



# Minimum heat flux and minimum film-boiling temperature on a completely wettable surface: Effect of the Bond number

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## ABSTRACT

We investigated the effect of Bond number of sphere  $Bo_s$  and surface super-hydrophilicity at minimum film-boiling temperature  $T_{MFB}$  and minimum heat flux  $q''_{min}$  using quenching experiment at atmospheric pressure and the saturation temperature of water. In particular, we focused on the vapor-releasing dynamics in film boiling and evaluated the main parameters such as vapor-bubble releasing frequency  $f_b$  and vapor-bubble departure diameter  $D_b$ . We selected two sizes of quench sphere (sphere diameter  $D_s = 15$  mm and 25 mm) based on critical Bond number  $Bo_c$  to evaluate the vapor-releasing dynamics depending on the  $Bo_s$ . The super-hydrophilic surface was prepared by the anodic oxidation on zirconium (Zr-702) sphere. High speed visualization and inverse heat transfer calculation facilitate a qualitative and quantitative analysis of film boiling heat transfer. The surface super-hydrophilicity of the quench sphere increases  $T_{MFB}$  and  $q''_{min}$ : 12% and 366% increase for  $D_s = 15$  mm and 20% and 305% increase for  $D_s = 25$  mm, respectively.  $D_b$  strongly depends on  $D_s$  and exhibits a relatively weak dependency to the surface super-hydrophilicity.  $f_b$  is affected by the  $D_s$  and the surface super-hydrophilicity. The increase in  $T_{MFB}$  is explained by the liquid-solid contact in film boiling. The D25-CWS exhibits the large area fraction of liquid-solid contact versus total heat transfer surface compared to the D15-CWS. The increase in  $q''_{min}$  is related to minimum frequency of vapor-bubble releasing to sustain the stable liquid-vapor interface  $f_{b,min}$  because the large  $f_{b,min}$  indicates the fast destabilization of the liquid-vapor interface in film boiling during quenching.

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## 1. Introduction

Understanding the minimum heat flux  $q''_{min}$  and minimum film-boiling temperature  $T_{MFB}$  is essential for analyzing the film-boiling heat transfer during quenching. The vapor film with low thermal conductivity ( $k_v \sim 0.025$  W/m-K) covers the heat transfer surface, which deteriorates the quench rate in a high-temperature thermal-power system [1]. One of the strategies to increase the quench rate is to increase  $q''_{min}$  and  $T_{MFB}$  [2,3]. The  $q''_{min}$  and  $T_{MFB}$  indicate the collapse criteria of vapor film that serves as an insulator, and these film-boiling crisis are, particularly, affected by the system dimension: Bond number  $Bo = (\rho_l - \rho_v)gR^2/\sigma_{lv}$  [4].

Classical  $q''_{min}$  and  $T_{MFB}$  are described by the hydrodynamic and the thermodynamic limits, respectively [5]. The hydrodynamic model to predict  $q''_{min}$  is based on the vapor-releasing dynamics

suggested by Zuber [6]:  $q''_{min} = e_b n_b f_{b,min}$  where  $e_b$ ,  $n_b$ , and  $f_{b,min}$  are the energy per bubble, number of bubbles released per unit area per release cycle, and minimum number of cycles per second to just compensate for the normal collapse rate, respectively. These parameters are represented by Taylor instability of the liquid-vapor system (Eq. (1)–(3)), and, are mainly functions of the most dangerous wavelength  $\lambda_D = 3^{0.5} \lambda_c = 2\pi\{3\sigma_{lv}/[(\rho_l - \rho_v)g]\}^{0.5}$ , which is only determined by the properties of liquid and vapor (0.027 m for the atmospheric pressure  $P_{atm}$  and saturation temperature  $T_{sat}$  of water). The thermodynamic model to predict  $T_{MFB}$  is explained by the superheat limit of the liquid;  $T_{MFB} \sim (23/32)T_{cr}$  [7]. However, this model is often substituted by the hydrodynamic model considering  $\lambda_D$  and Newton's law of cooling:  $T_{MFB} = q''_{min}/h_{film} + T_{sat}$  [8]. Thus, the analysis of the vapor bubble dynamics in film boiling is an intuitive approach to explain the change in  $T_{MFB}$  and  $q''_{min}$  during quenching.

$$e_b = \left(\frac{4\pi}{3}\right) \left(\frac{\lambda_D}{4}\right)^3 \rho_v h_{lv} \quad (1)$$

