



Optimization, selection and feasibility study of solar parabolic trough power plants for Algerian conditions



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ABSTRACT

In the present study, optimization of two parabolic trough solar thermal power plants integrated with thermal energy storage (TES), and fuel backup system (FBS) has been performed. The first plant uses Therminol VP-1 as heat transfer fluid in the solar field and the second plant uses molten salt. The optimization is carried out with solar multiple (SM) and full load hours of TES as the parameters, with an objective of minimizing the levelized cost of electricity (LCOE) and maximizing the annual energy yield. A 4E (energy–exergy–environment–economic) comparison of the optimized plants alongside the Andasol 1 as reference plant is studied. The molten salt plant resulting as the best technology, from the optimization and 4E comparative study has been chosen for the viability analysis of ten locations in Algeria with semi-arid and arid climatic conditions. The results indicate that Andasol 1 reference plant has the highest mean annual energy efficiency (17.25%) and exergy efficiency (23.30%). Whereas, the highest capacity factor (54.60%) and power generation (236.90 GW h) are exhibited by the molten salt plant. The molten salt plant has least annual water usage of about 800,482 m³, but demands more land for the operation. Nevertheless the oil plant emits the lowest amount of CO₂ gas (less than 40.3 kilo tonnes). From the economic viewpoint, molten salt seems to be the best technology compared to other plants due to its lowest investment cost (less than 360 million dollars) and lower levelized cost of electricity (LCOE) (8.48 ¢/kW h). The viability study proposes Tamanrasset, as the best location for erection of a parabolic trough solar thermal power plant with a low LCOE of 7.55 ¢/kW h, and a high annual power generation (more than 266 GW h). According to the feasibility analysis, the semi-arid and arid Algerian sites are suitable for realization of PTSTPP with integrated TES and FBS; especially the southern locations (19°N–32°N, 8°W–12°E).

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1. Introduction

Algeria is located in north-west Africa, between 19° and 38° north latitudes and 8° west and 12° east longitudes, with a total area of 2,381,741 km². The country is by far the largest African country and has significant variations in its climatic, topographic and socio-economic characteristics [1]. Algeria, with a total population of 37.9 million inhabitants (till January 2013), from more than 8.68 million in 1948, has experienced a growth of over 250% in population during the last 50 years [2].

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Algeria is one of the most important players in African and world energy markets, both as a significant hydrocarbon producer and as an exporter. According to the International Energy Agency (IEA) statistics for 2011, Algeria has produced a total amount of energy of 145,846 kTOE (1,696,188 GW h). The main sources of this energy production are from crude oil (52.10%), followed by gas (44.80%). The energy needs have increased due to population growth and economic development over the last decades. The energy consumption of Algeria was 41,852 kTOE (486,739 GW h) in 2011 with CO₂ emissions more than 123,475 kilo tonnes [3].

Algeria is experiencing a continual increase in population, energy consumption, gases emissions, and major changes in economic trends in the last decades. In view of these factors and abiding the Kyoto Protocol, the Algerian government has launched the renewable energy and energy efficiency program. This program was launched in 2011, with a total cost of 120 billion USD [4]. The program leans on a strategy focused on developing and expanding the use of inexhaustible energy resources, such as solar

