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Authors: Qingjun Zhang, Meiling Liu, Chenxiaodong Li, Aiwu Zeng

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Design and control of extractive distillation process for separation of the minimum-boiling azeotrope ethyl-acetate and ethanol

Qingjun Zhang¹, Meiling Liu³, Chenxiaodong Li¹, Aiwu Zeng^{1, 2,*}

1 State Key Laboratory of Chemical Engineering, Tianjin University, School of Chemical Engineering and Technology, Tianjin 30072, P.R. China.

2 Collaborative Innovation Center of Chemical Science and Engineering (Tianjin).

3. College of Chemical and Environmental Engineering, Shandong University of Science and Technology, Qingdao 266590, P.R. China.

*Corresponding author: E-mail: awzeng@tju.edu.cn (A. Zeng).

Graphical Abstract

Separation of Azeotrope Ethyl Acetate-Ethanol by Extractive Distillation

Step 1: Entrainer Ranking or Screening (iso-and equi-volatility curves, minimum trade-off curves, TAC)

Step 2: Steady-state simulation and optimization (Sequential iterative optimization methods: Min TAC)

> Step 3: Heat integration simulation B₁-E alternative

Step 4: Dynamic simulation of conventional process Single-end control strategy with the feedforward strategy of the mass flowrate ratio reflux-to-feed

Step 5: Dynamic simulation of heat-integrated case Bypassing portion hot stream around the economizers with the dual-point temperature control strategy

Highlight:

- \bigstar 1. The capable solvent is screened by the IECs, minimum-tradeoff curves and TAC.
- \bigstar 2. The three evaluation indicators are employed to rank the different configurations.
- \bigstar 3. The application of exergy loss analysis represents the thermodynamic efficiency.
- \bigstar 4. The simple types of heat integration (B₁-E, F-B₁-E) are investigated.
- \star 5. A new control scheme of bypassing stream with dual-temperature strategy is devised.

Abstract: Design and control of extractive distillation process is explored by taking the separation of minimum-boiling azeotrope ethyl-acetate and ethanol as an example. The two evaluation indicators of second-law efficiency and CO_2 emissions are employed to evaluate different alternatives, which consist of conventional case, F-E process (hot solvent stream to preheat fresh feed of extractive column), B₁-E process (hot solvent stream to preheat feed of recovery column), and F-B₁-E process (hot solvent stream to preheat feed of extractive case can

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