



## Research Paper

## Developing a performance correlation for counter-flow regenerative indirect evaporative heat exchangers with experimental validation

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## HIGHLIGHTS

- The performance correlation for counter-flow regenerative IEHX is developed.
- Three dimensionless groups are identified to evaluate the thermal performance.
- The empirical constants are determined via data-fitting from simulation results.
- Experimental study is conducted to validate the developed correlation.

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## ABSTRACT

The present article aims to determine a minimum parametric representation for evaluating the thermal performance of a counter-flow regenerative IEHX (indirect evaporative heat exchanger). Three dimensionless groups have been identified in order to develop a performance correlation based on non-dimensional forms of the governing equations. Numerical simulations were carried out to determine the empirical constants of the correlation by fitting the simulated dimensionless outlet temperature as a function of each dimensionless group. Simulations have been conducted by changing the value of each dimensionless group while keeping a constant value for other parameters. The simulated dimensionless outlet temperature was varied from 0.20 to 0.73. A prototype of a counter-flow regenerative IEHX was designed and experimentally studied. The correlation was validated by comparing the calculated results with experimental findings as well as published experimental data acquired from literature. The developed correlation is able to predict the performance of the counter-flow regenerative IEHX within a discrepancy of 12%. We further demonstrated that the correlation could be a practical approach to predict the performance and optimize the configuration of the IEHX.

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## 1. Introduction

The evaporation of water into the air is a natural phenomenon resulting in a reduction of the air stream dry-bulb temperature. Due to the large latent heat of water evaporation, the evaporative cooling system is considered as an effective and promising technique for cooling applications. The IEHX (indirect evaporative heat exchanger) is able to produce cooled air without increasing its absolute humidity. A typical IEHX comprises a series of plates separating the primary air in the dry channel and the secondary air in the wet channel.

To comprehensively study the simultaneous heat and mass transfer process that occurs in the evaporative cooler, mathematical modelling has been the subject of many research works found in literature [1]. For a conventional indirect evaporative cooling unit, the theoretical minimum temperature of the primary air is its wet-bulb temperature [2,3]. Theoretical studies showed that the thermal performance of IEHX is affected by several key parameters such as the channel dimension, the intake air humidity ratio and temperature [4]. Guo and Zhao [5] conducted parametric study and discussed the optimal parameters for designing the indirect evaporative cooler.

To achieve a sub-wet bulb cooling, researchers have proposed different methods to further improve the thermal performance of the indirect evaporative cooler. Hsu et al. [6] investigated four prototypes of the IEHX and indicated that the air can be cooled to a temperature lower than its inlet wet-bulb temperature by using

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$A$	area [ $\text{m}^2$ ]
$\alpha$	thermal diffusivity [ $\text{m}^2/\text{s}$ ]
$c$	molar concentration [ $\text{mol}/\text{m}^3$ ]
$c_{pa}$	specific heat of moist air [ $\text{kJ}/(\text{kg}\cdot\text{K})$ ]
$D$	diffusivity [ $\text{m}^2/\text{s}$ ]
$h_c$	convection heat transfer coefficient [ $\text{kW}/(\text{m}^2\cdot\text{K})$ ]
$h_m$	mass transfer coefficient [ $\text{kg}/(\text{m}^2\cdot\text{s})$ ]
$h_{fg}$	specific latent heat of water evaporation [ $\text{kJ}/\text{kg}$ ]
$H$	height of the channel [ $\text{m}$ ]
$k$	thermal conductivity [ $\text{kW}/(\text{m}\cdot\text{K})$ ]
$L$	length of the channel [ $\text{m}$ ]
$Le_f$	Lewis factor
$m$	mass flow rate of air [ $\text{kg}/\text{s}$ ]
$M$	molar mass [ $\text{kg}/\text{mol}$ ]
$Nu$	Nusselt number
$p$	pressure [ $\text{kPa}$ ]
$T$	temperature [ $^{\circ}\text{C}$ ]
$u$	velocity in $x$ direction [ $\text{m}/\text{s}$ ]
$v$	velocity in $y$ direction [ $\text{m}/\text{s}$ ]
$W$	width of the channel [ $\text{m}$ ]
$\omega$	humidity ratio [ $\text{kg}/\text{kg}$ ]

$\rho_a$	air density [kg/m <sup>3</sup> ]
$\theta$	dimensionless group
$\xi$	dimensionless coefficient
$\Pi$	dimensionless group
$x$	spatial coordinate in Cartesian systems; flow length in a channel [m]
$y$	spatial coordinate in Cartesian systems

<i>a</i>	air
<i>p</i>	primary air, primary channel
<i>s</i>	secondary air, secondary channel
<i>in</i>	inlet
<i>out</i>	outlet
<i>w</i>	water film, plate
<i>dew</i>	dew-point temperature

\* dimensionless parameter

Several researchers also investigated cross-flow IEHXs and compared their thermal performance in terms of the air flow arrangement [21,22]. Moshari and Heidarinejad [23] indicated that the counter-flow regenerative IEHX can produce lower temperature comparing to cross-flow IEHX. Lee et al. [24] investigated and compared the performance of flat plate, corrugated plate and finned channel type IEHXs. Zhan et al. [25,26] studied the performance of a counter-flow and a cross-flow M-cycle IEHXs. Their results demonstrated that the counter-flow arrangement could produce about 20% higher cooling capacity and 15–23% greater dew-point effectiveness in comparison to the cross-flow configuration. Anisimov and Pandelidis [27,28] developed a numerical model to study the effect of different flow patterns on the performance of IEHX. Their simulation results also indicated that the parallel and regen-

It can be observed from previous works that the performance of IEHX is influenced by a number of system parameters, such as channel height, channel length, intake air temperature, intake air humidity ratio, and intake air velocity. The literature review indicates several research gaps. Firstly, previous theoretical studies were conducted to examine the effect of a specific operating parameter [5,11–13,15,27]. However, existing works have yet to adequately analyze the combined influence of various design and operating parameters. Secondly, many numerical formulations employ complex numerical methods and require long computational time due to numerous iterative calculations in order to achieve the desired solution accuracy [11–13,22–25]. Few attempts have been made to develop practical correlations that enable one to conveniently evaluate the performance of counter-flow regenerative IEHXs without any iterative processes.

To address these issues, the present study proposes the development of an empirical correlation based on dimensionless groups for the purpose of evaluating the thermal performance of a

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