Accepted Manuscript

Title: Integrated Batch Reactive Distillation Column Configurations for Optimal Synthesis of Methyl Lactate

Author: Dhia Y. Aqar Nejat Rahmanian Iqbal M. Mujtaba

PII:	S0255-2701(16)30213-6
DOI:	http://dx.doi.org/doi:10.1016/j.cep.2016.07.009
Reference:	CEP 6827
To appear in:	Chemical Engineering and Processing
Received date:	2-6-2016
Accepted date:	16-7-2016

Please cite this article as: Dhia Y.Aqar, Nejat Rahmanian, Iqbal M.Mujtaba, Integrated Batch Reactive Distillation Column Configurations for Optimal Synthesis of Methyl Lactate, Chemical Engineering and Processing http://dx.doi.org/10.1016/j.cep.2016.07.009

This is a PDF file of an unedited manuscript that has been accepted for publication. As a service to our customers we are providing this early version of the manuscript. The manuscript will undergo copyediting, typesetting, and review of the resulting proof before it is published in its final form. Please note that during the production process errors may be discovered which could affect the content, and all legal disclaimers that apply to the journal pertain.



ACCEPTED MANUSCRIPT

Integrated Batch Reactive Distillation Column Configurations for Optimal Synthesis of Methyl Lactate

Dhia Y. Aqar, Nejat Rahmanian, Iqbal M. Mujtaba^{*} Chemical Engineering Division, School of Engineering, Faculty of Engineering and Informatics, University of Bradford, Bradford, BD7 1DP, UK *Corresponding author I.M.Mujtaba@bradford.ac.uk

Abstract

Although batch reactive distillation process outperforms traditional reactor-distillation processes due to simultaneous reaction and separation of products for many reaction systems, synthesis of Methyl lactate (ML) through esterification of lactic acid (LA) with methanol in such process is very challenging due to difficulty of keeping the reactants together when one of the reactants (in this case methanol) has the lowest boiling point than the reaction products. To overcome this challenge, two novel reactive distillation column configurations are proposed in this work and are investigated in detail. These are: (1) integrated conventional batch distillation column (i-CBD) with recycled methanol and (2) integrated semi-batch and conventional batch distillation columns (i-SBD) with methanol recovery and recycle.

Performances of each of these configurations are evaluated in terms of profitability for a defined separation task. In i-SBD column, an additional constraint is included to avoid overflow of the reboiler due to continuous feeding of methanol into the reboiler as the reboiler is initially charged to its maximum capacity. This study clearly indicates that both integrated column configurations outperform the traditional column configurations (batch or semi-batch) in terms of batch time, energy consumption, conversion of LA to ML, and the achievable profit.

Keywords: Dynamic Modelling; Optimization; Methyl Lactate; i-CBD; i-SBD; Esterification

1. Introduction

Batch reactive distillation process is extensively employed in the chemical industry, particularly for seasonal demand and/or low-volume production. The integration of reaction and distillation in a single vessel (reactive distillation) has offered a number of specific advantages over conventional process of chemical reaction followed by separation (Mujtaba and Macchietto, 1997). It can save the thermal heat consumption, reduce capital and operating costs, overcome the chemical reaction

Download English Version:

https://daneshyari.com/en/article/7089591

Download Persian Version:

https://daneshyari.com/article/7089591

Daneshyari.com