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Design and evaluation of a micro combined cooling, heating, and power system based on polymer exchange membrane fuel cell and thermoelectric cooler



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ARTICLE INFO	A B S T R A C T		
Keywords: CCHP PEM fuel cell Thermoelectric Carbon dioxide	The main purpose of the present study is to propose a combined cooling; heating and power cycle in microscale to be portable, maintenance free, undetectable, environmentally friendly and can provide the energy demand of a single-family when access to energy suppliers is limited. The prime mover of the cycle is a polymer exchange membrane fuel cell. Heat is recovered from a low-quality waste of 80 °C and water condensate is also recovered from the electrochemical products for domestic hot water. A thermoelectric cooler is used as the cooling system. The mathematical models of the fuel cell and the thermoelectric cooler are coded and the results of simulations are validated with the published data in the literature. The results show that the models are qualified and they can be trusted to be combined for proposing a new micro combined cooling, heating, and power system. The results show that the cycle is capable of producing 2.79 kW of electricity, 3.04 kW of heat and 26.8 W of cooling. The overall efficiency of the trigeneration cycle has reached 76.94% and a fuel saving of 43.25% is achieved. The exergy efficiency is 53.86%. In addition, the carbon dioxide production has reduced about 2.58 kg. hr ⁻¹ . The overall weight of the proposed cycle is estimated less than 100 kg. The exergy analysis introduces the fuel cell as the most exergy destructor.		

1. Introduction

The world population has increased and human lifestyle has changed due to demanding high-quality comfort conditions that need consuming energy to be fulfilled. As a result, the footprint of electricity can be found in every corner of earth planet. In addition, heating and cooling are vital to reaching the requested standards of comfort conditions. As a result, the fuel consumption and air pollution have increased and new threats are emerging from the present human lifestyle. Limited energy resources, global warming, and air pollution are among the most dangerous threats that may vanish human civilization from the planet that used to be green.

Energy Information Administration (2016) reported that 14.77% of the world total electricity was provided by all renewable energy resources, 84.88% by different fossil fuels and the remaining 0.33% by other energy resources. International Energy Outlook has predicted that the share of renewable energy in the world total energy demand would increase to 16% until 2040 while the remaining 84% would be provided by the fossil fuels. These statistics and predictions reveal that the fossil fuels play the main role as the human energy resource up to 2040 [1]. Accordingly, improving the existing energy processes is vital to reduce air pollutants and increase the energy conversion efficiency in energy systems. Since most of the energy users need electricity, cooling and heating simultaneously, the combined production of cooling, heating, and power (CCHP) is an alternative to increase the overall efficiency while providing the energy demands locally. Local CCHP systems not only give the opportunity to use the waste heat of the power generator unit (PGU) but also omit the electricity grid losses.

Portable micro-CCHP systems that can provide the energy demands of a single family for inaccessible electricity grid situations are highly demanded and favorable especially if they could be highly efficient, silent, undetectable and environmentally friendly. This research is devoted to propose and design a micro-CCHP system with such characteristics.

To achieve such characteristics the PGU of the CCHP should be silent, has recoverable waste heat, and electrically efficient. In addition, the cooling system should be silent, light and compact as well.

Different PGUs such as micro-gas turbine, micro-steam turbines, Stirling engines, fuel cells and reciprocating internal combustion engines in microscale can be utilized in the micro-CCHP [2].

Micro-gas turbines are available in the capacity ranges from $15\,kW$ to $250\,kW$ for electricity production, the exhaust gas temperature

