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A numerical investigation of thermal airflows over strip fin heat sinks \star

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The benefits of using strip fin heat sinks (SFHSs) where the cross-sectional aspect ratio of the fins lie between 14 those for plate fins (high aspect ratio) and pin fins (aspect ratio ≈ 1) are explored computationally, using a con-15 jugate heat transfer model. Results show that strip fins provide another effective means of enhancing heat transfer, especially when staggered arrangements of strip fins are used. A detailed parameter investigation 17 demonstrates that perforating the strip fins provides additional improvements in terms of enhanced heat trans-18 fer, together with reduced pressure loss and heat sink mass. Results are also given which show that, for practical applications in micro-electronics cooling, perforated SFHSs offer important benefits as a means of achieving smaller processor temperatures for reduced mechanical power consumption. 21

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32 1. Introduction

The inexorable rise in heat flux densities from micro-electronic com-33 34ponents and devices is presenting the industry with formidable chal-35lenges in maintaining processor temperatures below critical values, in order to circumvent a range of important failure modes, [1]. These chal-36lenges have stimulated a number of cooling innovations, including the 37 use of highly conductive inserts to provide more efficient pathways to 38 heat removal, [2], and a number of promising liquid cooling methods. 39 The latter include on-chip cooling, direct liquid jet impingement and di-40 electric liquid immersion which removes heat by convection currents, 41 [3]. 42

This paper focuses on what remains currently the most popular ap-43 44 proach for cooling microelectronics, namely convective heat transfer to air as it flows over a network of extended surface fins on a heat sink. It 45has recently been estimated that heat sinks account for more than 80% 46of the thermal management solutions for electronics, which will be 4748worth over \$10 billion in 2016 [4]. Heat sinks provide a low cost and reliable means of achieving a large total heat transfer surface area without 49 excessive primary surface area, and the surface fins act as turbulence 5051promoters which enhance heat transfer rates by breaking up the thermal boundary layer. The main goals of heat sink design are to provide 52sufficient heat transfer rates, to ensure that processor temperatures re-53 54main below critical values, for minimal pressure loss and heat sink mass, 55see e.g. [5].

56 Heat sinks based on rectangular plate fins (PFHSs) are the most com-57 mon. Several experimental and numerical studies of PFHSs have

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http://dx.doi.org/10.1016/j.icheatmasstransfer.2016.03.014 0735-1933/© 2016 Elsevier Ltd. All rights reserved. appeared in the literature, see e.g. [6,7], and these have demonstrated 58 that the heat transfer rate can be improved by modifying the arrange-59 ment of the fins by, for example, employing staggered arrangements 60 of plate fins, see e.g. [8,9], or periodically interrupted diverging and con-61 verging fins, [10]. Generally, it is found that staggered arrangements of 62 plate fins can improve heat transfer but at the cost of significantly larger 63 pressure drops across the PFHSs. 64

A number of recent studies have shown that perforating the fins in 65 PFHSs can lead to localised air jets which result in substantial improve- 66 ments in heat transfer rate with reduced pressure losses. Shaeri and 67 Yaghoubi [11] and Dhanawade and Dhanawade [12] studied thermal 68 air flows through arrays of plate fins, with one or more rectangular per- 69 forations respectively parallel to the dominant flow direction. They 70 found that perforations reduce the pressure loss by reducing the size 71 of the wakes behind the fins and the length of the recirculation zone 72 around the lateral surface of the fins, whereas air jets through the perfo-73 rations generally enhance the heat transfer rate. Ismail et al. [13] also 74 found that the shape of the perforations can be influential and that the 75 pressure drop with circular perforations is substantially smaller than 76 with square ones. 77

The plate fins on heat sinks are often replaced by pins with a much 78 smaller cross-sectional aspect ratio, typically with the ratio of fin length 79 to width AR \approx 1, see Fig. 1. These are often referred to as pinned heat 80 sinks (PHSs) and several studies have shown that PHSs can be much 81 more effective at disrupting the boundary layer and improving rates of 82 heat transfer, see e.g. [14,15], but at the cost of much larger pressure 83 drops. The effect of pin arrangement in terms of pin density and orien- 84 tation to the dominant flow direction (either in-line or staggered) has 85 also been shown to be very influential in PHSs. Generally, increasing 86 pin density and employing staggered arrangements of pins both lead 87 to increased rates of heat transfer and larger pressure losses, [8,16–19]. 88

