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# Mixed convection of Al<sub>2</sub>O<sub>3</sub>-water nanofluid in a double lid-driven square cavity with a solid inner insert using Buongiorno's two-phase model



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### ABSTRACT

The present paper investigates steady conjugate mixed convection in a double lid-driven square cavity including a solid inner body. The annulus is filled with water-Al<sub>2</sub>O<sub>3</sub> nanofluid based on Buongiorno's two-phase model. The top horizontal wall is maintained at a constant low temperature and moves to the right while the bottom horizontal wall is maintained at a constant high temperature and moves to the left. The governing equations are solved numerically using the finite element method. The governing parameters are the inner solid location (case 1-case 4), the nanoparticles volume fraction ( $0 \le \phi \le 0.04$ ), Reynolds number ( $1 \le Re \le 500$ ), Richardson number ( $0.01 \le Ri \le 100$ ), the size of the inner solid  $(0.1 \le D \le 0.7)$  and thermal conductivity of the inner solid ( $k_w = 0.01$ , 0.045, 0.1, 0.76 and 1.95 W/m °C). The other parameters; Prandtl number, Lewis number, Schmidt number, ratio of Brownian to thermophoretic diffusivity and the normalized temperature parameter are fixed at Pr = 4.623,  $Le = 3.5 \times 10^5$ ,  $Sc = 3.55 \times 10^4$ , NBT = 1.1 and  $\delta = 155$ , respectively. The results show that the nanofluid strategy in such a cavity has a noticeable augmentation of heat transfer. However, at low Reynolds number, the addition of nanoparticles has an adverse effect on the Nusselt number when the Richardson number is very high. It is also found that a big size solid body can augment heat transfer in the case of high values of both the Reynolds and the Richardson numbers.

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#### 1. Introduction

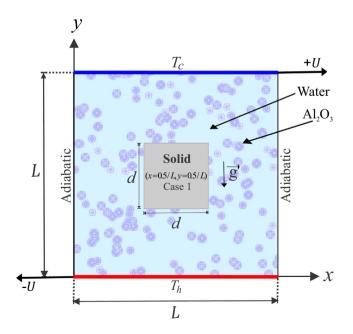
Mixed convection or combined convection fluid flow and heat transfer in cavities is a significant phenomenon in science and engineering systems due to its wide applications in the operation of solar collectors, heat exchangers, drying technologies, home ventilation, high-performance building insulation and lubrication technologies. Mixed convection is more complicated compared to other modes of convection due to the coupling between the buoyancy force by the temperature difference and the shear force by the movement of the wall(s). The study of Papanicolaou and Jaluria [1] performed a numerical investigation of laminar mixed convection in a rectangular cavity with an isolated thermal source. Huang and Lin [2] studied numerically the effects of Grashof and Reynolds numbers on the vortex flow and thermal characteristics in laminar mixed convection in a horizontal rectangular duct. Prasad and

\* Corresponding author. E-mail address: alsabery\_a@ukm.edu.my (A.I. Alsabery). Koseff [3] investigated experimentally the recirculating mixed convection flow in a lid-driven rectangular cavity filled with pure fluid (water). Their results indicated that the convection heat transfer is a very weak function of the Grashof number for the examined range of the Reynolds number. Khanafer and Chamkha [4] considered the mixed convection flow in a lid-driven cavity filled with a Darcian fluid-saturated porous medium. The low thermal conductivity of conventional heat transfer fluids such as water and oils is a primary limitation in enhancing the performance and the compactness of many engineering electronic devices. An innovative and new technique to enhance heat transfer is using solid particles in the base fluid (i.e. nanofluids) in the range of sizes 10-50 nm. A nanofluid is defined as a smart fluid with suspended nanoparticles of average sizes below 100 nm in conventional heat transfer fluids such as water, oil, and ethylene glycol [5]. Due to small sizes and very large specific surface areas of the nanoparticles, nanofluids have superior properties like high thermal conductivity, minimal clogging in flow passages, longterm stability and homogeneity. Also, nanoparticles are used because they stay in suspension longer

