



Comparative study of the conventional types of heat and mass exchangers to achieve the best design of dew point evaporative coolers at diverse climatic conditions

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ABSTRACT

The objective of this research is a comparative analysis of various kinds of heat and mass exchangers of dew point indirect evaporative cooler. Considering three key performance parameters of an evaporative cooler, namely life-cycle cost, annual water consumption and the annual average of the coefficient of performance as objective functions, the best design of two popular types of the dew-point evaporative cooler (counter-regenerative and cross configurations) for employing in small-scale residential buildings was found through a multi-objective optimization approach. Both operational and geometric characteristics of the coolers were selected as the design (decision) variables while proper constraints such as thermal comfort were imposed. Afterward, between the optimized counter-regenerative and cross configurations, the foremost one was selected for representative cities of four diverse groups within the Köppen-Geiger climate classification system. It was found that in very hot and dry areas, the counter-regenerative configuration was the ideal choice while in other investigated climates, using cross configuration was a better alternative. Moreover, the results showed that in comparison to the base case conditions by using the best-optimized configurations, 64.4, 86.4, and 1039.0% improvements in life-cycle cost, the annual water consumption, and the annual average of the coefficient of performance were achieved, respectively.

1. Introduction

During recent years, dew point indirect evaporative cooling system (DPIEC) has occupied an important role in air-conditioning system technologies. The system was originally patented and developed by Valery Maisotsenko [1–3]. Therefore, the system is also known as the Maisotsenko (M-cycle) indirect evaporative cooling system [4,5]. Maisotsenko (M-cycle) indirect evaporative coolers (MCIECs) not only provide the supply air temperature below the wet-bulb close to dew point temperature by the highest efficiency but also consume much lower electricity than the similar vapor compression systems [6]. Additionally, MCIECs are an environmental option for the conventional vapor compression system [7]. Providing cooled air without adding moisture and wet-bulb effectiveness of higher than 100% could be counted as the main advantages of MCIECs compared to direct evaporative cooling systems (DECs) and other indirect evaporative cooling systems (IECs) [8]. There are different versions of the air flow arrangement in the M-cycle heat and mass exchangers [9]. Fig. 1a represents a counter-flow regenerative heat and mass exchanger with

partial extraction of air (also known as regenerative heat and mass exchanger). Moreover, Fig. 1b shows a cross-flow heat and mass exchanger. Each of these illustrated figures is one of the different types of air flow arrangement. Counter-flow regenerative and cross-flow M-cycles (CoFRMC and CrFMC) are the major popular developed kinds of heat and mass exchangers of MCIECs [10].

There have been two main approaches by which the performance of MCIECs has been analyzed: conducting experiments and developing analytical or numerical models. Conducting experiments is a method in which the researchers have performed a number of experiments and then they have reported and interpreted the results [11–14]. For instance, Xu et al. [11] investigated the performance of an innovative CoFRMC, in which high-quality wet material layer and intermittent water distribution system were employed. In another study, Kashif Shahzad et al. [12] tested an integrated cooling system which composed of solid desiccant and CrFMC. Moreover, Duan et al. [13] found the potential of electrical energy saving of a CoFRMC at diverse climatic conditions of China using an experiment-based evaluation. Khalid et al. [14] also studied the performance of a CrFMC under low inlet air

