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Dynamic performance assessment of a solar-assisted desiccant-based air handling unit in two Italian cities



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ABSTRACT

Desiccant-based air handling units can provide significant operational advantages and can use solar energy as the main heat source. Hereinafter a plant equipped with a silica-gel desiccant wheel is analyzed for two Italian locations (Benevento and Milano).

A parametric study involving collectors types, surfaces, tilt angles and installation site has been performed. The proposed system has been compared with a conventional HVAC unit, through dynamic simulations. In terms of energy and environmental analysis, solar desiccant systems should always be preferred to conventional ones, even when the solar thermal energy surplus is fully dissipated. A maximum primary energy saving of about 10% and 20% with flat plat and evacuated tube collectors, respectively, occurs in both locations. The savings increase up to about 58% and 72% in Benevento and 43% and 58% in Milano, when the solar heat excess is completely used for further energy demands.

One observes that systems with evacuated tube collectors are preferable where the available space for the solar field is small, instead with larger surfaces flat plate collectors are advantaged.

In terms of economic analysis, the shortest payback periods are 6 and 8 years for Benevento and Milano, respectively.

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1. Introduction

In the summer operation mode of conventional Heating, Ventilation and Air Conditioning systems (HVAC) the most energyintensive process consists of the air cooling and dehumidification. Mechanical dehumidification is commonly used to reduce the moisture content of the air flow. This process takes place by reducing the air temperature to low values, lower than the dew point temperature. Alternatively the hygroscopic properties of some materials can be exploited. These substances, such as silica gel, need to be periodically regenerated with low temperature heat. Waste heat [1] from cogeneration devices [2–4], from industrial processes [5,6] or solar thermal energy [7,8] is typically used as thermal energy for regeneration.

Desiccant and Evaporative Cooling systems (DEC) can achieve benefits such as a more accurate humidity control, a better indoor air quality, a significant reduction in CO_2 emissions, primary energy and electricity savings [9] but they are more expensive and more complex from a technological and operational point of view. In addition Solar-assisted Desiccant and Evaporative Cooling systems (SDEC) are equipped with a solar field to collect solar radiation, as well as with back-up systems and heat storage tanks. The

* Corresponding author. *E-mail address:* francesco.tariello@unisannio.it (F. Tariello). last two components are considered to compensate the uncertainty of the source and improve its exploitation.

Numerous parameters affect the operation of DEC and SDEC systems. They have been studied in many papers with different approaches, also with non-conventional layouts. For example, a mathematical model was introduced and experimentally validated by Elzahzby et al. [10]. It is realized to preventively evaluate the performance of a solar-driven hybrid air-conditioning system. It is a one-rotor six-stage unit. A two-stage dehumidification, two-stage precooling and two-stage regeneration process is realized in only one silica-gel desiccant wheel (DW). In terms of thermal COP it was highlighted that it decreases from a maximum value of 2.2 to a minimum of 0.7 increasing the regeneration temperature and the DW rotation speed. Instead thermal COP varies between 1.1 and 0.6 varying regeneration air velocity.

Li et al. [11] arranged a Matlab/Simulink model of a solar heating and cooling desiccant system coupled with solar air collectors. The simulated results showed good agreement with experimental data and so the simulator was used to optimize collector parameters: area, air leakage and insulation. The authors found that thermal COP of the DEC system is about 0.35 and about 76% of the total cooling is provided by the solar-assisted HVAC system. Regarding the seasonal total heating load, about 49% can be handled by solar energy. Nomenclature

