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A three-dimensional phase field model coupled with a lattice kinetics solver for modeling crystal growth in furnaces with accelerated crucible rotation and traveling magnetic field

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ABSTRACT

In this study, we present a new three-dimensional numerical model for crystal growth in a vertical solidification system. This model accounts for buoyancy, accelerated crucible rotation technique (ACRT), and traveling magnetic field (TMF) induced convective flow and their effect on crystal growth and the chemical component's transport process. The evolution of the crystal growth interface is simulated using the phase-field method. A semi-implicit lattice kinetics solver based on the Boltzmann equation is employed to model the unsteady incompressible flow. A one-way coupled concentration transport model is used to simulate the component fraction variation in both the liquid and solid phases, which can be used to check the quality of the crystal growth. Numerical results indicate that ACRT can slightly increase the quality of grown crystal, but the effect of TMF on quality of grown crystal depends on the temperature profile of the ampoule wall. Finally, excellent scalability of our developed parallel methods is demonstrated on the three-dimensional cases.

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1. Introduction

Due to the importance of crystals in a number of medical imaging applications and radiation detection [1-3], numerical simulations of crystal growth from the melt in vertical gradient furnaces [4,5] have attracted significant attention.

Vertical growth techniques include both high- and ambientpressure methods with recent advances in ambient-pressure methods at the forefront [3]. Ambient-pressure methods offer reduced experimental complexity and have been shown to produce large single-crystal volumes with properties as good or better than high-pressure methods. Thus, there has been a shift toward lowpressure methods using vertical gradient furnaces and sealed ampoule growth [3]. However, material uniformity, property homogeneity, and crystal defects remain difficult problems to solve for certain systems grown in this manner, such as cadmium zinc telluride (CZT). Modeling and simulation techniques are promoted as vehicles toward understanding the solidification process in complex systems and are thought to provide a more systematic method for determining optimal growth conditions and improved materials.

Recent advances in computer models for growth processes in the vertical gradient furnace have been useful in understanding

the general effects of furnace operating conditions on the growth of crystals [6]. As such, computer models have become a valuable tool in furnace design and the optimization of operating conditions [7–11]. At the same time, most existing models use a simplistic description of the crystal/melt interface and its dynamic. Furthermore, in these models, it is assumed that latent heat dissipates without disturbing the continuity of the heat fluxes at the interface. This approach fails to account for the effects of crystal anisotropy and solidification kinetics, which may be important in the simulations of crystal dendritic growth or lateral overgrowth [12,13]. Applying a traveling magnetic field (TMF) to the verticalgradient furnace is a direct way to introduce a body force in the direction of gravity [14-16]. TMF can adjust the magnitude of the force by adjusting the strength of the electric current. As such, we believe TMF can be used to affect crystal guality in the vertical solidification system. The accelerated crucible rotation technique (ACRT) is applied to the vertical solidification system to improve mixing in the melt [17-21], which can increase the quality of crystal growth. Already, we have developed a phase-field-based model to simulate crystal growth in the vertical gradient furnace [22]. The model accounts for anisotropy in kinetic and interfacial free energy coefficients, as well as the effect of front curvature on crystal growth. The model was used to study the effects of ACRT and TMF on crystal growth in a prototypical vertical gradient furnace.





