



Heat transfer from a flat plate in inhomogeneous regions of grid-generated turbulence



G. Melina^{a,*}, P.J.K. Bruce^a, J. Nedić^b, S. Tavoularis^c, J.C. Vassilicos^a

^a Department of Aeronautics, Imperial College London, London SW7 2AZ, United Kingdom

^b Department of Mechanical Engineering, McGill University, Montreal, Quebec H3A 0C3, Canada

^c Department of Mechanical Engineering, University of Ottawa, Ottawa, Ontario K1N 6N5, Canada

ARTICLE INFO

Article history:

Received 20 December 2017

Received in revised form 5 March 2018

Accepted 6 March 2018

Keywords:

Forced convection

Flat plate

Grid-generated turbulence

IR thermography

ABSTRACT

Experiments on the convective heat transfer from a flat plate, vertically mounted and parallel to the flow in a wind tunnel, were carried out via Infra-Red thermography and hot-wire anemometry. The Reynolds number based on the inflow velocity and on the length of the plate was about 5×10^5 . A step near the leading edge of the plate was used to promote transition to turbulence, with tripping effects on the heat transfer coefficients shown to be negligible for more than 90% of the plate's length. Different types of grids, all with same blockage ratio $\sigma_g = 28\%$, were placed upstream of the plate to investigate their potential to enhance the turbulent heat transfer. These grids were of three classes: regular square-mesh grids (RGs), single-square grids (SSGs) and multi-scale inhomogeneous grids (MIGs). The heat transfer coefficients at the mid-length of the plate were correlated with the mean velocity and the turbulence intensity of the flow at a distance from the plate at which the ratio of the standard deviations of the streamwise and wall-normal velocity fluctuations began to increase. However, the heat transfer was shown to be insensitive to the turbulence intensity of the incoming flow in close proximity of the tripping step. Furthermore, the integral length scale of the streamwise turbulent fluctuations was found not to affect the heat transfer results, both near the tripping step and in the well-developed region on the plate. For the smallest plate-to-grid distance, the strongest heat transfer enhancement (by roughly 30%) with respect to the no-grid case was achieved with one of the SSGs. For the largest plate-to-grid distance, the only grid producing an appreciable increase (by approximately 10%) of the heat transfer was one of the MIGs. The present results demonstrate that MIG design can be optimised to maximise the overall heat transfer from the plate. A MIG that produces a uniform transverse mean shear, which is approximately preserved over significant downstream distances from the grid and with a velocity decreasing with distance from the plate, allows a sustained heat transfer enhancement, in contrast to all other grid designs tested here. The most efficient configuration for a MIG is one for which the section of the grid that has lower blockage and thicker bars is adjacent to the plate.

© 2018 Elsevier Ltd. All rights reserved.

1. Introduction

Convective heat transfer from a flat plate is a topic of interest in classical fluid mechanics and in many engineering applications, as different industrial devices make use of flat surfaces to exchange heat with a fluid in motion. A relevant example in the renewable energy industry is the case of high-temperature pressurised-air solar receivers, which are key components in solar power tower plants [33,6]. Considerable effort has been made towards achieving the highest possible heat transfer rate in such devices. Among the suggested solutions, there are two main categories: modifications

to the heat transfer surface (e.g., by the addition of roughness or riblets) and modifications to the flow upstream of the flat surface [5]. In many cases, the latter approach could be the only practical one, as it does not require alterations of the entire heated surface, which may be undesirable or too cumbersome to make. The present study is focused upon devising strategies to enhance heat transfer from a flat surface that is contained within a duct (in this case the test section of a wind tunnel). Two strategies appear to be potentially effective in this respect. An obvious one would be to increase the near-wall mean velocity, which can be achieved by diverting fluid from distant regions of the cross-section towards the wall. An important condition for this approach would be to sustain the near-wall velocity increase over sufficient distance along the heated surface to make a significant enhancement of the

* Corresponding author.

E-mail address: g.melina13@imperial.ac.uk (G. Melina).