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Nomenclature

| | | | |
|----------------|--|----------------------|---|
| <i>AACOP</i> | the annual average of coefficient of performance | <i>PWF</i> | present worth factor |
| <i>AACC</i> | the annual average of cooling capacity (kW) | <i>RFMP</i> | retailer's profit |
| <i>AADP</i> | the annual average of dew-point efficiency | <i>RLSHS</i> | the ratio of low speed to the high speed of the fan |
| <i>ANN</i> | artificial neural network | <i>T</i> | temperature (°C) |
| <i>AWC</i> | annual water consumption ($\text{m}^3 \text{year}^{-1}$) | <i>TOPSIS</i> | technique for order preference by similarity to ideal solution |
| <i>C</i> | cost (\$) | \bar{T}_r | mean radiant temperature (°C) |
| c_p | constant pressure specific heat ($\text{J kg}^{-1} \text{K}^{-1}$) | <i>SCST</i> | soft computing and statistical techniques |
| <i>CC</i> | cooling capacity (W) | <i>SH</i> | fan static head (Pa) |
| <i>CoFRMC</i> | counter-flow regenerative Maisotsenko (M-cycle) indirect evaporative cooler | <i>SRM</i> | the stepwise regression method |
| <i>COP</i> | the coefficient of performance | <i>V</i> | velocity (m s^{-1}) |
| <i>CrFMC</i> | cross-flow regenerative Maisotsenko (M-cycle) indirect evaporative cooler | <i>W</i> | cooler width (m) |
| <i>d</i> | discount rate | <i>WAR</i> | working air to total inlet air ratio |
| D_H | hydraulic diameter (m) | <i>WC</i> | water consumption |
| <i>DEC</i> | direct evaporative cooler | <i>X</i> | the size of a component of the system whose cost is determined based on that |
| <i>DPIEC</i> | dew point indirect evaporative cooling system | <i>years</i> | the system's life span (years) |
| <i>EPC</i> | electrical power consumption (W) | | |
| <i>EW</i> | external work (W m^{-2}) | <i>Scripts</i> | |
| f_{on} | the fraction of time in an hour in which CoFRMC or CrFMC is on | <i>air</i> | air |
| f_{cl} | clothing surface area factor | <i>base</i> | base condition |
| f_{resale} | the fraction of resale income at the end of system life span to the initial cost | <i>board</i> | board |
| <i>gap</i> | the height of dry channel (m) | <i>db</i> | dry bulb |
| <i>GMDH</i> | group method of data handling type neural network | <i>dp</i> | dew point |
| <i>H</i> | cooler height (m) | <i>I</i> | initial |
| h_c | convective heat transfer coefficient ($\text{W m}^{-2} \text{K}^{-1}$) | <i>in</i> | inlet air |
| <i>i</i> | inflation rate | <i>fan</i> | fan |
| I_{cl} | insulation ($\text{m}^2 \text{K W}^{-1}$) | <i>fr</i> | friction |
| I_R | resale income (\$) | <i>O</i> | operating |
| <i>k</i> | conductive heat transfer coefficient ($\text{W m}^{-1} \text{K}^{-1}$) | <i>O1</i> | operating in the first year |
| <i>L</i> | channel length (m) | <i>out</i> | outlet (product) air |
| L^* | dimensionless length of the channel | <i>PE</i> | purchase of equipment |
| <i>LCC</i> | life-cycle cost (\$) | <i>rel</i> | relative |
| \dot{m} | the mass flow rate (kg s^{-1}) | <i>sa</i> | supply air |
| <i>M</i> | metabolic rate (W m^{-2}) | <i>sensible</i> | sensible |
| <i>MCIEC</i> | Maisotsenko (M-cycle) indirect evaporative cooler | <i>thermostat</i> | thermostat |
| <i>NSGA-II</i> | non-dominated sorted genetic algorithm 2 | <i>w</i> | water |
| <i>Q</i> | volumetric flow rate ($\text{m}^3 \text{h}^{-1}$) | <i>wa</i> | working air |
| Q_a | volumetric flow rate of required fresh air ($\text{m}^3 \text{h}^{-1}$) | | |
| <i>P</i> | pressure (Pa) | <i>Greek symbols</i> | |
| P_a | water vapor partial pressure (Pa) | Δ | difference |
| <i>PMV</i> | predicted mean vote | ζ | minor loss coefficient |
| <i>POF</i> | Pareto optimal frontier | η | efficiency |
| <i>PPD</i> | predicted percentage dissatisfied (%) | ν | kinematics viscosity ($\text{m}^2 \text{s}^{-1}$) |
| PW_C | present worth of the cash flow of C (\$) | ρ | density (kg m^{-3}) |
| | | ϕ | relative humidity (%) |
| | | ω | absolute humidity ($\text{kg}_{\text{moisture}}/\text{kg}_{\text{dry air}}^{-1}$) |

velocity conditions experimentally. Although experimental measurements provide accurate results, they suffer from the cost of experiments. Developing a model is an alternative approach; however, a developed model must be validated with experimental data. If numerical or analytical models are validated using experimental data, they can be employed in the cases in which there is a lack of experimental data. The models have been obtained either by numerical methods or soft computing and statistical techniques (SCSTs). In the numerical modeling [15–19], different analytical methods such as the effectiveness-NTU method (ϵ -NTU) [16,18], the Eulerian-Lagrangian computational fluid dynamics (CFD) [15] and the finite difference method (FDM) [17,19] have been applied and the obtained numerical results have been validated against existing experimental data. Moreover, in the statistical modeling [5,7,20,21], the effective parameters have been determined

and after extraction of enough data from experiments or numerical models, the modeling process has been conducted to transfer the data into analytical models [22]. Artificial neural networks (ANN) [20], group method of data handling (GMDH) [5,7,20], genetic programming (GP) [20], response surface methodology (RSM) [21], multiple linear regression (MLR) [20] and stepwise regression method (SRM) [6,20] are the statistical techniques by which MCIECs have been modeled so far. In Fig. 2, a graphical summary of the mentioned classification was presented.

From the point of view of the subject, the conducted studies about MCIECs were categorized into some groups. The largest group of studies is those research that the performances of the system are investigated under a variety of effective parameters such as inlet air conditions, the air flow velocity, the dimensions of the air flow passages, and working

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