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# Representative Domain Size for the Simulation of Coalescence Filtration in Nonwoven and Foam Media

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## Abstract

Pore-scale filtration simulations require high spatio-temporal resolutions and significant computational effort, hence, keeping the domain size to a minimum is desirable. Previous studies have considered domains based on Brinkman length, or are limited by computing power, and little information is available for conditions involving high fluid saturation – typical of steady state mist filtration. In this study, simulations are performed to characterize the effect of domain size on pressure drop, residual saturation, liquid film thickness and interfacial area concentration, using virtual nonwoven and foam filters with similar micro-structural properties. Further, experiments using micro-CT are performed to validate the present computational simulations. It is found that two phase flow through filters are more sensitive to local geometric variations or mesh resolution in the porous media than single phase flow. Statistical uncertainties in the steady state quantities of less than  $\pm 10\%$  can be expected to cope with the increase in computing power required for practical mesh sizes. A computational domain size of about  $50-100 \times d$  (where  $d$  is the strut or fibre diameter) was found to be required for CFD for the operating conditions considered.

**Keywords** : saturation, filtration, foam, fibre, CFD, domain size

## Nomenclature

$A_f$	specific filter surface area, $m^{-1}$	<i>Symbols</i>	
$A_{ic}$	interfacial area concentration, $m^{-1}$	$\alpha$	packing density, –
$C_{Br}$	multiplication factor, –	$\beta$	fibre orientation angle, $^\circ$
$d$	diameter of the filter elements, m	$\varepsilon$	liquid volume fraction, –
Eu	Euler number, –	$\kappa$	permeability, $m^2$
$l$	filter thickness (or depth), m	$\lambda$	oil film thickness, m
$p$	pressure, Pa	$\mu$	dynamic viscosity, Pa-s
Re	Reynolds number, –	$\xi$	oil centre of mass in the filter, m
$S$	oil saturation, –	$\rho$	density, $kg/m^3$
$u$	velocity, m/s	$\theta$	contact angle, $^\circ$
$w$	width (cross-section) of the filter, m	$\psi_p$	polydispersity foam, –
$x, y, z$	lengths along the coordinate axes, m		

## 1 Introduction

Several natural and anthropogenic processes including industrial gas compression, oil and gas production and distribution, lubricated manufacturing and in engine crank-cases produce liquid mists that are either valuable products or undesirable byproducts which may need to be recovered. Recovery of such mists for reuse or treatment is typically accomplished through coalescence filtration, employing highly porous fibrous (nonwoven) [1], knitted stainless steel [2] or foam [3] filter media, which are regarded to provide high filtration efficiencies and low pressure

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