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Comparative evaluations of thermofluidic characteristics of sandwich panels with X-lattice and Pyramidal-lattice cores



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ABSTRACT

This study compares the thermo-fluidic characteristics of sandwich panels with the X-lattice and the Pyramidal lattice at a given porosity and surface area density. The numerical model is validated against available experimental data at first. At a given Reynolds number in the range of 3100–5700, numerical results reveal that the X-lattice sandwich panel provides a 47–60% higher average overall Nusselt number. The special topology of the X-lattice induces counter-rotating spiral primary flow and more complex secondary flows, including one which becomes a longitudinal vortex later. The flow in the Pyramidal lattice sandwich panel is composed of a parallel primary flow and a counter-rotating vortex pair entrenched in the zone behind ligaments of the Pyramidal lattice. Compared with the Pyramidal lattice sandwich panel, endwall heat transfer of the X-lattice sandwich panel is enhanced by 75–97% and the ligaments surface heat transfer is enhanced by 85–97% at a given Reynolds number. It is also found that the friction factor of the X-lattice sandwich panel is about 2 times higher for the spiral primary flow and more complex secondary flows induced by the staggered ligaments. Finally, at a given pumping power, the cooling performance of the X-lattice is much better, too. Taking the identical fabrication method and cost into account, apparently the X-lattice is superior in engineering applications.

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1. Introduction

For energy systems, thermal management is a matter of great importance. Under certain circumstances, for example, active cooling of combustion chambers of hypersonic vehicles and jet blast deflector of aircraft carriers [1–5], a heat sink is required to be able to bear the severe thermal/mechanical load concurrently [1,2,4–7]. For these situations, the sandwich panel cored with the periodic cellular material (PCMs) is one of the promising structures. It is revealed that PCMs with high specific strength/stiffness are lightweight and that the open topologies with high specific surface area makes PCMs excellent heat dissipation structures [7]. Due to these advantages, many researches have been carried out on fabrication methods of cost-effective PCMs, friendly PCMs design and mechanical/thermal performance of PCMs in the previous decades.

A cost-effective fabrication method of PCMs is the first concern. Nowadays, fabrication methods including investment casting [8],

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metal wire weaving [9], metal sheet folding [10–12] have been applied to prepare PCMs including those shown in Fig. 1. For investment casting, a melted parent metal is poured into a casting die, then the expendable fabricate by rapid prototyping is gasified, finally the casting is taken after cooled. The investment casting is an extremely complex process, which is suitable for low volume production of products with complex appearance [8]. Metal wire weaving literally is weaving of the helical metal wires. Unfortunately, solution to weave PCMs with complex topologies by machine is still not found [9]. For metal sheet folding, perforated or expanded metal sheet fabricated based on the target topology, is automatically folded. In view of production cost and process simplicity, metal sheet folding is the most effective process for automatic product lines [11].

Thermal and mechanical performance of PCMs is another concern reported by many researchers. Research on thermal and mechanical performance is one step behind the development of PCMs' fabrication method. Hoffmann et al. [13] did research into the thermo-fluidic characteristics of a casted Kagome metallic lattice through experiments. They found that the orientation of the lattice relative to the flow direction is one factor affecting both

