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# Optimization of crystal growth of sub-micron ZSM-5 zeolite prepared by using Al(OH)<sub>3</sub> extracted from fly ash as an aluminum source



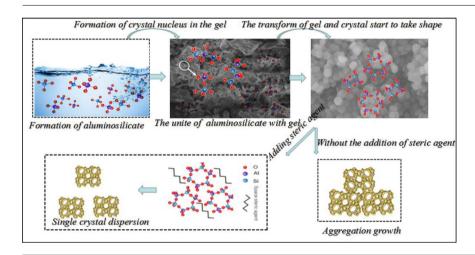
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#### HIGHLIGHTS

- A novel approach was proposed to prepare ZSM-5 zeolite by using Al(OH)3 extracted from fly ash, as an aluminum source.
- The variations of crystallization curves for ZSM-5 growth under different hydrothermal conditions were investigated.
- The formation of ZSM-5 crystal was investigated.
- Growth process regulation of ZSM-5 was discussed under the effect of organic steric hindrance agents.

#### GRAPHICAL ABSTRACT



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#### ABSTRACT

A novel approach was proposed to prepare ZSM-5 zeolite via hydrothermal synthesis by using Al(OH)<sub>3</sub>, which was extracted from fly ash by a staged treatment, as an aluminum source. The synthesis parameters and crystal growth of ZSM-5 were optimized. The optimization of crystal growth for ZSM-5 was investigated under the effect of organic steric-hindrance agents. The crystal phase and morphology of the ZSM-5 were characterized by X-ray diffractometry and scanning electron microscopy, and the particle size distribution was measured by laser particle-size analyzer. The crystal growth of ZSM-5 under different hydrothermal conditions obeyed the "S" regulation. According to the analysis, the formation of ZSM-5 crystal occurred via four steps: (1) the formation of amorphous aluminosilicate by the condensation of silicate ions and aluminate ions; (2) the particle growth and aggregation of the amorphous aluminosilicate; (3) crystallization and crystal growth of ZSM-5; (4) Gentle growth after the zeolite crystal reaches a certain size. The addition of organic steric hindrance agents resulted in a decrease in grain size and crystal-particle formation with a narrow size distribution. Single-grain dispersion resulted and the micropore volume, mesopore volume, and specific surface areas were improved by the presence of organic steric agents.

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**Table 1** Chemical composition of raw CFA.

| Composition | SiO <sub>2</sub> | $Al_2O_3$ | Fe <sub>2</sub> O <sub>3</sub> | TiO <sub>2</sub> | CaO  | MgO | K <sub>2</sub> O | Na <sub>2</sub> O | MnO <sub>2</sub> | P <sub>2</sub> O <sub>5</sub> | LOI |
|-------------|------------------|-----------|--------------------------------|------------------|------|-----|------------------|-------------------|------------------|-------------------------------|-----|
| wt.%        | 51.44            | 30.91     | 6.76                           | 0.53             | 3.54 | 1   | 0.8              | 0.54              | 0.16             | 0.22                          | 4.1 |

(LOI = loss on ignition).

#### 1. Introduction

Coal fly ash (CFA) is an industrial solid waste that is generated during coal combustion and transformation, and resulting in serious pollution. According to statistics, CFA from coal combustion exceeded  $5.8 \times 10^8$  metric tons in 2014 [1], and has become the largest solid-waste resource. The large amount of CFA deposition occupies infield, contaminates water resources and the atmosphere, and is harmful to human health. Unfortunately, only  $\sim 50\%$  CFA is used. Because of its compositional similarity to volcanic materials with high SiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub> contents, CFA is an ideal raw material for zeolite production. Bukhari et al. described the efficient conversion of CFA to zeolites such as ZSM-5 [2]. Na-A zeolite [3], Na-X zeolite [4,5], Na-P zeolite [6–8] and MCM zeolites [9] are produced using fly ash as a raw material, and zeolites are used widely for the purification of pollutant water and refining of oil products and chemicals of catalytic synthesis.

