



Colloids and Surfaces A

journal homepage: www.elsevier.com/locate/colsurfa

Micellization and adsorption modeling of single and mixed nonionic surfactants



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G R A P H I C A L A B S T R A C T



ARTICLE INFO

Keywords: Micelle Aggregation number Surface tension Nonionic surfactants Isothermal titration calorimetry

ABSTRACT

The surface tension and heats of dilution of aqueous solutions of octyl- β -p-glucopyranoside (C₈G₁), tetraethylene glycol monooctyl ether (C₈E₅) and C₈E₅-C₈G₁ mixtures at 298.2 K were studied by tensiometry (ST) and isothermal titration calorimetry (ITC). Single surfactant micelle formation and growth were modeled using a multiple chemical equilibrium approach under the assumption that micelles are sphero-cylinders that can be thermodynamically described by three parameters, namely spherical and cylindrical contributions to the micelle molar Gibbs energy and the enthalpy of micellization. The two-dimensional virial equation of state was employed to correlate the surface tensions, which required two additional parameters: a 2D second virial coefficient and a reference monomer concentration. For the binary surfactant solutions, combining and mixing rules were suggested with no further parameters. For the single surfactants, the model correlated very well both ITC and ST experimental data. For mixed surfactants, ST data were also very well predicted, but this was not the case for ITC data. For the critical micelle concentrations, the model enthalpograms presented both positive and negative deviations from the experimental results, depending on the surfactant relative concentrations. Very low C₈G₁ concentrations promoted the demicellization of Small aggregates.

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https://doi.org/10.1016/j.colsurfa.2018.08.005

Received 26 June 2018; Received in revised form 1 August 2018; Accepted 2 August 2018 Available online 06 August 2018 0927-7757/ © 2018 Elsevier B.V. All rights reserved.

M. Medeiros et al.

List of symbols				calorimetry step
			R	gas constant
	A	surface area	r	intermolecular distance
1	b, b _i	2D second virial coefficient for mixtures and for substance	r_i	hydrophilic head hard-disk radius of surfactant i
		i, respectively	S	entropy
1	b_{AB}	2D cross second virial coefficient for amphiphiles A-B in-	S_A	monomeric form of surfactant A
		teractions	\overline{S}	micelle weight-average aggregation number
i	F	Helmholtz energy	Т	absolute temperature
i	F_{ITC}, F_{ST}	objective function for ITC and ST curve fitting, respec-	u _{ii}	tail-tail intermolecular energy
		tively	ν	aggregation number variance
2	g_A^0	molar Gibbs energy of free amphiphile A	x_A	free monomer mole fraction of amphiphile A
2	3a gb	micellization parameters defined in Eq. (6)	x_s	mole fraction of s sized micelles
2	Scyl	molar Gibbs energy contribution from amphiphiles in the	$x_{s\beta}$	mole fraction of <i>s</i> sized micelles with composition β
		cylindrical body	x_i^{∞}	free monomer concentration of substance i when the sur-
2	3sp	molar Gibbs energy contribution from amphiphiles in the		face pressure is $\Pi \infty$
		spherical end caps	у	variable defined in Eq. (9)
1	g_s^0	molar Gibbs energy of micelle of size s	z	total surfactant concentration
2	$S_{s\beta}^{0}$	molar Gibbs energy of micelle of size s and composition $\boldsymbol{\beta}$		
4	Δg_s^0	standard molar Gibbs energy of micellization of s sized micelle	Greek	
	$\Delta g^0_{c\beta}$	standard molar Gibbs energy of micellization of s sized	α	bulk mole fraction of surfactant A
	Сзр	micelle with composition β	β	micelle composition
i	H	enthalpy	β	average micelle composition
1	h_A^0	molar enthalpy of free amphiphile A	γ	surface tension
1	$h_{s\beta}^0$	molar enthalpy of micelle of size s and composition β	η_i	surface excess of substance i
4	Δh_A^0	standard molar enthalpy of micellization of surfactant A	μ_i	chemical potential of specie i
4	$\Delta h_{s\beta}^0$	standard molar enthalpy of micellization of s sized micelle	μ_i^{∞}	chemical potential of specie <i>i</i> in the reference diluted so-
		with composition β		lution
i	$K_{a,} K_{b}$	equilibrium constants defined in Eq. (8)	$\Delta_{ads}\mu_i$	molar Gibbs energy of adsorption of substance i, defined in
i	Ks	equilibrium constant for s sized micelle formation		Eq. (45)
j	K _{sβ}	equilibrium constant for s sized micelle formation with	П	surface pressure
		composition β	Π^{∞}	reference surface pressure, 0.01 mN.m^{-1}
1	n	numberof amphiphiles in micelle spherical end cap	Ω	vector of adjustable parameters
1	M_s	micelle with <i>s</i> amphiphiles	σ	standard deviation of a measurement
1	$M_{s\beta}$	micelle with <i>s</i> amphiphiles and composition β	ξ_A	surface mole fraction of amphiphile A
1	N_w, N_s	number of moles of water and surfactant, respectively		
	0. a	heat and molar heat absorbed in isothermal titration		