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Nomenclature

α	thermal diffusion coefficient [m ² s ⁻¹]	<i>a</i> ₂	phase field model parameter
α_l	thermal diffusion coefficient of liquid phase [m ² s ⁻¹]	a_s	anisotropy strength
α_s	thermal diffusion coefficient of solid phase [m ² s ⁻¹]	С	non-dimensional chemical components' concentration
β	kinetic coefficient [s m ⁻¹]	$c _l$	non-dimensional chemical components' concentration
β_T	coefficient of thermal expansion $[K^{-1}]$		at solid–liquid interface in liquid side
Δt	time step interval [s]	$c _{s}$	non-dimensional chemical components' concentration
Δx	mesh size [m]		at solid-liquid interface in solid side
ϵ	phase field model parameter	C_p^l	specific heat capacity of liquid [J kg ⁻¹ K ⁻¹]
η	derivative of pressure with respect to density $[m^2 s^{-2}]$	C_n^s	specific heat capacity of solid $[] kg^{-1} K^{-1}]$
Γ	interface between liquid and solid phases	C_r^p	reference chemical components' concentration
λ	parameter that controls the strength of the coupling be-	Clks	lattice sound speed $[m s^{-1}]$
	tween the phase and diffusion fields	C _{lk}	reference lattice speed $[m s^{-1}]$
μ	liquid dynamic viscosity [kg m ⁻¹ s ⁻¹]	d_0	capillary length [m]
μ_m	magnetic permeability [H m ⁻¹]	D_l	chemical component diffusion coefficient in liquid
$\frac{V}{\nabla^2}$	differential operator in Cartesian coordinate system		phase [m ² s ⁻¹]
V-	second-order differential operator in Cartesian coordi-	D_s	chemical component diffusion coefficient in solid phase
~ 2	nate system		$[m^2 s^{-1}]$
$\nabla_{r,z}^2$	second-order differential operator in axisymmetric	f_{\dots}	particle distribution function [kg m ⁻³]
0	coordinate system	f_{il}^{eq}	discretized equilibrium Maxwell distribution [kg m ⁻³]
Ω	entire domain containing both liquid and solid phase	$f_{il,\rho}$	discretized particle distribution function for density
ω	demain accurrent angular frequency [HZ]		$[\text{kg m}^{-3}]$
Ω_g	domain occupied by new grown solid phase	${f}_{il, \vec{u}}$	discretized particle distribution function for velocity
Ω_l	domain occupied by the reliduid phase		[kg m ⁻³]
52 _S	aloctric current phase shift between soils	f _{il}	discretized particle distribution function [kg m ⁻³]
φ_n	phase field	Н	height of ampoule [m]
ψ	pliase lielu donsitu [kg m $^{-3}$]	h	heat transfer coefficient [W m ⁻² K]
ρ	density of liquid $[kg m^{-3}]$	Jo	electric current density [A m ⁻²]
P_l	density of solid $[kg m^{-3}]$	k	segregation coefficient
ρ_s	electrical conductivity [s m ⁻¹]	K _l	thermal conductivity of liquid [W m ⁻¹ K ⁻¹]
τ	characteristic time of attachment of atoms at the inter-	Ks	thermal conductivity of solid [W m ⁺ K ⁺]
L	face [s]	L	latent neat [] kg *]
Tell Tell	tangential coordinates of curvilinear coordinate system	IN	total number of lattice directions excluding the station-
•\$1,1,•\$1,2	moving with the interface [m]		ary 0 direction
r	linear relaxation parameter	n n	norm coordinate of amplifuncer coordinate system mov
c	values at the beginning of the time step	n _{sl}	ing with the interface [m]
$\dot{\varsigma} + 1$	values at the end of the time step	D	radius of ampoule [m]
θ	surface tension $[kg s^{-2}]$	r	r direction in axisymmetric coordinate system distance
\vec{e}_z	unit vector of z direction [m]	I	from the centerline of amoule [m]
\vec{e}_{il}	particle velocity [m s ⁻¹]	S.	thermal source term caused by phase filed transition
F	total external forces $[\text{kg m}^{-2} \text{ s}^{-2}]$	J_{ψ}	[K s^{-1}]
\vec{F}_L	time-averaged Lorentz force per volume [kg m ⁻² s ⁻²]	Т	temperature [K]
ġ	gravity acceleration [m s ⁻²]	t	time [s]
$\vec{n}_{sl,x}$	x component of normal direction of the solid-liquid	T _o	reference temperature [K]
	interface [m]	T _c	cold end temperature [K]
$\vec{n}_{sl,y}$	y component of normal direction of the solid-liquid	T_{h}	hot end temperature [K]
	interface [m]	T_i^n	interface temperature [K]
$\vec{n}_{sl,z}$	z component of normal direction of the solid-liquid	T_m	melting temperature [K]
_	interface [m]	T_{w}	ampoule wall temperature [K]
\vec{n}_{sl}	normal direction of the solid–liquid interface [m]	U	magnitude of velocity $[m s^{-1}]$
S_0	total momentum source term [kg m ⁻² s ⁻¹]	и	velocity component in x direction [m s ^{-1}]
S _{0b}	momentum source caused by buoyancy force	U_{pull}	ampoule pulling speed [m s ^{-1}]
z	$[kg m^2 s^2]$	v	velocity component in y direction $[m s^{-1}]$
S _{0L}	momentum source caused by Lorentz force [kg m ⁻² s ⁻¹]	V_i	normal interfacial velocity $[m s^{-1}]$
u i	velocity vector [m s ⁻¹]	W	interface thickness [m]
u_p	velocity of particles in Boltzmann equation [in s *]	w	velocity component in z direction $[m s^{-1}]$
\vec{u}_{wall}	velocity of the ampoule wall [m s ⁻¹]	W_0	phase field model parameter for interface thickness [m]
x	position vector in Cartesian coordinate system [m]	x, y, z	coordinates in Cartesian coordinate system [m]
\widetilde{F}_{il}	external forces in lattice scheme $[kg m^{-3} s^{-1}]$	Zi	position of solid-liquid interface [m]
A_1	in-phase components of magnetic potential [V s m^{-1}]	Z_{i0}	initial position of solid-liquid interface [m]
<i>a</i> ₁	phase field model parameter		
<i>A</i> ₂	out-of-phase components of magnetic potential		
	[V s m ⁻¹]		

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