



A systematic parametric study and feasibility assessment of solar-assisted single-effect, double-effect, and triple-effect absorption chillers for heating and cooling applications



Ali Shirazi^{a,*}, Robert A. Taylor^a, Stephen D. White^b, Graham L. Morrison^a

^a School of Mechanical and Manufacturing Engineering, The University of New South Wales (UNSW), Kensington, New South Wales 2052, Australia

^b Commonwealth Scientific and Industrial Research Organization (CSIRO) Energy Centre, Newcastle, New South Wales 2304, Australia

ARTICLE INFO

Article history:

Received 24 November 2015

Accepted 28 January 2016

Keywords:

Solar heating and cooling

Absorption chiller

Single-effect

Double-effect

Triple-effect

TRNSYS

ABSTRACT

The present work investigates the feasibility of solar heating and cooling (SHC) absorption systems based on combining three types of LiBr–H₂O absorption chillers (single-, double-, and triple-effect) with common solar thermal collectors available on the market. A single-effect chiller is coupled with evacuated tube collectors (ETCs) – SHC1. A double-effect chiller is integrated with parabolic trough collectors (PTCs), linear Fresnel micro-concentrating collectors (MCTs) and evacuated flat plate collectors (EFPCs) respectively – SHC2, SHC3, and SHC4. PTCs are employed to provide high-temperature heat to a triple-effect absorption chiller (SHC5). Although triple-effect chillers have been around for a while, this paper represents the first system-level analysis of these chillers coupled with high-temperature solar concentrating collectors for air-conditioning applications. A simulation model for each configuration is developed in a transient system simulation environment (TRNSYS 17). Furthermore, a unique, comprehensive perspective is given by investigating the impact of characteristic solar beam radiation to global radiation ratios on the techno-economic performance of the proposed SHC plants for a wide variety of climatic regions worldwide. The results of parametric study suggest that a storage volume of around 70 L/m² is a good choice for SHC1, while 40–50 L/m² storage capacity is sufficient for the other configurations (SHC2 to SHC5). The simulation results reveal that when the fraction of direct normal irradiance (DNI) is less than 50%, SHC2, SHC3, and SHC5 require larger collector area compared to SHC1, showing there is no advantage in using concentrating collector powered multi-effect chillers over solar single-effect chillers in climates with low DNI level. However, in climates with DNI fractions above 60%, the smallest solar field is achieved by SHC5, followed by SHC2. SHC4, which benefits from both relatively high COP of double-effect chiller and the diffuse component in the solar field, results in the most reasonable trade-off between energetic and economic performance of the system in a wide range of climatic conditions.

© 2016 Elsevier Ltd. All rights reserved.

1. Introduction

Air-conditioning demand in many countries accounts for about 50% of the energy consumption in buildings – which is mainly supplied by conventional fossil fuels [1,2]. The use of renewable energy technologies in buildings can reduce fossil fuel consumption, and as a result mitigate their environmental impacts [3,4]. Solar cooling is a promising, clean alternative which has the advantage of being *in phase* with the buildings' cooling demand [5–7]. The available technologies on the market for thermally driven cooling systems are absorption and adsorption chillers, solid and liquid

desiccant cooling systems, and ejector refrigeration cycles [8]. Of these, absorption chillers are considered as the most desirable method for harnessing solar thermal energy due to their reliability and higher efficiency. In addition, absorption chillers can be available for large-scale applications and their cost is lower than the rest of thermally-driven air-conditioning systems for such uses [9,10]. There are three types of absorption chillers commercially available on the market – single-, double-, and triple-effect chillers. The advantage of moving toward a higher effect cycle is to enhance the COP of the chiller, if a high temperature heat source is available. The most common working fluid pair used in absorption chillers for air-conditioning applications is lithium bromide–water (LiBr–H₂O), where LiBr is the absorbent and water is the refrigerant [9]. The driving heat source temperature for

* Corresponding author.

E-mail address: a.shirazi@unsw.edu.au (A. Shirazi).

