t^{-1}$ DM feedstock/ $\in t^{-1}$ slurry)		in AT scenarios
LV	low volume input (or throughput) of feedstock	UASB	upwards flow anaerobic sludge blanket reactor
LV	processed by the green biorefinery (0.2 t DM h^{-1})	W (mK)⁻	$^{-1}$ watts per m K – indication of insulation
LA	lactic acid fraction of silage feedstock		properties
LA MJ	mega joules (1×10^6 J)	Х	radius of the catchment area (km)
M) MV	medium volume input (or throughput) of	X	average haul distance to the biorefinery
101 V	feedstock processed by the green biorefinery		facility (km)
	$(0.8 \text{ t DM h}^{-1})$	Y	average grass yields of the catchment area
N	nitrogen fertiliser (kg ha ^{-1} a ^{-1})		$(t DM ha^{-1} a^{-1})$
	plant available nitrogen in waste slurries	τ	tortuosity factor, the relationship between the
N-NH4	returned to fields supplying the green biorefinery		actual transport distance and the direct distance
	facility (kg ha ^{-1} a ^{-1})	η	electrical efficiency of the CHP unit (%)
	acincy (sgila a)		

biochemicals such as lactic acid, which can be used as a building block for plastic production (polylactic acid (PLA)). After extracting the desired fractions from the biomass the residual grass or silage slurries ('stillage') can then be fed into an anaerobic digester to produce biomethane gas, which is converted into electricity and heat [5].

1.2. Key factors for developing a GBR blueprint for Irish grasslands

A "Blueprint for an Irish GBR" has been proposed by O'Keeffe et al. [6], producing insulation materials from the grass fibre

fraction and a proteinaceous product for animal feed from the grass juice fraction. Three GBR system models have been developed to generate scenarios to enable the selection of the most technically feasible Irish GBR scenario and are outlined in a companion paper [7]. The key factors identified for determining the most suitable GBR scenario were investigated. These include:

 Viable feedstock system – grass/silage (GS) or silage only (S): The GS system processed grass during the summer (4 months) and silage for the remainder of the year. The S system used silage only as the feedstock for the complete annual production [4,8]. Download English Version:

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