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# Synthesis of magnetic Fe<sub>3</sub>O<sub>4</sub>/activated carbon nanocomposites with high surface area as recoverable adsorbents

Ruey-Shin Juang<sup>a,b,c</sup>, Yao-Chung Yei<sup>d</sup>, Chien-Shiun Liao<sup>d</sup>, Kuen-Song Lin<sup>d</sup>, Hsi-Chuan Lu<sup>e</sup>, Sea-Fue Wang<sup>e</sup>, An-Cheng Sun<sup>d,\*</sup>

<sup>a</sup> Department of Chemical and Materials Engineering, Chang Gung University, Guishan, Taoyuan 33302, Taiwan

<sup>b</sup> Division of Nephrology, Department of Internal Medicine, Chang Gung Memorial Hospital, Linkou, Taiwan

<sup>c</sup> Department of Safety, Health and Environmental Engineering, Ming Chi University of Technology, Taishan, New Taipei City 24301, Taiwan

<sup>d</sup> Department of Chemical Engineering and Materials Science, Yuan Ze University, Chung-Li, Taoyuan 32003, Taiwan

e Department of Materials and Mineral Resources Engineering, National Taipei University of Technology, Taipei 106, Taiwan

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## ABSTRACT

The magnetic  $Fe_3O_4$ /activated carbon nanocomposites with high surface area were synthetized as recoverable adsorbents by chemical binding of  $Fe_3O_4$  nanoparticles on activated carbon (AC) powders. The component AC and  $Fe_3O_4$  in this nanocomposite possesses amorphous non-graphitic structure and cubic crystal structure, respectively. All composite samples presented superparamagnetic properties. The saturation magnetization of  $Fe_3O_4$ /AC nanocomposites was significantly lower than that of bare  $Fe_3O_4$  particles, indicating that  $Fe_3O_4$  particles were truly attached on AC surface. The microstructure image indicated that the  $Fe_3O_4$  particles were uniformly dispersed on AC surface and thus maintained high specific surface area. The adsorption capacity of methyl orange (MO) at 30 °C slightly decreased from 384 mg/g on AC powders to 324 mg/g on  $Fe_3O_4$ /AC nanocomposites, which was reduced by 15% after magnetic fabrication. It was found that MO adsorption on  $Fe_3O_4$ /AC nanocomposites followed the pseudo-second order kinetic model and the isotherms could be described by the Langmuir model. The easy recovery of magnetic adsorbents from aqueous solution demonstrated their application potential to remove toxic pollutants in water and wastewater treatment.

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## 1. Introduction

Industrial activities increase the convenience in the human life since the 18th century. Inevitably, lots of industrial wastewaters containing organic compounds such as dyes from printing, papermaking, textile, and food industries were produced and discharged into the environments. Most of industrial organic pollutants are colored, toxic, carcinogenic, or teratogenic. However, most of colored substances such as dyes are very hard to remove naturally. Textile and dyeing effluents hugely affect human health and endanger thousands of animals and plants. People try to remove dyes from wastewater, but it is very difficult when their concentrations in the effluents are less than 1 mg/L [1,2]. Thus, efficient treatment of textile effluents becomes an important task. Several methods such as adsorption [3,4], centrifugation [5,6], ultrafiltration [7,8], ion exchange [9,10], and electrochemistry [11,12] are usually used to separate dyes from aqueous solutions. Among these methods,

\* Corresponding author.

E-mail address: acsun@saturn.yzu.edu.tw (A.-C. Sun).

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adsorption is powerful and comparatively cheap, and therefore most widely applied for this purpose [13-17].

Activated carbon (AC) is the most common materials used to remove different organic pollutants and has been widely applied to industrial wastewater treatment in practice [18]. AC has a high specific surface area and various functional groups to adsorb colored dyes, particularly in the powdered form [19,20]. However, it is still hard to remove and recover the used AC powders from water, resulting in secondary pollution [21]. Because there is no polarity on AC powders, they cannot be controlled by electric and/or magnetic fields. Centrifugation [5] and filtration [7] are usually adopted to separate the used AC powders from liquid solutions; however, both methods are costly. If AC has the polarity on its surface, we may apply electric and/or magnetic fields to trap, restore, and recycle to avoid secondary pollution after adsorption processes. The idea of combining AC powders and magnetic nanoparticles to adsorb organic pollutants is hence considered [15,22-31], which provides a low-cost, simple, and quick way for practical applications. However, the combination of AC powders and magnetic nanoparticles will create another problem; that is, most pore space within AC powders may be occupied by

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Fig. 1. Chemical structure of methyl orange (MO).

magnetic nanoparticles, leading to a sharp decrease in surface area [29–31]. For example, Ma et al. [31] prepared magnetic ACs from their powdered forms by chemical co-precipitation. The BET surface areas and total pore volumes of the samples changed from 1106 m<sup>2</sup>/g and 0.97 cm<sup>3</sup>/g to 254 m<sup>2</sup>/g and 0.29 cm<sup>3</sup>/g, respectively, after magnetic fabrication. Although AC powders are easily recovered after connecting with magnetic materials, the loss of massive pore space is accompanied by a significant decrease of adsorption ability for organic pollutants. This is particularly the case when magnetic nanoparticles themselves do not show certain adsorption ability for the pollutants of interest [29–31].

