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Iron precipitated onto ceria-zirconia nanoparticle mixtures for the production of hydrogen via two-step thermochemical water splitting

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ABSTRACT

Several novel materials were synthesized by precipitating iron oxide (using the previously optimized 10% Fe loading by weight) onto mixtures of nanoparticle zirconia and ceria to investigate the effects of adding CeO₂ to FeO_x/ZrO₂ materials in the thermochemical water splitting reaction. At water splitting temperatures of 1000 °C (after thermal reduction at 1450 °C), the stability of the CeO₂-containing materials was lower than for the FeO_x/ZrO₂ material, and there was no advantage to adding CeO2 to the FeOx/ZrO2 material. However, when operating at a water splitting (WS) temperature of 1200 °C, the stability increased and the hydrogen production was significantly higher over most materials compared with a water splitting temperature of 1000 $^\circ\text{C}.$ At a WS temperature of 1200 $^\circ\text{C}$ the FeO_x/Zr_75Ce_{25}O_2 (75% Zr₇₅O₂ and 25% CeO₂ by weight) and FeO_x/Zr₅₀Ce₅₀O₂ materials performed slightly better than the FeO_x/ZrO₂ material, and X-ray photoelectron spectroscopy data revealed that the surface concertation of iron is less important compared with water splitting at 1000 °C. The temperature programmed reduction data indicated that the FeO_x-CeO₂ interactions were weaker compared with FeO_x -ZrO₂ interactions, since the FeO_x reduction occurred at lower temperatures for the CeO2-containing materials. The weaker interactions can explain why the stability was lower for the materials containing CeO₂ (sintering of FeO_x was likely more pronounced) The X-ray diffraction data revealed that ZrO₂-CeO₂ solid solutions formed after activation at 1450 °C and lattice volume calculations indicated that iron did incorporate into the ZrO₂-CeO₂ matrices. More incorporation was observed after water-splitting at 1200 °C compared with a lower temperature (1000 °C), and likely explains why the materials were more stable during water-splitting at 1200 °C.

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Introduction

The production of hydrogen for use as a renewable energy carrier is an attractive pathway to help mitigate the negative environmental impacts of fossil fuels [1]. Renewable hydrogen can be produced through the use of concentrated solar energy by a two-step solar thermochemical water splitting cycle. Solar energy is a largely available and abundant renewable resource and can provide the energy required to dissociate

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water into its constituent parts, hydrogen (H_2) and oxygen (O_2) . Using solar thermochemical cycles to produce hydrogen also has potential benefits of presenting higher energy conversion efficiencies than water electrolysis [2].

Several solar thermochemical water splitting cycles are based on a two-step process that utilizes a metal oxide to aid in water decomposition [1,3]. Direct water splitting, without the use of a metal oxide, is thermodynamically unfavorable and requires operating temperatures in excess of 2000 °C and is therefore incredibly energy intensive [3,4], in addition to resulting in highly explosive mixtures. In contrast, a two-step metal oxide process can significantly reduce the maximum operating temperature, and also allows for separation of H₂ and O₂ in the two steps. For a thermochemical cycle using iron oxide as the primary reactive material [5–7], the cycle can be represented by the following chemical reactions:

$3FeO + H_2O \rightarrow Fe_3O_4 + H_2$	(water splitting, WS)	Step 1
$Fe_3O_4 \rightarrow 3FeO + \frac{1}{2}O_2$	(metal oxide regeneration/ thermal reduction, TR)	Step 2

In the first exothermic step (water splitting), a reduced metal oxide (oxygen-deficient material) reacts with steam to produce hydrogen. In the second, endothermic step, the oxidized material is heated until oxygen desorbs from the material and the reduced metal oxide is regenerated. The material is then cycled back to a WS step and the TR is repeated for multiple cycles. Inert gas flows over the material during the thermal reduction to reduce the partial pressure of O_2 near the material while also preventing immediate reoxidation of the oxygen-deficient material [8]. Since the reduced metal oxide is regenerated, the net reaction is the dissociation of water to produce hydrogen and oxygen in two separate steps.

