



# Recovery of volatile fatty acids from fermentation of sewage sludge in municipal wastewater treatment plants



S. Longo<sup>a</sup>, E. Katsou<sup>a</sup>, S. Malamis<sup>a,\*</sup>, N. Frison<sup>b</sup>, D. Renzi<sup>c</sup>, F. Fatone<sup>a</sup>

<sup>a</sup>Department of Biotechnology, University of Verona, Strada Le Grazie 15, 37134 Verona, Italy

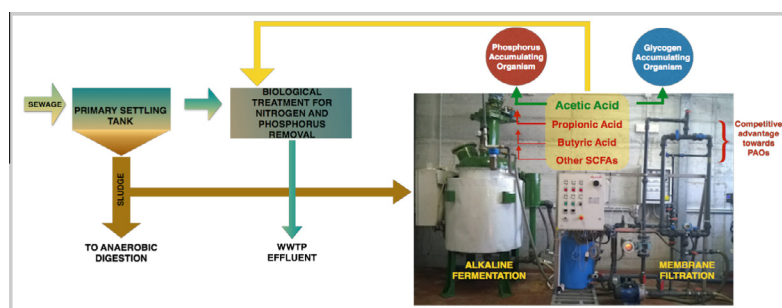
<sup>b</sup>Department of Environmental Sciences, Informatics and Statistics, University Ca' Foscari of Venice, Dorsoduro 2137, 30121 Venice, Italy

<sup>c</sup>Alto Trevigiano Servizi srl, Via Schiavonesca Priula 86, 31044 Montebelluna, Italy

## HIGHLIGHTS

- Wollastonite use during fermentation resulted in low nutrient release in the liquid.
- Higher SCFAs in the liquid phase with the use of caustic soda.
- Wollastonite enhanced the sludge dewatering characteristics and filterability.
- Fermentation liquid improved nutrient removal rates compared to acetic acid.

## GRAPHICAL ABSTRACT



## ARTICLE INFO

### Article history:

Received 24 July 2014

Received in revised form 19 September 2014

Accepted 20 September 2014

Available online 6 October 2014

### Keywords:

Sludge alkaline fermentation  
Short chain fatty acids  
Membrane filtration  
Wollastonite  
Nutrient removal

## ABSTRACT

This work investigated the pilot scale production of short chain fatty acids (SCFAs) from sewage sludge through alkaline fermentation and the subsequent membrane filtration. Furthermore, the impact of the fermentation liquid on nutrient bioremoval was examined. The addition of wollastonite in the fermenter to buffer the pH affected the composition of the carbon source produced during fermentation, resulting in higher COD/NH<sub>4</sub>-N and COD/PO<sub>4</sub>-P ratios in the liquid phase and higher content of propionic acid. The addition of wollastonite decreased the capillary suction time (CST) and the time to filter (TTF), resulting in favorable dewatering characteristics. The sludge dewatering characteristics and the separation process were adversely affected from the use of caustic soda. When wollastonite was added, the permeate flux increased by 32%, compared to the use of caustic soda. When fermentation liquid was added as carbon source for nutrient removal, higher removal rates were obtained compared to the use of acetic acid.

© 2014 Elsevier Ltd. All rights reserved.

## 1. Introduction

Wastewater facilities are increasingly required to implement treatment process improvements to meet stricter discharge limits

\* Corresponding author.

E-mail addresses: [stefano.longo@univr.it](mailto:stefano.longo@univr.it) (S. Longo), [ekatsou@yahoo.com](mailto:ekatsou@yahoo.com) (E. Katsou), [malamis.simos@gmail.com](mailto:malamis.simos@gmail.com) (S. Malamis), [nicolafrison85@gmail.com](mailto:nicolafrison85@gmail.com) (N. Frison), [drenzi@altotrevigianoservizi.it](mailto:drenzi@altotrevigianoservizi.it) (D. Renzi), [francesco.fatone@univr.it](mailto:francesco.fatone@univr.it) (F. Fatone).

<http://dx.doi.org/10.1016/j.biortech.2014.09.107>

0960-8524/© 2014 Elsevier Ltd. All rights reserved.

with respect to nutrients and at the same time want to maintain low operating expenses. Often commercially available organic carbon sources are used in wastewater treatment plants (WWTPs) for biological nutrient removal (BNR) from wastewater. However, the price of commercial synthetic carbon sources has significantly increased over the last years. Therefore, the use of non-conventional carbon sources seems to be an appealing alternative, considering their lower greenhouse gas (GHG) footprint compared to conventional ones. Fermenting sludge to produce short chain fatty acids (SCFAs) that can then be used in the subsequent BNR process