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T1.1	Nomenclature	
T1.2	Ac	cross-sectional area of the flow passage of the heat
T1.3		sink, m ²
T1.4	D	pin diameter of the pin fin heat sink, mm
T1.5	d	perforation diameter of the pin fin, mm
T1.6	D_h	hydraulic diameter, m
T1.7	Н	pin fin height, mm
T1.8	θ	thermal resistance, K/W
T1.9	h_p	projected heat transfer coefficient, W/m ² ·K
T1.10	h	heat transfer coefficient, W/m ² ·K
T1.11	k	turbulence kinetic energy, kg m ² /s ²
T1.12	п	number of perforations
T1.13	Ν	number of pins
T1.14	L	heat sink length, mm
T1.15	Nu	Nusselt number
T1.16	Р	fan power, W
T1.17	Δp	pressure drop, Pa
T1.18	Pr	Prandtl number
T1.19	Pr_t	turbulent Prandtl number
T1.20	Q	power applied on the base, W
T1.21	Sz	pin pitch in streamwise direction, mm
T1.22	Re	Reynolds number
T1.23	T	temperature, °C
T1.24	ΔT	temperature difference, °C
T1.25	U	air velocity, m/s
T1.26	θ_s	thermal resistance in terms of surface area, K m ² /W
T1.27	T _{base}	base temperature, °C
T1.29	h _T	Total heat transfer coefficient, W/m ² ·K
T1.30	Greek	
T1.31	α	fluid thermal diffusivity (m ² /s)
T1.32	α,β,β*	turbulence model constants
T1.33	ϕ	porosity V _{void} /V
T1.34	μ	fluid viscosity (Pa·s)
T1.35	μ_t	turbulent eddy viscosity, Pa·s
T1.36	ρ	fluid density (kg/m ³)
T1.37	v	kinematic viscosity, m ² /s
T1.38	ν_t	turbulent Kinematic Viscosity, m ² /s
T1.39	σ_{ε}	K-E turbulence model constant
11.40 TT1.40	σ	turbulence model constant for the K-equation
11.42	ω	κ - ω turbulence model constant

In comparison with PFHSs, relatively few studies have considered
the effect of perforations on heat transfer and pressure drops in PHSs.
Sahin and Demir [20,21], for example, studied the effect of cross sectional shape (circular or square) for in-line pin arrays while Dhumne



Fig. 1. The six fin designs considered, and a definition of pin aspect ratio, AR = l/w.

and Farkade [9] considered the effect of staggered pin arrangements for 93 singly-perforated pins of circular cross-section. Dai et al. [22] studied 94 the benefits of micro-jets to improve heat transfer rate and reduce 95 pressure drop by inducing flow separation in PHSs. Collectively, these 96 studies have shown that perforations can also lead to substantial im- 97 provements in heat transfer for reduced pressure losses for PHSs. Al- 98 Damook et al. [15] have very recently used complementary experimen-99 tal and numerical methods to explore the benefits of using multiple pin 100 perforations within PHSs. They showed that the heat transfer rate in- 101 creases monotonically with the number of pin perforations, while the 102 pressure drop and fan power, required to overcome the pressure drop, 103 both reduce monotonically; the location of the perforations was found 104 to be much less influential. Their conjugate heat transfer analysis 105 showed, further, that improved heat transfer with pin perforations 106 leads to significantly reduced processor case temperatures and pin 107 mass. Their experiments also revealed that practical considerations, in- 108 cluding pin perforation alignment with the dominant flow direction and 109 the quality of the pins' surface finish, can affect the heat transfer and 110 pressure drop significantly. 111

Most studies of PHSs to date have considered cases where the pins 112 have cross-sectional aspect ratios, AR \approx 1. The present study focuses 113 on the benefits of employing pins with a larger aspect ratio, AR = 1142.25, as a compromise between the simplicity of PFHSs and the need 115 to employ several small pins on PHSs. Such heat sinks are referred to 116 here as strip fin heat sinks (SFHSs) and very few previous studies of 117 SFHSs have appeared in the literature. Jonsson and Moshfegh [23], for 118 example, studied the performance of strip fins, square pins, circular 119 pins, and plate fins with in-line and staggered arrangements. Using a 120 coarse arrangement of strip fins with AR = 5.3, the pressure drop in 121 their experiments was substantially lower than for a denser arrange- 122 ment of pins but with a similar thermal resistance. Hong and Cheng 123 [24] studied the performance of strip fins in staggered arrangements 124 in a micro-channel heat sink. They varied the fins' length and the spaces 125 between fins to find the optimal design. Their results showed that SFHSs 126 clearly enhance the rate of heat transfer and that the pressure drop is 127 strongly related to strip fin spacing. 128

The present study is the first detailed numerical investigation into the 129 benefits of employing perforations in SFHSs. It compares the thermal and 130 hydraulic performance of staggered and in-line arrangements of strip 131 fins with PHSs with circular and square pins of AR = 1, and shows 132 how these can be further enhanced by perforating the strip fins. The 133 paper is organised as follows. Section 2 describes the conjugate heat 134 transfer model for the heat sink problems under consideration and the 135 numerical methods used to solve them. A comprehensive set of solutions 136 is presented in Section 3 and conclusions are drawn in Section 4.

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2. Numerical methods

2.1. Problem description

The heat sink designs considered are shown in Fig. 1 with circular 140 and square pins, of cross-sectional aspect ratio AR = l/w = 1, and 141 strip fins with AR = 2.25, where *l*, and *w* are the fin length and width 142 respectively. Those values are chosen to facilitate a convenient compar- 143 ison with the PHSs considered here. Heat sinks with solid and perforat- 144 ed fins in in-line or staggered arrangements shown in Fig. 2 are 145 investigated. The perforated fins contain three circular perforations 146 aligned with the direction of flow and the diameter of each perforation 147 is 1 mm. The case with circular pins in an in-line arrangement has re- 148 cently been studied by Al-Damook et al. [15]. The dimensions of the 149 base plate, fin height and fin thickness or diameter are the same for all 150 heat sinks and are equal to 50×50 mm, 10 mm and 2 mm, respectively. 151 The number of fins is 64 for those with in-line arrangement and 60 for 152 heat sinks with a staggered configuration. Following Al-Damook et al. 153 [15], the heat sinks are aluminium with thermal conductivity 202 W/ $_{154}$ $m \cdot K$ and with a base plate thickness of 2 mm. 155

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