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## Nomenclature

$A$	area or length	$S$	weighting factor
$A_{eq}$	heat transfer area to produce one bubble	$T$	temperature
$Bi$	Biot number	$T_{sat}$	saturation temperature
$Bo$	Bond number	$T_{cr}$	critical temperature
$Bo_s$	Bond number for sphere	$T_w$	wall temperature
$Bo_c$	critical bond number	$T_i$	initial temperature
$c_1, c_2$	fitting constant	$T_{leid}$	Leidenfrost temperature
$C_p$	specific heat	$T_{MFB}$	minimum film boiling temperature
$D$	diameter	$T_c$	center temperature
$D_v$	vapor dome diameter	$\Delta T_{sat}$	wall superheat
$D_s$	sphere diameter	$t$	time
$D_b$	bubble diameter	$t_{cool}$	cooling time
$D_{tube}$	capillary tube diameter	$V$	volume or electric potential
$e_b$	energy per single bubble	$\nabla V$	electric field
$f_b$	frequency of releasing bubble	$x$	$x$ -coordinate
$f_{b,min}$	minimum number of cycles per second to compensate for the normal collapse rate (or, minimum frequency of releasing bubble)		
$f_{b,min}^*$	increase ratio for $f_{b,min}$	<b>Greeks</b>	
$F_\sigma$	surface tension force	$A$	wave number
$F_{buoy}$	buoyancy force	$\alpha^*$	critical wave number
$g$	gravitational acceleration	$\beta$	growth factor (or, the rate of amplification in interfacial disturbance)
$h_{lv}$	latent heat of vaporization	$\beta^*$	maximum growth factor
$h$	heat transfer coefficient	$\Phi$	$\Phi$ - coordinate
$h_{film}$	heat transfer coefficient in film boiling	$e_{max}$	maximum height of surface roughness
$H$	immersion depth	$\theta$	$\theta$ - coordinate
$k$	thermal conductivity	$\theta_c$	contact angle
$L$	length, or height	$\lambda$	wavelength
$L_c$	characteristic length	$\lambda_c$	critical wavelength
$n_b$	number of bubbles released per unit area per release cycle	$\lambda_D$	most dangerous wavelength
$P$	pressure, or probability	$\rho$	density
$P_{atm}$	atmospheric pressure	$\sigma_{lv}$	surface tension of liquid-vapor
$q''$	heat flux	$\psi$	property coefficient
$q''_{min}$	minimum heat flux		
$q''_{min}^*$	increase ratio for $q''_{min}$	<b>Abbreviation</b>	
$R, r$	radius	BZS	bare zirconium surface
		CWS	completely wettable surface
		PDF	probabilistic density function

$$n_b = 2/(\lambda_D)^2 \quad (2)$$

$$f_{b,min} = 0.4 \left\{ \frac{[4(\rho_l - \rho_v)^3 g^3]}{[27(\rho_l + \rho_v)^2 \sigma_{lv}]} \right\}^{0.25} \quad (3)$$

The vapor bubble dynamics in film boiling varies depending on the  $Bo_s$ , which directly affects  $q''_{min}$  and  $T_{MFB}$  [4,9,10]. For  $\lambda_D$ , the critical wavelength  $\lambda_c = 2\pi\{\sigma_{lv}/[(\rho_l - \rho_v)g]\}^{0.5}$  is a criterion to analyze film boiling on a sphere and determines the releasing dynamics of the vapor bubbles [4].  $\lambda_c$  is 0.016 m at  $P_{atm}$  and  $T_{sat}$  of water and corresponds to the critical Bond number for a sphere;  $Bo_c = (\rho_l - \rho_v)g(\lambda_c/2)^2/\sigma_{lv} \sim 9.85$ . Small spheres ( $D_s < \lambda_c$  or  $Bo_s < Bo_c$ ) exhibit the single vapor dome in film boiling, whereas large spheres ( $D_s > \lambda_c$  or  $Bo_s > Bo_c$ ) have multiple vapor domes. This classification corresponds well to the interfacial motion in film boiling, which illustrates the growth of a capillary wave at the liquid-vapor interface in accordance with  $D_s$ .

Frederking and Daniels [9] analyzed the relationship between  $D_b$  and  $f_b$  from a sphere during film boiling and compared it to the classical instability theory. The balance between buoyancy force  $F_{buoy}$  and surface tension force  $F_\sigma$  is the key to determine the stability of the liquid-vapor interface system. The rate of amplification in interfacial disturbance  $\beta$ , which is approximated by  $\{[g(\rho_l - \rho_v)\alpha/\rho_l] - (\sigma_{lv}\alpha^3/\rho_l)\}^{1/2}$ , and the wave number  $\alpha = 2\pi/\lambda$  are

the main variables. Considering the stable liquid-vapor interface (small  $\lambda$  or large  $\alpha$ ) and the unstable state (large  $\lambda$  or small  $\alpha$ ), we obtain the critical wave number  $\alpha^* = 3^{-0.5}\{\sigma_{lv}/[g(\rho_l - \rho_v)]\}^{-0.25}$  and maximum growth factor  $\beta^* = 2^{0.5}3^{0.25}g^{0.75}(\rho_l - \rho_v)^{0.75}/(3\rho_l^{0.5}\sigma_{lv}^{0.25})$  by  $\partial\alpha/\partial\beta = 0$ . Assuming that  $f_b \sim (1/\beta^*)$  and  $D_b \sim (1/\alpha^*)$ , one can postulate the relationship between  $f_b$  and  $D_b$  as constant (Eq. (4)), but, this relationship is modified by considering the dependence on  $T_w$  and  $D_s$  (Eq. (5)) [11].

$$f_b(D_b)^{0.5} \sim \left[ \frac{g(\rho_l - \rho_v)}{\rho_l} \right]^{0.5} \quad (4)$$

$$f_b(D_b)^{0.5} \sim \left[ \frac{g(\rho_l - \rho_v)}{\rho_l} \right]^{0.5} \left\{ 1 + \frac{2 \left\{ \frac{\sigma_{lv}}{[g(\rho_l - \rho_v)]} \right\}^{0.5}}{D_c^2} \right\}^{0.5} \quad (5)$$

Gunnerson and Cronenberg [10] suggested the  $T_{MFB}$  and  $q''_{min}$  model according to  $Bo_s$ ,  $D_b$  and the minimum frequency of vapor bubble release  $f_{b,min}$  were categorized depending on  $D_s$  (Eqs. (6)–(8)),<sup>2</sup> and  $q''_{min}$  was simply described by the energy transport per bubble (Eq. (9)). They defined the four  $D_s$  ranges (small,

<sup>2</sup> It corresponds the large sphere suggested by Gunnerson and Cronenberg [10] suggested:  $0.013 < D_s < 0.157$  m.

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