Nomenclature

β	coefficient of thermal expansion of air	Re_{L_0}	inlet Reynolds number based on U_∞ and L_0
ϵ	turbulent kinetic energy dissipation rate per unit mass	Re_{ϵ_0}	inlet Reynolds number based on U_∞ and t_0
ϵ_p	emissivity of black paint	Re_X	Reynolds number based on U_∞ and X
δ_{99}	99% boundary layer thickness	Re_{H_p}	Reynolds number based on U_∞ and H_p
η	Kolmogorov length scale	res	sum of squared residuals
Θ_u	integral time scale of u	St	local Stanton number
λ	Taylor length scale	\overline{St}	vertically averaged value of St
ν	kinematic viscosity	T	temperature
ν_t	turbulent viscosity	t_0	thickness of the largest bars of the grid in the $y - z$ plane
ρ	density	T_{aw}	adiabatic wall temperature
σ_g	blockage ratio of the grid	T_{film}	film temperature
σ_{SB}	Stefan-Boltzmann constant, $\sigma_{SB} = 5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$	t_m	average value of the thickness of the bars for the central iterations of the multi-scale grids
τ	dimensionless strain	t_p	thickness (in the $x - z$ plane) of the flat plate
Roman symbols		t_w	thickness of the Inconel foil covering the flat plate
A_p	area of the heated section of the flat plate	u, v, w	streamwise (along x), vertical (along y), transverse (along z) velocity fluctuations
c_p	specific heat capacity	u', v', w'	standard deviations of u, v, w
C_ϵ	dissipation coefficient	$\bar{U}, \bar{V}, \bar{W}$	streamwise (along x), vertical (along y) and transverse (along z) instantaneous velocity components
d_{hw}	diameter of the hot-wire	U, V, W	time-averaged values of $\bar{U}, \bar{V}, \bar{W}$
d_p	distance between the heated side of the flat plate and the nearest wind tunnel's lateral wall	U_∞	inlet velocity (upstream of the grids)
\mathcal{D}_i	measured values of St/St_∞^{NG}	V_D	voltage drop
E_{1e}	mean value of $\overline{St}_\infty/\overline{St}_\infty^{NG}$ in $0.3 \leq X/L_p \leq 0.4$	w_s	width of the step (trip) on the flat plate
E_2	mean value of $\overline{St}_\infty/\overline{St}_\infty^{NG}$ in $0.45 \leq X/L_p \leq 0.85$	w_{LE}	width of the flat plate's leading edge
$E_{1e,2}$	mean value between E_{1e} and E_2	W_t	width of the wind tunnel's test section
$E_u (E_v)$	power spectral density of u (v)	x^*	wake interaction length scale for the largest bars of the grids
f	frequency	x_m^*	wake interaction length scale for the central iterations of the MIGs
f_{sh}	vortex shedding frequency of the largest bars of the grid	x_{LE}	distance between the leading edge of the flat plate and the grid
\mathcal{F}_i	values of St/St_∞^{NG} predicted by the fit	x_{peak}	centreline streamwise location of the maximum turbulence intensity
g	gravitational acceleration	x_{TE}	distance between the trailing edge of the flat plate and the grid
Gr_{H_p}	Grashof number based on H_p	xyz	reference frame with its origin fixed at the centre of the grid
h	convective heat transfer coefficient	XYZ	reference frame with its origin fixed at the heated side of the flat plate
H_p	height of the flat plate	z_p	z -coordinate of the heated side of the flat plate
h_s	height of the step (trip) on the flat plate	z_r	z -coordinate where res is minimum
H_t	height of the wind tunnel's test section (or total length of the cylinder)	Subscripts	
I	electric current	c	centreline values ($y = z = 0$)
k	streamwise wavenumber, $k = 2\pi f/U$	$film$	evaluated at T_{film}
K_p	pressure gradient parameter	r	values at $y = 0$ and $z = z_r$
k_s	mean shear rate parameter in the z -direction	w	wall values
L_0	distance between the largest bars of the grid	∞	inlet values or based on inlet conditions
l_{hw}	sensing length of the hot-wire	Acronyms	
L_j	distance between the bars in the j -th iteration of the multi-scale grids	FOV	Field Of View
L_m	average value of the distance between the bars of the central iterations of the multi-scale grids	FSG	fractal square grid
L_p	length of the heated section of the flat plate	HW	hot-wire
L_u	integral length scale of u in the streamwise direction, $L_u = U\Theta_u$	IR	Infra-Red
L_ϵ	dissipation length scale	MIG	multi-scale inhomogeneous grid
n_j	number of bars in the j -th iteration of the MIGs	NG	No Grid
q_{cond}	heat flux lost by thermal conduction	RG	regular grid
q_{conv}	convective heat flux	SSG	single square grid
q_{input}	input heat flux		
q_{rad}	radiative heat flux		
R^2	coefficient of determination of the fit		
Re_θ	boundary layer momentum thickness Reynolds number		

overall heat removal. A second strategy would be to produce near-wall turbulence with an intensity, length scale and structure that would be most effective in enhancing convective heat transfer.

Once more, it is essential that such turbulence would be sustained sufficiently to affect appreciably the overall heat removal. Because local mean velocity and turbulence characteristics are intimately

Download English Version:

<https://daneshyari.com/en/article/7054350>

Download Persian Version:

<https://daneshyari.com/article/7054350>

[Daneshyari.com](https://daneshyari.com)