$C_p$	specific heat capacity	U, V	dimensionless velocity components in the X and Y-
ď	side length of inner solid square	,	direction, respectively
$d_f$	diameter of the base fluid molecule	$u_B$	Brownian velocity of the nanoparticle
$d_p$	diameter of the nanoparticle	<i>x</i> , <i>y</i> & <i>X</i> , <i>Y</i>	space coordinates & dimensionless space coordinates
Ď	dimensionless side length of the inner body, $D = d/L$		-
$D_B$	Brownian diffusion coefficient	Greek symbols	
$D_{B0}$	reference Brownian diffusion coefficient	α	thermal diffusivity
$D_T$	thermophoretic diffusivity coefficient	β	thermal expansion coefficient
$D_{T0}$	reference thermophoretic diffusion coefficient	δ	normalized temperature parameter
g	gravitational acceleration	$\theta$	dimensionless temperature
Gr	Grashof number	λ	constant moving parameter $(+1 \text{ or } -1)$
k	thermal conductivity	$\mu$	dynamic viscosity
K <sub>r</sub>	square wall to nanofluid thermal conductivity ratio,	v	kinematic viscosity
	$K_r = k_w/k_{nf}$	$\rho$	density
L	side length of enclosure	$\phi$	solid volume fraction
Le	Lewis number	$\phi^*$	normalized solid volume fraction
N <sub>BT</sub>	ratio of Brownian to thermophoretic diffusivity	$\phi$	average solid volume fraction
Nu	average Nusselt number		
Pr	Prandtl number	subscript	
Re	Reynolds number	b	bottom wall
Re <sub>B</sub>	Brownian motion Reynolds number	С	cold
Ri	Richardson number, $Ri = Gr/Re^2$	f	base fluid
Sc	Schmidt number	ĥ	hot
T	temperature	nf	nanofluid
$T_0$	reference temperature (310 K)	p	solid nanoparticles
$T_{fr}$	freezing point of the base fluid (273.15 K)	, t	top wall
u, v	velocity components in the <i>x</i> and <i>y</i> -direction, respec- tively	w	solid inner square

than larger particles. Thus, nanofluid seems a good candidate for heat removal mechanisms in practical, thermal, fluid-based applications. The thermal conductivity of nanoparticles is higher than that of traditional fluids. Thus, nanofluids can be used in a large industrial applications such as oil industry, nuclear reactor coolants, solar cells, construction, electronics, renewable energy and many others. The solid particles are usually metal or metal oxides such as copper (Cu), copper oxide, aluminum oxide ( $Al_2O_3$ ), titanium (TiO<sub>2</sub>) and silver (Ag).

A comprehensive work on natural convection in cavities that are partially occupied by nanofluids was reported by Khanafer and Vafai [6]. Tiwari and Das [7] numerically investigated the mixed convection heat transfer in a two-sided lid-driven square cavity filled with nanofluid by using the finite volume method. They found that the presence of nanoparticles in water tended to increase the heat transfer capacity and both the Richardson number and the direction of the moving walls affect the fluid flow and heat transfer within the cavity. The numerical simulation of the fluid and temperature distributions and the convective heat transfer of the nanofluid could be classified by two main approaches, namely a single-phase model (homogenous) or a two-phase model [8]. The single-phase approach considers the fluid phase and the nanoparticles as being in thermal equilibrium where the slip velocity between the base fluid and the nanoparticles is negligible. On the other hand, the two-phase approach assumes that the relative velocity between the fluid phase and the nanoparticles may not be zero where the continuity, momentum and energy equations of the nanoparticles and the base fluid are handled using different methods. There are number of numerical studies used the single-phase model for simulation of the nanofluids. Abu-Nada and Chamkha [9] considered the mixed convection flow in a lid-driven inclined square enclosure filled with a nanofluid. Salari et al. [10] modeled a numerical study on the mixed convection flow inside a square lid-driven cavity filled with nanofluid when both bottom and side walls are heated simultaneously by finite heat sources. Ismael et al. [11] investigated numerically the mixed convection inside a lid-driven square cavity filled with pure fluid. Ghalambaz et al. [12] numerically studied the effects of the diameter and concentration of nanoparti-



**Fig. 1.** Physical model of convection in a square cavity together with the coordinate system for case 1 (x = 0.5/L, y = 0.5/L).

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