ZSM-5 zeolites were extended infinitely as three-dimensional crystalline aluminosilicates with corner-sharing  $[AlO_4]^{5-}$  and  $[SiO_4]^{4-}$  tetrahedra that form frameworks with a high  $SiO_2/Al_2O_3$  ratio [10]. They have been used mainly in practical applications, such as catalyst carriers in the petroleum refining industry [11,12], and for separating and extracting organic compounds in water for environmental protection in water purification because of their favorable adsorption performance [13,14]. Therefore, the preparation of zeolites with a smaller grain size and the reduction of production costs are two issues of crucial importance for industrial applications. It is of vital importance to reduce costs to contrast with the high-cost chemical raw materials of silica and aluminum salts.

We selected CFA as a source of aluminum components by activation and separation to synthesize ZSM-5 zeolite via hydrothermal synthesis. The process parameters for the synthesis (crystallization temperature, crystallization time, water–silica ratio) and the crystal growth of ZSM-5 zeolite were optimized. The influences of organic steric-hindrance agents on the grain growth of ZSM-5 zeolite were investigated. The crystal phase and morphology of the ZSM-5 zeolite was characterized by X-ray diffractometry (XRD) and

scanning electron microscopy (SEM). The specific surface area and pore volume were measured by Brunauer–Emmett–Teller (BET) and the particle size distribution (PSD) was determined by laser particle analyzer. The results provide a theoretical basis for a new approach to fly ash utilization — the synthesis of ZSM-5 zeolites with Al(OH)<sub>3</sub> as an aluminum resource as extracted from fly ash.

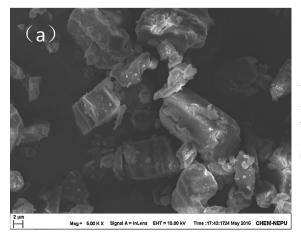
#### 2. Experimental section

The chemical composition of CFA is provided in Table 1. Tetrapropylammonium hydroxide (TPAOH, 25% aqueous solution) was from Kente Chemical Ltd., Zhejiang Province, China. Tetraethoxysilane (TEOS) was from Damao Chemical Ltd., Tianjin City, China. Ethanol, polyethylene glycol (PEG), polyvinylpyrrolidone (PVP), triethanolamine (TEA) and sodium hydroxide from Bomao Chemical Ltd., Shandong Province, China, were commercial analytical grade reagents.

The CFA samples were calcined at  $800\,^{\circ}\text{C}$  to remove unburned carbon, washed with deionized water to remove soluble impurities and dried at  $120\,^{\circ}\text{C}$  for  $12\,\text{h}$ . To increase the leaching efficiency of the silicon and aluminum compounds and the utilization of CFA, a dried sample ( $10\,\text{g}$ ) was mixed with  $Na_2CO_3$  powder (Waco;  $97\,\text{wt.\%}\,Na_2CO_3$ ) at a mass ratio of CFA:  $Na_2CO_3 = 1:1.5$  and calcined at  $840\,^{\circ}\text{C}$  for  $4\,\text{h}$ .

The above powder was mixed with  $3\,\text{mol}\,\text{L}^{-1}$  HCl in a mass/volume ratio of powder:HCl=1:10 g mL<sup>-1</sup> and aged for 2 h at 80 °C with stirring at 250 rpm. The solution was centrifuged to separate the silica gel and AlCl<sub>3</sub> solution that contained impurities. By adjusting the pH of the AlCl<sub>3</sub> solution with 6 wt.% NaOH solution to pH=3.8, we make sure that all iron ions were converted to Fe(OH)<sub>3</sub> and removed by centrifugation to obtain NaAlO<sub>2</sub>. Continuous CO<sub>2</sub> was inlet to yield Al(OH)<sub>3</sub>, and Na<sub>2</sub>CO<sub>3</sub> can be obtained and recycled. The SEM image and XRD pattern of the Al(OH)<sub>3</sub> samples as extracted from the fly ash is shown in Fig. 1.

The alcohol and TPAOH were diluted with deionized water with stirring at 300 rpm at  $50 \,^{\circ}$ C for 1 h. The quantity of deionized water depended on the different  $H_2O/SiO_2$  ratios. The TEOS was added



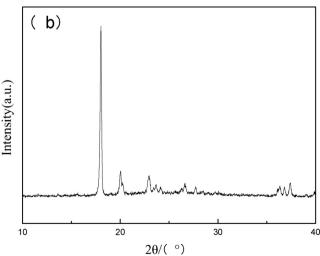


Fig. 1. The SEM image(a) and XRD pattern(b) of Al(OH)<sub>3</sub> samples.

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