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Integrated decision making for the optimal bioethanol supply chain



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ABSTRACT

Bioethanol production poses different challenges that require an integrated approach. Usually previous works have focused on specific perspectives of the global problem. On the contrary, bioethanol, in particular, and biofuels, in general, requires an integrated decision making framework that takes into account the needs and concerns of the different members involved in its supply chain.

In this work, a Mixed Integer Linear Programming (MILP) model for the optimal allocation, design and production planning of integrated ethanol/yeast plants is considered. The proposed formulation addresses the relations between different aspects of the bioethanol supply chain and provides an efficient tool to assess the global operation of the supply chain taking into account different points of view. The model proposed in this work simultaneously determines the structure of a three-echelon supply chain (raw material sites, production facilities and customer zones), the design of each installed plant and operational considerations through production campaigns. Yeast production is considered in order to reduce the negative environmental impact caused by bioethanol residues. Several cases are presented in order to assess the approach capabilities and to evaluate the tradeoffs among all the decisions.

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1. Introduction

Nowadays, new perspectives have arisen around the firms integration resulting in new strategic challenges. Different entities or enterprises (suppliers, industrial facilities, warehouses, clients, etc.) integrate their activities in order to achieve global objectives. Generally, they do not belong to the same company, work in different trades and common actions affect their operations and performances. Previous approaches have pursued individual objectives, neglecting the combination of the units in the network. In this context, a supply chain (SC) is a common option where a set of units (e.g. suppliers, plants, warehouses, customers) makes a set of activities ranging from the purchase of raw materials to the transportation of finished products to clients. Thus, a first integration requirement can be posed respect to the links among the SC members.

In order to achieve an appropriate coordination, many decisions have to be taken into account. They can be classified into three levels regarding to their significance and the time period required in the planning horizon. Firstly, decisions about location, sizing and technology of plants and distribution centers are generally classified as strategic and they correspond to a planning horizon of several years. In a second level, procurement, product assignment as well as distribution channel and transportation policy are considered as tactical decisions and they can be reviewed every few months. Finally, production planning, and the distribution of raw material, semi-finished and finished products in the supply chain are considered as operational decisions that are easily changed in the short term [1].

In general, previous works have addressed decision levels in hierarchical approaches in which SC design is first determined. SC design has been traditionally defined by determining the number and location of production plants, the sizing for each facility, and the flows among the different nodes of the network, pursuing economic objectives. Then, for each plant involved in the network, plant design decisions are made. Finally, planning decisions are determined using demand targets previously defined. On the other hand, there are few works dealing with SC design where first the plants are designed and then the surrounding SC. For example, in Baliban et al. [2] the synthesis and design of a thermochemical refinery is first solved and, then, in Elia et al. [3] the SC network of this kind of plants is designed. However, these hierarchical approaches do not consider any interactions between decision making levels and thus the SC design and planning decisions may result in suboptimal or even infeasible plant planning problems. Due to significant relations between decisions levels, it is necessary to consider the simultaneous optimization in order to determine the global optimal solution and to assess the tradeoffs among the different elements involved. Thus, a second integration