## Nomenclature

BNR	biological nutrient removal	soda-SFL	sludge fermentation liquid in which caustic soda is added
COD	chemical oxygen demand	sPRR	specific phosphorus release rate
CST	capillary suction time	sPUR	specific phosphorus uptake rate
DNBPR	denitrifying via nitrite biological phosphorus removal	SRT	solids retention time
FL	fermentation liquid	TMP	transmembrane pressure
GHG	greenhouse gas	TN	total nitrogen
HAc	Acetic acid	TP	total phosphorus
Hi-But	Iso-Butyric acid	TS	total solids
Hn-But	n-Butyric acid	TSS	total suspended solids
HPr	Propionic acid	TTF	time to filter
HRT	hydraulic retention time	TVS	total volatile solids
Hi-Va	Iso-Valeric acid	UF	ultrafiltration
Hn-Va	n-Valeric acid	VFA	volatile fatty acid
OFMSW	organic fraction of municipal solid waste	VSS	volatile suspended solids
OLR	organic loading rate	WAS	waste activated sludge
S/L	solid/liquid	W	wollastonite
SCFA	short chain fatty acid	W-SFL	sludge fermentation liquid where wollastonite has been added
sCOD	soluble COD	WWTP	wastewater treatment plant
SF	sludge fermentation		
SFL	sludge fermentation liquid		
sNUR	specific nitrogen uptake rate		

seems to be a sustainable process, having the additional advantage of decreasing the amount of sludge to be disposed (Li et al., 2011; Tong and Chen, 2007; Ucisik and Henze, 2008; Zheng et al., 2010). Recovering SCFAs from sewage sludge is currently a challenge in WWTPs. Depending on process conditions of the sewage sludge fermentation, the concentration of SCFAs can be satisfactory (i.e. >2 g/L), with favorable proportions of acids for the subsequent BNR process (i.e. ~40% acetic acid (HAc), ~15% propionic acid (HPr), ~25% butyric acid (HBut)) (Jiang et al., 2009; Lee et al., 2014; Li et al., 2011). The results of recent studies have shown that the use of sludge fermentation liquid (SFL) decreases the production of nitrous oxide (N<sub>2</sub>O) and nitric oxide (NO) during the BNR processes accomplished via the nitrite pathway (Zhu and Chen, 2011). Despite the extensive work on sludge fermentation, there is still a gap of knowledge about how process parameters (i.e. pH, temperature, solids retention time (SRT), hydraulic retention time (HRT)) can affect the efficiency of sludge fermentation in terms of the composition and the quantity of SCFAs. Most applications of waste-derived SCFAs still remain at laboratory scale (Lee et al., 2014). To ascertain the transferability of the process from the laboratory to the market, pilot scale studies are also required.

The pH is an important factor that controls the hydrolysis and acidification during sewage sludge fermentation. Alkaline conditions are expected to lead to more soluble protein and carbohydrate generation. At the same time, the methanogenic activity is inhibited resulting in enhanced SCFAs production (Wu et al., 2009). The optimum pH has been found to be in the range of 9–11 and can be maintained with the use NaOH and Ca(OH)<sub>2</sub> (Su et al., 2013; Wu et al., 2009). However, this practice is not desirable in full-scale plants, since it increases the cost and the environmental impact of the process. The addition of alkaline silicate minerals to control the pH can increase the sustainability of the fermentation process. The economic evaluation concerning the use of biowaste derived external carbon sources revealed that the organic fraction of municipal solid waste (OFMSW) fermentation liquid (FL) is a less expensive option compared to the use of synthetic HAc for the treatment of high strength nitrogenous effluents (Katsou et al., 2014). Considering the complex physicochemical nature of fermented effluents, the separation of SCFAs from fermented sludge is not a straightforward process. There are very

few studies examining the solid/liquid (S/L) separation of fermented effluents. The effective and straightforward separation of FL from the fermented sludge can enhance the sustainability of the process and can lead to reduced production of wet sludge. In previous studies, the sludge dewatering ability was negatively affected by the use of caustic soda due to the release of Na<sup>+</sup>, which impaired the separation of the FL from the fermented sludge (Su et al., 2013). One commonly applied technique for S/L separation is filtration. Nevertheless, membrane filtration is energy demanding, which limits its applications (Zhang et al., 2009). S/L separation is not always effective and the deteriorated filtration capability of the sludge makes the conventional sludge dewatering methods not practical (Tong and Chen, 2007; Yuan et al., 2006).

Within this context, the application of an efficient separation method based on membrane filtration is examined, aiming at the optimization of the whole treatment scheme. Membrane technology has been studied for the separation, isolation, recovery and utilization of volatile fatty acids (VFAs) (Zacharof and Lovitt, 2012). Membrane filtration is expected to allow the selective separation and retain the VFAs within the liquid stream, while rejecting the suspended solids. To apply this technology effectively, pretreatment of the fermented effluent is necessary since membrane fouling can be the major operational deficiency limiting the wider adoption of the process for the S/L separation.

This work studied the integration of the sewage sludge fermentation–membrane separation (SF–MS) process in order to recover SCFAs from sewage sludge and subsequently use them for nutrient bioremoval in a WWTP. The use of a suitable alkaline silicate mineral (wollastonite) was studied to enhance the performance of the fermentation process and the subsequent S/L separation stage. Finally, the feasibility of using the SFL as carbon source for enhanced BNR was assessed.

## 2. Methods

### 2.1. Source of sewage sludge and reasons for wollastonite selection

The sewage sludge used for the fermentation experiments was collected from the municipal WWTP of Carbonera (Veneto Region,

Download English Version:

<https://daneshyari.com/en/article/680278>

Download Persian Version:

<https://daneshyari.com/article/680278>

[Daneshyari.com](https://daneshyari.com)