Nomenclature

A	heat transfer surface area (m^2)	u	wind velocity (m/s)
a	characteristic coefficient (–)	U_L	collector overall heat loss coefficient ($\text{W}/\text{m}^2 \text{K}$)
A_a	aperture area (m^2)	USD	US dollar
A_r	receiver area (m^2)	V	specific volume (L/m^3)
c_1	first-order heat loss coefficient ($\text{W}/\text{m}^2 \text{K}$)	$\Delta\Delta T'$	characteristic temperature difference ($^\circ\text{C}$)
c_2	second-order heat loss coefficient ($\text{W}/\text{m}^2 \text{K}^2$)	<i>Greek symbols</i>	
c_3	wind speed dependence of heat losses ($\text{J}/\text{m}^3 \text{K}$)	β	collector slope ($^\circ$)
c_4	long-wave irradiance dependence of heat losses (–)	γ	collector azimuth angle ($^\circ$)
c_5	the collector effective thermal capacitance ($\text{J}/\text{m}^2 \text{K}$)	γ_s	solar azimuth angle ($^\circ$)
c_6	wind dependence of the zero loss efficiency (s/m)	δ	thickness (m)
c_{CO_2}	CO_2 emission penalty cost (USD/tonne CO_{2-e})	η	thermal efficiency (–)
CDE	carbon dioxide emission (tonne)	θ	solar incidence angle on the collector ($^\circ$)
CDEC	carbon dioxide emission cost (USD)	θ_z	solar zenith angle ($^\circ$)
c_E	unit cost of electricity (USD/kWh)	σ	Stefan–Boltzmann constant ($\text{W}/\text{m}^2 \text{K}^4$)
CI	capital investment cost (USD)	<i>Subscripts</i>	
c_{NG}	unit cost of natural gas (USD/GJ)	a	air, ambient
COP	coefficient of performance (–)	AC	absorber–condenser
C_{op}	operating cost (USD)	ACH	absorption chiller
c_p	specific heat at constant pressure ($\text{kJ}/\text{kg K}$)	AH	auxiliary heater
CR	concentration ratio (–)	aux	auxiliary
DNI	direct normal irradiance ($\text{kW h}/\text{m}^2$)	avg	average
E	energy (kWh)	b	beam
e	characteristic coefficient (–)	C	cooling
EF	emission factor ($\text{kg CO}_2/\text{kWh}$)	CHW	chilled water
EFPC	evacuated flat plate collector	Config.	configuration
E_L	long-wave irradiance (W/m^2)	CT	cooling tower
ETC	evacuated tube collector	CTRL	controller
F	collector efficiency factor (–)	CW	cooling water
$F'(\tau\alpha)_n$	collector zero loss efficiency at normal incidence (–)	d	diffuse
GHI	global horizontal irradiance ($\text{kW h}/\text{m}^2$)	DV	diverting valve
G_t	global irradiance on the tilted collector (W/m^2)	E	electricity, evaporator
k	thermal conductivity ($\text{W}/\text{m K}$)	G	generator
$K(\theta)$	incidence angle modifier (–)	H	heating
M	mass (kg)	HW	hot water
\dot{m}	mass flow rate (kg/s)	L	load
MCT	micro-concentrating collector	l	linear, longitudinal
NTU	number of transfer units	MV	mixing valve
PEC	primary energy consumption (kWh, GW h)	NG	natural gas
PEF	primary energy factor (–)	P	pump
PTC	parabolic trough collector	PRV	pressure relief valve
\dot{Q}	heat transfer rate (kW)	q	quadratic
r	characteristic coefficient (kW)	SC	solar collector
R^2	coefficient of determination	SCW	solar collector water
s	characteristic coefficient ($\text{kW } ^\circ\text{C}^{-1}$)	ST	storage tank
SF	solar fraction	t	transversal
SPBP	simple payback period (year)	u	useful
T	temperature ($^\circ\text{C}$)	w	water
t	time (s)		
U	overall heat loss coefficient ($\text{W}/\text{m}^2 \text{K}$)		

single-effect chillers is about 80–100 $^\circ\text{C}$, while their COP is limited to around 0.7 [11]. Double- and triple-effect chillers, on the other hand, require driving temperatures of around 180–240 $^\circ\text{C}$, and can reach COPs of up to 1.4 and 1.8, respectively [11].

The majority of solar absorption chillers installed around the world are based on single-effect chillers and low-temperature solar thermal flat plate or evacuated tube collectors (FPCs and ETCs) [12,13]. This configuration is usually considered as the most promising design in European climates [14]. The main drawback of solar single-effect chillers is the low COP of the chiller, requiring a large collector area to provide the thermal energy demand. In addition to the cost of large collector areas, this may be a significant limiting factor for the use of such systems in buildings with limited available rooftop area.

The combination of high-temperature solar thermal collectors and multi-effect absorption chillers is becoming more attractive due to their higher COP compared to single-effect chillers [15,16]. This means that the multi-effect chillers require less solar thermal energy (and potentially less collector area) to supply a given amount of cooling. However, they require very high driving temperatures which can only be achieved by more expensive collectors and pipework. If concentrating collectors are used, they have a lower solar gain per unit area because they can only utilize the direct normal irradiance (DNI) as opposed to FPCs and ETCs which can also harness solar diffuse radiation [17]. This disadvantage may be partially compensated by employing tracking systems, but these require regular maintenance, especially in dusty environments. Therefore, it is not clear if solar-powered multi-effect

Download English Version:

<https://daneshyari.com/en/article/7161039>

Download Persian Version:

<https://daneshyari.com/article/7161039>

[Daneshyari.com](https://daneshyari.com)