Α	area (m ²)	
a_1	efficiency slope $(W/(m^2 K))$	
02	efficiency curvature $(W/(m^2 K^2))$	
с	unitary cost $(\ell/N m^3)$ or $(\ell/W h)$ or (ℓ/m^2)	
c c	charge cost $(U/kg K)$	
c_p	specific field $(J/(Kg K))$	
C	valorization coefficient (ϵ/m^2)	
CO_2	equivalent CO ₂ emission (kg/y)	
EC	extra cost (€)	
En	primary energy (kW h/y)	
$\vec{F_1}$	potential	
E _n	notential	
Г <u>2</u> Г	cash flow per year (Chu)	
г С	cash now per year (e/y)	
G	total incident radiation (W/m ²)	
g	total solar energy transmittance	
I _{a,tot}	annual incentive (€/y)	
k	tank fluid thermal conductivity (W/(m K))	
LHV	Lower Heating Value (kW h/Nm^3)	
m	mass of node (kg)	
MC	annul maintenance $\cot(E/u)$	
WIC	annul maintenance $\cos(e/y)$	
тс	specific annual maintenance cost (%/y)	
m_{down}	bulk fluid flowrate down the tank (kg/s)	
\dot{m}_{up}	bulk fluid flowrate up the tank (kg/s)	
\dot{m}_{1in}	mass flowrate entering at inlet 1 (kg/s)	
\dot{m}_{1out}	mass flowrate leaving at outlet 1 (kg/s)	
m	mass flowrate entering at inlet 2 (kg/s)	
m _{2m}	mass flowrate leaving at outlet 2 (kg/s)	
M ² out	number of years	
IN OC	number of years	
UC .	operating cost (e/y)	
PES	primary energy saving	
S	gross solar collector area (m ²)	
t	temperature (°C)	
Т	temperature (K)	
T	temperature of the fluid entering at inlet 1 (K)	
T_{1m}	temperature of the fluid entering at inlet 2 (K)	
12in	temperature of the huld entering at finet 2 (K) total lass coefficient $(M/(m^2 K))$	
0		
V	volume (N m ² /y)	
Greek syr	nbols	
α	specific emission factor of electricity supplied by the	
	$arid (kaCO_{-}/kW h_{-})$	
0	grid (RgCO ₂ /RW fiel)	
р	specific emission factor for primary related to natural	
	gas combustion ($kgCO_2/kW h_{Ep}$)	
ΔCO_2	equivalent CO_2 avoided emission	
Δk	de-stratification conductivity (W/(m K))	
ΔT	temperature difference (K)	
ΔT_{ln}	logarithmic mean temperature difference (K)	
Δχ	distance between node <i>i</i> and the node below it $(i + 1)$	
$\Delta r_{l+1} \rightarrow l$	(m)	
A	$\begin{pmatrix} 111 \\ d_{i} \\ d_{i$	
$\Delta x_{i-1 \rightarrow i}$	distance between node <i>i</i> and the node above it $(i - 1)$	
	(m)	
ΔU	additional loss coefficient (W/(m ² K))	
η	efficiency	
n _B	boiler efficiency	
nal	collector efficiency	
1100 1100	Italian national electric system efficiency	
TEG	intercept officiency	
1/0 -	time (a) or (b)	
τ	time (s) or (n)	

ω	air humidity ratio (g/kg)	
Subscripts		
Subscript.	ambiant	
u a		
aux	auxiliaries	
В	boiler	
С	cross section area of the node	
chil	chiller	
col	collector	
el	electrical	
F1	notential	
F _o	notential	
hy	heat exchanger	
11X ;	neat excitatiget	
1	generic node	
in	inlet	
j	generic air state	
k	generic year	
NG	natural gas	
r	generic bracket	
S	surface of the node	
tank	storage tank	
th	thermal	
tot	total	
101		
Superscrip	pts	
AS	Alternative System	
CS	Conventional System	
Acronyms	5	
AHU	air handling unit	
AS	Alternative System	
R	hoiler	
BN	Benevento	
	cooling coil	
CC CF		
CF	cross-flow neat exchanger	
СН	chiller	
COP	coefficient of performance	
CS	Conventional System	
DEC	Desiccant and Evaporative Cooling	
DHW	domestic hot water	
DW	desiccant wheel	
EC	evaporative cooler	
HC	heating coil	
HC2	nost-heating coil	
	Heating Degree Day	
	Heating Ventilation and Air Conditioning systems	
HVAC	Heating, ventriation and An Conditioning systems	
HVV	not water	
HW-HX	hot water heat exchanger	
LHV	Lower Heating Value	
MI	Milano	
PV	photovoltaic cell	
PVT	photovoltaic-thermal collector	
SC	solar thermal collectors	
SDFC	solar-driven desiccant and evaporative cooling system	
SDLC	Simple Day Back	
JFD TC	Simple ray Dack	
12	lank storage	

As concern the solar technologies, in the literature solar air collectors, flat plate and evacuated tube collectors are typically considered. However, in few cases, also hybrid devices (Photovoltaic-Thermal collectors, PVT), or concentrated thermal collectors and concentrated hybrid devices (Concentrated Photovoltaic Thermal collectors) are adopted.

Bourdoukan et al. [12] developed and experimentally validated the simulation model of a solar heat pipe vacuum collectors with a stratified tank under various operation conditions. These components were simulated in combination with a desiccant based air handling unit (AHU) in three different locations characterized by different climates. They demonstrated to be more efficient than Download English Version:

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