1. Introduction

Surfactants are used as individual components in aqueous solution or in other solvents in only a few cases in many applications and in industrial practice. In most cases, they are employed as mixtures of two or more surfactants. For example, in the case of emulsifiers, it is known that two emulsifiers operate better than one. In liquid detergents, personal care preparations and other applications, it is common to find more than one surfactant in commercial formulations. In the field of pharmacy, improved oil recovery and the production of water-based paints require mixtures of surfactants to reach emulsification, wetting and dispersion. In general, the industrial and biological use of surfactants corresponds to mixtures of amphiphiles [1,2], their individual use being scarce. Thus, the prediction of the properties of surfactant mixtures is crucial for the determination of the optimum composition to meet the application requirements.

Usually, when experimental data are available, the mass action law with one chemical equilibrium reaction is employed to correlate the measurements and to describe the thermodynamics behind micelle formation [2–4]. For single surfactant solutions, this model assumes that the micelle size distribution is monodisperse. Accordingly, this approach cannot explain the experimentally observed micelle growth, because it assumes that all formed micelles have the same aggregation number. Nevertheless, it relates the Gibbs energy of micellization (normally, an adjustable parameter of the model) to the critical micelle concentration (cmc), i.e., the concentration when a sudden change of an observable property occurs. The extension of this model to describe mixed surfactant micellization is not straightforward; it requires the aggregation number of mixed micelles which is not a trivial function of the pure surfactant micelle sizes. For surfactant mixtures, the cmc and micelle composition can be estimated by the pseudo-phase separation model of Holland and Rubingh [5] which considers micelles as a macroscopic phase in equilibrium with the free monomers solution; the amphiphiles activity coefficients in the micelles is described by the regular solution theory. This model has one binary parameter for nonideal mixing. However, as in the monodisperse mass action law, the pseudo-phase model does not allow for the estimation of micelle size distributions; a pseudo-phase is equivalent to micelles with infinite aggregation numbers. In the lack of experimental information, the molecular thermodynamic theories of Puvvada and Blankschtein [6] and of Nagarajan and Ruckenstein [7] provide a methodology to estimate the micellization Gibbs energy. In these predictive models, the micelle size distribution is considered, and it is consistent with the multiple chemical equilibrium approach. The required equilibrium constants are estimated from the geometrical and molecular characteristics of the amphiphiles. On the other hand, for low surface coverage, air-liquid surface tension (ST) data can be correlated by many two-dimensional gas-like equations of state (SEoS). It is known that ST data can be easily correlated by several SEoSs with two or three adjustable parameters [8]. For mixed surfactant monolayers, however, it is very important to have a solid theoretical ground for the mixing and combining rules to estimate mixed surface parameters from the single

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