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Nomenclature

Abbreviations and symbols

TEO	
TEC	thermoelectric cooler
$s(J. kg^{-1}.$	K ⁻¹) entropy

activation voltage loss concentration voltage loss Ohmic voltage loss

 $V_{\rm ell}(V)$

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1100101144			uctivition voltage loss
		$V_{conc}(V)$	concentration voltage loss
A_{cell} (m ²)	cell area	$V_{ohm}(V)$	Ohmic voltage loss
<i>A</i> (m ²)	sectional area of the element	$\dot{\mathrm{w}}(W)$	power
CCHP	combined cooling, heating and power	X_{H_2O}	saturation molar fraction
C (kJ. kg ⁻¹ . K ⁻¹) specific heat capacity		$X_{N2,in}$	nitrogen mole fraction at the inlet
COP	coefficient of performance	$X_{N2,out}$	nitrogen mole fraction in the outlet
COPe	coefficient of performance of the electrical chiller	α(μν. K ⁻	¹)seebeck factor for the thermoelectric thermocouple
conv	conventional systems	β	exergy efficiency
DHW	domestic hot water	$\alpha_T(\mu v. K)$	⁻¹) total seebeck factor for a thermoelectric module
<i>E</i> (W)	electricity	λ_{air}	air stoichiometric ratio
$F(C.mol^{-1})$ Faraday's constant		ε	emission coefficient
$h(J. kg^{-1})$ enthalpy		μ	membrane moisture content
h_{cell} (W. m ⁻² . K ⁻¹) air convection heat transfer coefficient		σ(W. m ⁻	⁻² . K ⁻⁴) Boltzmann's constant
$H_V(J.mol^{-1})$ heat of evaporation of water		$\sigma_m(\mathrm{m.}\Omega^-)$	⁻¹ .) membrane conductance
$HHV_{H2}(J)$.mol ⁻¹) higher heating value	η	efficiency
<i>i</i> (A. cm ⁻²	²) current density	$\Phi(W)$	exergy rate
<i>i</i> ₀ (<i>A</i> . cm ⁻	⁻²) current density	ψ (J. kg ⁻¹	¹) specific exergy
I(A)	current	$\Delta(W)$	exergy destruction
L (m)	element length		
K (W. m ⁻	⁻¹) thermal conductance of thermoelectric module	Subscript	s and superscripts
$k(W. m^{-1})$	K ⁻¹) thermal conductivity of thermoelectric module		
N _{cell}	number of cells	а	actual
n _e	number of transmitted electrons	b	boiler
n	number of TEC modules	act	activation
Ν	number of pairs of thermocouples in each TEC module	amb	ambient
P (bar)	pressure	comb	combustion
PEMFC	polymer exchange membrane fuel cell	comp	compressor
PGU	power generation unit	с	cold
PHE	plate heat exchanger	conc	concentration
рр	power plant	cons	consumed
$P_{H_2O}(\text{bar})$) water saturation pressure	ele	electromotor
$P_{H_2}(\text{bar})$	partial pressure of hydrogen	gen	generated
$P_{O_2}(\text{bar})$	partial pressure of oxygen	h	hot
$P_{inc}(W)$	input power	ohm	Ohmic
$Q_c(W)$	cooling capacity	inc	input cooling
R(J. mol⁻	⁻¹ .K ⁻¹) constant of gases	FC	fuel cell
$R(\Omega)$	electrical resistance of the thermoelectric module	PEMFC	polymer exchange membrane fuel cell
$T_{FC}(\mathbf{K})$	temperature of the fuel cell	1	liquid
$T_H(\mathbf{K})$	hot side temperature	m	membrane
$T_L(\mathbf{K})$	cold side temperature	S	isentropic
$T_o(\mathbf{K})$	ambient temperature	sat	saturated
$t_{FC}(^{\circ}C)$	temperature of the fuel cell		
$t_m(m)$	membrane thickness		

membrane isentropic saturated the operating gas. Helium is heated by an external burner to about 650 °C in the heater. The exhaust temperature is about 800 °C that is used for preheating of the combustion air to about 600 °C. The exhaust finally leaves the engine at 85 °C, the net weight is 460 kg and its dimensions are $0.98 \times 0.7 \times 1.28$ (m). Its electrical output ranges from 2 to 9.5 kW with an electrical efficiency of 22-24.5%. The operating maximum pressure is 150 bar [5]. This engine is silent but its electrical efficiency is rather low. In addition, its weight and dimensions are rather big and the very high operating pressure of 150 bars is dangerous for portable applications.

Fuel cells are silent PGUs that have higher electrical efficiency with respect to rotary and reciprocating engines. No combustion exists inside a fuel cell, instead, some electrochemical reactions happen and the outputs include electricity, heat, and water. Fuel cells are available in different types of Alkaline (AFC), Proton Exchange Membrane (PEMFC), Direct Methanol (DMFC), Phosphoric Acid (PAFC), Molten Carbonate (MCFC), and Solid Oxide (SOFC). They have been compared

ranges from 240 to 310 °C that is proper for heating and potential thermally activated cooling systems such as absorption and adsorption chillers [3]. However, the minimum capacity of the micro-gas turbine which is commercially available is 15 kW which is really big for a single family and portable demands. They are rather noisy (65 dB at 10 m distance at full load) and their electrical efficiency in this size is about 23%. The dimensions of a 15 kW micro gas turbine are $0.76 \times 1.5 \times 1.9 (m) and$ its weight is 578 kg. These characteristics cross the micro-gas turbine out as a candidate for the target micro-CCHP [4].

Micro-steam turbines which are mostly used in organic Rankine cycles are commercially available in electrical capacity of 275 kW and dimensions of $0.86 \times 1 \times 2(m)$. They also need a micro steam generator, condenser and a feed pump [2]. According to the large size and capacity, the micro-steam turbine cannot be considered as the prime mover of a portable micro-CCHP.

Stirling engines, the reciprocating external combustion engines are available in three types of α , β , and γ . SOLO Stirling 161 uses helium as

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