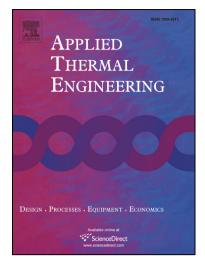
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Numerical investigation on effects of using segmented and helical tube fins on thermal performance and efficiency of a shell and tube heat exchanger

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Numerical investigation on effects of using segmented and helical tube fins on thermal performance and efficiency of a shell and tube heat exchanger

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Abstract: Thermal performance of a shell-and-tube heat exchanger is investigated numerically using ANSYS FLUENT software under various conditions. Before proceeding with simulations, sensitivity analysis is performed for both mesh grid and turbulence model and the results are compared and validated with results obtained from Bell-Delaware method. The numerical study is consisted of three parts: First the effect of tubes wall relative roughness and Reynolds number on total heat transfer and pressure drop is investigated. In the second part, effect of simple segmented tube fins on heat transfer is studied under two independent adjustable parameters, namely fin pitch and fin height while surface roughness is fixed. Finally, a novel design of fins (helical fin) is proposed and its influence on thermal performance of the heat exchanger is investigated and results are compared to no-fin and segmented fin configurations. It is found that tube fins in general enhance overall efficiency of the heat exchanger. The efficiency is increased by 9.5% and 6% when the proposed helical fins and segmented fins are used respectively. CFD results purpose the efficiency is increased by increasing fin height, but decreased by increasing fin pitch. Helical fins increase effectiveness of heat exchanger by 17% compared to plain tubes. Although increasing surface roughness increases the efficiency, it leads to faster corrosion which means higher maintenance costs and is not desirable. The efficiency of the heat exchanger therefore can be prominently increased when combination of low surface roughness and helical fins with smaller pitch and larger height are used.

Nomenclature

- B Central baffle spacing (mm)
- B_c Baffle cut (%)
- D_s Shell size (mm)
- d Distance from the wall for near wall Treatment (m)
- $d_o \qquad \text{Tube outer diameter (mm)}$
- g Gravitational acceleration (m/s²)
- T_h Hot fluid temperature (K)
- T_c Cold fluid temperature (K)
- Gb Generation of turbulence due to buoyancy
- Gk Production of turbulence kinetic energy due to mean velocity gradients
- *k* Kinetic energy of turbulent fluctuations per unit mass (m^2/s^2)
- K Thermal conductivity (W/mK)
- A Heat exchanger total tube area (m²)
- L Heat exchanger length (mm)
- N_b Number of baffles

- S Scalar measure of the deformation tensor
- S_{\perp} User defined source terms of transport equation
- T Temperature (K)
- u, v, w Velocity components (m/s)
 - \vec{V} Velocity Vector
- x, y, z Position coordinates
- U Heat transfer coefficient (W/m²)

Greek symbols

 ϵ Viscous dissipation rate (m²/s³)

- Φ Dissipation function
- v Dynamic viscosity (Pa s)
- ξ Heat exchanger effectiveness
- v_t Turbulent viscosity (Pa s)
- μ Molecular viscosity (m²/s)

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