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Nomenclature model constant in Eq. (6) $U_{\rm m}$ mean velocity at the inlet of the computational domain $CD_{k\omega}$ a term defined in Eq. (11) specific heat of fluid (I/(kg K)) V_{i} velocity components in 3-D Cartesian coordinate sys $c_{\rm pf}$ static pressure coefficient defined in Eq. (19) tem (m/s) $C_{\rm p}$ velocity magnitude (m/s) E_t turbulent kinetic energy (J) $V_{\rm m}$ F_1 non-dimensional blending function defined in Eq. (10) $V_{\rm m}/U_{\rm m}$ non-dimensional velocity magnitude non-dimensional blending function defined in Eq. (9) width of an X-lattice unit cell (m) F_2 w friction factor defined in Eq. (18) width of a core ligament (m) fн w_1 local heat transfer coefficient (W/(m² K)) W width of the sandwich panel (m) h H_c height of the sandwich channel (m) χ_{i} three components of 3-D Cartesian coordinate system thermal conductivity of fluid (W/(m K)) ke thermal conductivity of solid (W/(m K)) Cartesian coordinates (m) $k_{\rm s}$ *x*, *y*, *z* 1 length of a lattice core unit cell (m) dimensionless wall distance length of the sandwich panel (m) minimum distance between a point to its surrounding I Nu local Nusselt number solid wall in Eq. (9) (m) area-averaged local Nusselt number Nuave average overall Nusselt number Nu_{H} Greek symbols static pressure (Pa) $\alpha_1 - \alpha_3$ model constants in Eq. (12) production rate of turbulent kinetic energy due to fluid model constants in Eq. (12) β_1 - β_3 viscosity $(J/(m^3 s))$ defined in Eq. (7) model constants in Eq. (4) turbulent Prantle number Pr_{t} Δp pressure drop (Pa) heat flux applied on the outer surface of the bottom model constants in Eq. (12) $\sigma_{\rm k1}$ - $\sigma_{\rm k3}$ substrate (W/m²) σ_{ω_1} – σ_{ω_3} model constants in Eq. (12) Q pumping power (W) porosity fillet radii shown in Fig. 5 (m) dynamic viscosity of fluid (Pa s) $\mu_{\rm f}$ Re_{H} Reynolds number defined in Eq. (13) turbulent viscosity defined in Eq. (6) (Pa s) μ_{t} strain rate defined in Eq. (8) (1/s) S' density of fluid (kg/m³) $\rho_{\rm f}$ t_{s} thickness of the substrate (m) surface area density (m²/m³) ρ_{SA} thickness of a core ligament (m) turbulent frequency (1/s) ω fluid temperature in Eq. (3) (K) $T_{\rm f}$ T_{fb} bulk mean fluid temperature defined in Eq. (16) (K) **Abbreviations** inlet fluid temperature (K) $T_{\rm in}$ OA orientation A $T_{\rm s}$ solid temperature in Eq. (3) (K) **PCMs** periodic cellular materials wall temperature (K) T_{w}

pressure drop and heat transfer tremendously. Through experiments and numerical simulations, the pioneer, Kim et al. [14–17] thoroughly discussed the forced convective heat transfer mechanisms of a casted tetrahedral metallic lattice as shown in Fig. 1. Joo et al. [1] and Feng et al. [18] investigated heat transfer characteristics of a wire-woven bulk Kagome (WBK) lattice. They concluded that the WBK lattice thermally exceeds the casted Kagome lattice at identical porosity. Gao et al. [19,20] introduced a composite tetrahedral lattice and explored its thermal performance for electronics cooling. They also developed relevant

analytical models for engineering design based on their research. Yan et al. [4,5,11,21] introduced an X-type metallic lattice and investigated its flow characteristics and heat transfer mechanisms through experiments and numerical simulations. For a given porosity, they drew the conclusion that the overall thermal performance of the X-type lattice outperforms other reference lattices because of the unique spiral primary flow and three types of second flows. Zhao et al. [22] developed a woven lattice by weaving copper wires orthogonally and investigated the influence of weaving pattern and flow configurations on the thermal performance.

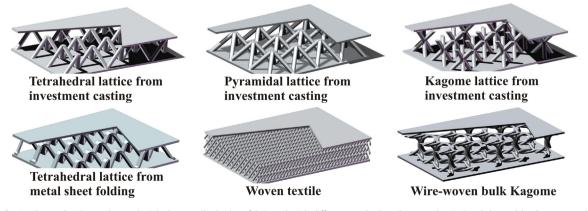


Fig. 1. The sandwich panels cored with the metallic lattices fabricated with different methods to bear mechanical and thermal load concurrently.

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