To remove organic pollutants from wastewater more efficiently, a large amount of magnetic AC powders is required. Consequently, it is desired to develop a facile way to prepare magnetic ACs with relatively high surface area. It was reported that the loss of surface area of graphene is minimized when Fe<sub>3</sub>O<sub>4</sub> nanoparticles are attached because such nanoparticles will be uniformly distributed on graphene nanosheets [32]. These implied that the decrease of surface area of AC powders could be minimized if Fe<sub>3</sub>O<sub>4</sub> nanoparticles were uniformly distributed on AC powder surface. Therefore, we systematically adjusted the weight ratio of FeCl<sub>3</sub> to NaOH used (F/N ratio) to modify the size and distribution of Fe<sub>3</sub>O<sub>4</sub> nanoparticles on AC powder surface in this study. The polyol-mediated solvothermal reduction method [32,33] was adopted to connect AC powders and magnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles (the so-called Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites), which were used to remove the model pollutant methyl orange (MO) from aqueous solution.

## 2. Experimental

### 2.1. Materials

AC powders with a size ranging from 20 to 40  $\mu$ m were purchased from Showa Chemical Co. (Gyoda, Saitama, Japan). Ferric chloride (FeCl<sub>3</sub>) is the precursor of Fe<sub>3</sub>O<sub>4</sub>, supplied by Riedel-de Haën (Morristown, NJ, USA). Sodium hydroxide and diethylene glycol (DEG) were obtained from Macron Fine Chemical Co. (Center Valley, PA, USA) and Sigma-Aldrich Co. (St. Louis, MO, USA), respectively. Methyl orange (MO, C<sub>14</sub>H<sub>14</sub>N<sub>3</sub>NaO<sub>3</sub>S) purchased from Acros Organics (Geel, Belgium) was chosen as the model adsorbate because it is one of azo dyes that are those constituting more than 50% used in industrial applications [34]. Fig. 1 shows the structure of MO. The commercially-available magnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles with a size of 20–40 nm were purchased from the Nanostructured and Amorphous Materials Inc. (Houston, TX, USA). Their magnetic properties and adsorption performance were also measured and compared in this study.

### 2.2. Synthesis of $Fe_3O_4/AC$ nanocomposites

Fig. 2 presented the synthetics process of magnetic  $Fe_3O_4/AC$  nanocomposites. First at all, NaOH (*y* g) was added into DEG (100 mL) at 120 °C for 1 h and then cooled down to 80 °C for 30 min (the so-called NaOH/DEG stock solution). Meanwhile, AC powders were dispersed in DEG (40 mL) by sonicating for 1 h as shown in step (a), which was the so-called AC/DEG solution. The AC surface had -OH and -COOH groups originated from its activation process. When *x* g of FeCl<sub>3</sub> was added into the AC/DEG



Fig. 2. Synthetic process of Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites.

solution at 220 °C for 30 min, the Fe<sup>3+</sup> ions were coordinated to the -COOH groups of AC as shown in step (b). At step (c), NaOH/DEG stock solution was rapidly injected into FeCl<sub>3</sub>/AC/DEG solution, and the reaction took place at 220 °C for 1 h. The Fe<sup>3+</sup> ions on AC were hydrolyzed to Fe (OH)<sub>3</sub>. Some Fe (OH)<sub>3</sub> would be transformed to Fe(OH)<sub>2</sub> in the solution. Then, Fe (OH)<sub>3</sub> was conjugated with Fe(OH)<sub>2</sub> and was dehydrated to form Fe<sub>3</sub>O<sub>4</sub> and H<sub>2</sub>O according to the reaction:

 $2Fe(OH)_3+Fe(OH)_2\rightarrow Fe_3O_4+4H_2O$ 

All reactions occurred under N<sub>2</sub> atmosphere. At final step (d), the Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites were produced. The wet products were dried at 60 °C in a vacuum oven for 24 h. In this work, Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposite particles were prepared with different parameters, where  $F_xN_y$  denote *x* g of FeCl<sub>3</sub> and *y* g of NaOH [32], and F/N ratio means the value of (*x*/*y*).

## 2.3. Characteristic of AC powders and Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposite

The magnetic hysteresis loops of bare AC powders and Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites were measured using a vibrating sample magnetometer, VSM (DMS model 1660, ADE Technologies Inc., MA, USA) in an applied field range of  $\pm 10$  kOe. Crystal structures of the powders were analyzed by D2 PHASER X-ray diffractometer, XRD (Bruker, Germany) with the scanning region of  $2\theta$  from  $10^{\circ}$  to  $70^{\circ}$ . The surface morphology of bare AC powders and the prepared Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites were determined by the JEOL scanning electron microscope, SEM (JSM-7800F Prime, Tokyo, Japan). The selected area electron diffractions (SAED) and microstructures of the powders were observed by a JEOL transmission electron microscope, TEM (JSM-2010, Tokyo, Japan) with accelerating voltage at 200 keV. The BET surface areas of the samples were measured from N<sub>2</sub> adsorption-desorption isotherms at -196 °C using a porosimeter (ASAP2020, Micromeritics Instrument Co., GA, USA). Prior to measurement, sample was dried overnight in an oven at 130 °C and then placed in the sample tube. After that, the tube was heated to 230 °C and evacuated for 4 h until the pressure was less than  $1.3 \times 10^{-7}$  bar. The total pore volumes of bare AC powders and Fe<sub>3</sub>O<sub>4</sub>/AC nanocomposites were determined from N<sub>2</sub> adsorption isotherms, according to the manufacturer's software (based on the Kelvin equation), and the pore size distribution

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