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Nomenclature			
Indices		NBC ^{UP}	maximum number of batches of product i in the cam-
afer	alcohol fermentor	,	paign of plant f
b	batch	NN_{f}^{LOW}	left end of discretization interval of variable NN _f
bak	baker's yeast	NN_{f}^{UP}	rigth end of discretization interval of variable NN_f
bfer	biomass fermentor	<i>Oper_{if}</i>	operation cost coefficient for product <i>i</i> in plant <i>f</i>
C	customers zone centrifuge	Q_{if}^{UP}	upper bound for the production of product i in plant f
cen cream	centrifuged cream	Q_{s}	maximum amount of sugar cane
d	points for discretizing the number of campaign repeti-		discrete size m for semicontinuous units in stage j at
	tions	<i>RF_{jmf}</i>	plant f
dis	distillation	SF _{ij}	size factor of product <i>i</i> in batch stage <i>j</i>
et	ethanol	T_{ij}	processing time for product <i>i</i> in stage <i>j</i>
f	production plant	tt _{df}	<i>d</i> -th point obtained from the discretization of variable
i	product		NN _f
j k	stage unit	VF _{jpf}	discrete size p for batch units in stage j at plant f
l l	slot	α_{jf}	cost coefficient for batch units of stage <i>j</i> at plant <i>f</i>
n. m	discrete size for semicontinuous unit	β_{jf} $ ho_i$	cost exponent for batch units of stage <i>j</i> at plant <i>f</i> conversion factor, <i>i</i> = tor, bak
M _{if}	number of available discrete sizes for a unit of semicon-	p_1	
55	tinuous stage j of plant f	Binary V	ariables
mol	molasses	ex _f	indicates if plant f is installed
п	number of batches of a product	NNC _{df}	specifies if the campaign of plant f is repeated tt_{df} times
р Р	discrete size for batch unit number of available discrete sizes for a unit of batch	2	over the time horizon H_f
P_{jf}	stage j of plant f	r_{jmf}	denotes if the units of semicontinuous stage j at plant f
r	raw material		have size <i>m</i>
S	raw materials site	v_{jpf}	denotes if the units of batch stage j at plant f have size p denotes if n batches of product i are processed in the
tor	torula	χ_{inf}	campaign of plant f
vin	vinasses	Y _{bjklf}	denotes if <i>b</i> is assigned to slot <i>l</i> and processed in unit <i>k</i>
		bjikij	of stage <i>j</i> in plant <i>f</i>
Sets		Z _{jkf}	specifies if unit <i>k</i> of stage <i>j</i> at plant <i>f</i> is employed
BI_i	batches of product <i>i</i> proposed for the production cam- paign		
EBi	batch processing stages used for producing <i>i</i>		ous variables
ES_i	semicontinuous processing stages used for producing <i>i</i>	ANB	annual net benefit
SR _{if}	available discrete sizes for units of semicontinuous	B _{if} CTC _f	batch size of product <i>i</i> at plant <i>f</i> cycle time of the campaign of plant <i>f</i>
	stage j in plant f	e _{jkpf}	represents the bilinear term $z_{ikf} v_{ipf}$
SV_{jf}	available discrete sizes for units of batch stage <i>j</i> in plant	ee _{jkmf}	represents the bilinear term $z_{jkf} r_{jmf}$
	f	INSC	installation cost
Daramat	240	INVC	investment cost
Paramet Cap ₁	Capacity of molasses truck	IS	income for sales
Cap ₁ Cap _i	truck capacity for transporting product <i>i</i>	NB _{if}	total number of batches of product <i>i</i> processed at plant f in the time horizon H_f
CCF	capital charge factor	NBC _{if}	number of batches of product <i>i</i> included in the cam-
inc _f	fixed cost for plant f installation	NDClf	paign of plant f
Cfuel	fuel cost	NCf	number of times that the campaign of plant <i>f</i> is cycli-
CSCane _s	sugar cane procurement cost, per mass unit, in site s	2	cally repeated over the time horizon H_f
CTC_{f}^{UP}	upper bound for variable <i>CTC_f</i>	ОС	operating cost
CTIFC _{ifc}	transportation cost, per mass unit, of final product i	Q _{if}	amount of product <i>i</i> produced in plant <i>f</i>
	from plant <i>f</i> to customer <i>c</i>	QC_{ifc}	amount of product <i>i</i> sent from plant <i>f</i> to customer zone <i>c</i>
CTRAW _{sr}	f transportation cost, per mass unit, of raw material r	QM_s	amount of molasses produced at site s
ה.	from site <i>s</i> to plant <i>f</i> duty factor of product <i>i</i> in semicontinuous stage <i>j</i>	QR_{sf}	amount of molasses sent from site s to plant f
D _{ij} dist1 _{sf}	distance between raw material site <i>s</i> and plant <i>f</i>	R _{jf}	size of a semicontinuous unit in stage j of plant f
dist2 _{fc}	distance between plant f and customer zone c	ResC	disposal cost
DM_{ic}^{LO}	minimun demand of product <i>i</i> from customer zone <i>c</i>	SCC TF _{jklf}	sugar cane cost final processing time of slot <i>l</i> in unit <i>k</i> of stage <i>j</i> at plant <i>f</i>
DM_{ic}^{UP}	maximun demand of product <i>i</i> from customer zone <i>c</i>	TI _{jklf}	initial processing time of slot l in unit k of stage j at plane j at
fc_f	conversion factor that indicates the kg of molasses	јку	plant f
J-J	required to produce one L of ethanol at plant f	TRANC	transportation cost of raw materials from sites to plants
H_f	time horizon for plant <i>f</i>		and of final products from production plants to
K_{jf}	maximum number of identical parallel units that can be		customer zones
T	allowed at batch stage <i>j</i> of plant <i>f</i>	u _{ijmnf}	variable that denotes to Q_{if} if the binary variables r_{jmf} and x_{inf} simultaneously take the value 1
L_{kjf}	number of slots postulated for unit k of stage j in plant f		and <i>my</i> simulationary take the value 1

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