Nomenclature

A	collector's aperture area (m^2)	S	sunshine duration (hr).
C_{env}	environmental cost according to CO_2 rejected (US\$)	S_0	maximum possible sunshine duration (day length) (hr).
CF	capacity factor	S_{SF_i}	entropy at the inlet of the SF ($\text{kJ/kg } ^\circ\text{C}$)
C_{inv}	total investment cost (US\$)	S_{SF_o}	entropy at the outlet of the SF ($\text{kJ/kg } ^\circ\text{C}$)
$C_{O\&M}$	annual operating and maintenance costs (US\$)	T_{amb}	ambient temperature (K)
crf	capital recovery factor	T_{sun}	temperature of the sun (K)
d_r	relative earth–sun distance	W_{des}	design cycle thermal requirement (kW)
$\dot{E}x_i$	exergy received by the SF (kW h)	δ	declination angle ($^\circ$)
$\dot{E}x_{in}$	total exergy received by the PB (kW h)	ω_s	sunrise hour angle ($^\circ$)
$\dot{E}x_u$	useful exergy delivered by the receiver (kW h)	φ	latitude ($^\circ$)
f	dilution factor (1.3×10^{-5}) [30]	$\eta_{cyclesdes}$	design point cycle efficiency
f_{backup}	fossil fill fraction ($0 < f_{backup} < 1$)	$\eta_{I,O}$	overall energy efficiency of the plant
h_{SFo}	enthalpy at the outlet solar field (kJ/kg)	$\eta_{I,PB}$	energy efficiency of the PB
h_{SF_i}	enthalpy at the inlet of the SF (kJ/kg)	$\eta_{I,SF}$	energy efficiency of the SF
H_0	monthly mean daily extraterrestrial solar irradiance on a horizontal surface (kW/m^2)	$\eta_{II,O}$	overall exergy efficiency of the plant
H_{BN}	monthly mean daily direct normal irradiance (kW h/m^2)	$\eta_{II,PB}$	exergy efficiency of the PB
\bar{H}_{BN}	monthly direct normal irradiance (kW/m^2)	$\eta_{II,SF}$	exergy efficiency of the SF
$\bar{\bar{H}}_{BN}$	annual direct normal irradiance (kW/m^2)	θ	angle of incidence (degree)
H_D	monthly mean daily diffuse solar irradiance on a horizontal surface (kW/m^2)	Δt_{es}	total number of desired storage hours (h)
H_G	monthly mean daily global solar irradiance on a horizontal surface (kW h/m^2)		
I_{BH}	monthly mean hourly direct solar irradiance on a horizontal surface (kW/m^2)	Abbreviation	
I_{BN}	monthly mean hourly direct normal irradiance (kW/m^2)	4E	energy–exergy–environmental–economic
I_{sc}	solar constant (kW/m^2)	FBS	fuel back-up system
I_D	monthly mean hourly diffuse solar irradiance on a horizontal surface (kW/m^2)	CSP	concentrating solar power
I_G	monthly mean hourly global solar irradiance on a horizontal surface (kW/m^2)	DNI	direct normal irradiance
k_d	annual discount rate	DSG	direct steam generation
\dot{m}_{PB}	mass flow rate of the HTF in the PB (kg/s)	HPT	high pressure turbine
\dot{m}_{SF}	mass flow rate of the HTF in the SF (kg/s)	HTF	heat transfer fluid
N	depreciation operation time of the system (years)	IEA	international energy agency
ND	number of the days in a year	KTOE	kilotonne of oil equivalent
PG_{net}	net power generation (kW h)	LCOE	levelized cost of electricity
\dot{Q}_{backup}	thermal energy must be supplied in the FBS (kW h)	LPT	low pressure turbine
\dot{Q}_i	total incident solar energy received by collector's aperture area (kW h)	NREL	National Renewable Energy Laboratory
\dot{Q}_{in}	total thermal energy received by the PB (kW h)	PB	power block
\dot{Q}_u	total useful energy delivered by the SF (kW h)	PTC	parabolic trough collector
\dot{Q}_{total}	the total energy needed to reach the thermodynamic state (kW h)	PTSTPP	parabolic trough solar thermal power plant
		SAM	Solar Advisor Model
		SF	solar field
		SM	solar multiple
		STEC	solar thermal electric components
		TES	thermal energy storage
		TMY	typical meteorological year

energy in order to diversify energy sources and prepare Algeria for tomorrow. The strategic choice is motivated by the enormous potential of solar energy, in which it is one of the most important sources in the world.

The geographic location in the Sunbelt region, climatic conditions such as low precipitation, plenty of unused flat land in proximity to transmission grids, road networks, and the abundant sunshine in Algeria are conducive for the production of electricity from concentrating solar thermal power [5]. The concentrating solar power (CSP) technology incorporates four different alternatives: parabolic trough power plants, linear Fresnel power plants, solar power towers and dish-Stirling systems. The parabolic trough power plant is considered as one of the most proven, mature and commercial concentrating solar power for implementation in arid and semi-arid regions [6]. It focuses sunlight onto a solar receiver by using mirrors, which is finally converted to heat or electricity. This technology ranges from remote power systems of few kilowatts to grid-connected power plants of hundreds of megawatts

[5]. In general parabolic trough solar thermal power plant (PTSTPP) consists of a solar field, power block, and thermal energy storage (TES). In addition to these systems, a fuel back-up system can be used for enhancing the plant's potential [7]. The levelized cost of electricity (LCOE) is a decisive parameter for feasibility analysis of solar thermal power plants [8]. The LCOE depends on plant configuration, working fluid, performance of the plant, and capital, operation and maintenance costs of the plant. Large number of researchers and academicians across the globe are working in this direction. Most of these studies and projects are based on oil or water-steam as heat transfer fluids in the solar field. Reddy and Kumar [6] analyzed a design for a solar parabolic trough field for power generation using oil and water as working fluids, and studied the feasibility of this technology under Indian climatic conditions. A comparative study in terms of design, yield and investment analyses between plants using oil and water as heat transfer fluid (HTF) with integrated solar thermal storage has been conducted by Feldhoff et al. [9]. According to them, the main

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