Multiple metal oxide pairs can be used for this type of thermochemical process and a lot of effort has been devoted to cycles based on iron oxide (Fe₃O₄/FeO) and cerium dioxide (ceria, $CeO_2/CeO_{2-\delta}$), although more complex mixed oxides, such as perovskites have also been used as the active metal oxide materials [1,9-34]. Oxide pairs, such as Fe₃O₄/FeO and $CeO_2/CeO_{2-\delta}$, are particularly interesting as they are nonvolatile and avoid recombination of gas phase products or immediate reoxidation of the reactive material in gas phase. The iron oxide cycle has favorable thermodynamics and multiple redox states available, but suffers from a low melting point of the reduced oxide (in a pure FeO_x cycle, FeO melts before all the Fe₃O₄ is reduced). Therefore, iron oxide must be deposited onto a high temperature, thermal shock resistant support, such as zirconia or stabilized-zirconia [35-39], to avoid detrimental melting, agglomeration and sintering. However, this introduces a large amount of inert material and, thus, reduces the thermal efficiency of the material. The iron oxide can also be doped with a component that reduces the temperature required in the thermal reduction step which can lead to further improvements [40-48]. The ceria-based cycles benefit from the ability to cycle between Ce⁴⁺ and Ce³⁺ oxidation states without structural collapse [33]. Unfortunately, the extent of reduction for ceria (i.e. the fraction of CeO_2 which is reduced to Ce_2O_3) is small at typical operating temperatures (approximately 1450 °C maximum), as temperatures closer to 2000 °C are required for a significant extent of reduction [33]. Since reducing bulk ceria is difficult at the temperatures of interest, the ceria surface is the primary region where reduction occurs [49]. To improve the reduction yield and properties of ceria, a number of dopants have been investigated [50-62]. Of particular interest is zirconium, as both experimental [62-65] and theoretical studies [66-68] reveal that this dopant can improve the oxygen storage capacity and reduction properties of ceria. By introducing Zr⁴⁺ into the CeO₂ structure, the bulk reduction of ceria is favored [62,66] allowing for a higher extent of reduction at an operating temperature of 1450 °C, and therefore a higher hydrogen production compared with pure ceria [69-76]. The smaller size of the zirconium cations can also help to alleviate strain during the cycling between Ce^{4+} and Ce^{3+} oxidation states, and detrimental sintering can also potentially be inhibited due to zirconia's high thermal resistance. However, since zirconia is an inert material, there is a limit to the benefits of zirconia addition and there exists an optimal balance between the increased reduction yields from Zr⁴⁺ addition and amount of reducible Ce^{4+} in the solid solution [71,73,75].

A potential development to the iron oxide water splitting cycle would be to decrease the amount of inert material present, perhaps by replacing at least part of the inert support material with an active material, such as ceria. While iron oxide and ceria combinations have been investigated in the water splitting reaction [54,60,77,78] (or CO₂ splitting [79]), the effects of adding iron to ceria-zirconia mixtures have only been tested in the thermochemical splitting of CO₂ [80]. Therefore, in this investigation novel iron-ceria-zirconia materials were examined for the production of hydrogen via thermochemical water splitting. More specifically, the objectives of this study were to examine the effects of ceria concentration in iron-ceria-zirconia mixed oxide materials in the water-splitting reaction and determine if the hydrogen production of these systems is enhanced compared to the ironzirconia and iron-ceria materials.

Experimental

Material synthesis

The reactive materials were synthesized by mixing commercially available nanoparticle powders of zirconia (ZrO₂) and ceria (CeO₂) (Nanostructured & Amorphous Materials Inc.) and depositing iron onto the solid mixture using a precipitation method reported previously [39]. In the precipitation method, aqueous solution of metal nitrate precursor an (Fe(NO₃)₃·9H₂O) (Alfa Aesar, 98.0–101.0%) was added to an aqueous dispersion of the support mixture. The support mixtures are labeled according to the weight percent (wt%) of ZrO_2 and CeO_2 , i.e. y wt% ZrO_2 and (100-y) wt% CeO_2 or ZryCe(100-y)O2. Therefore, Zr25Ce75O2 corresponds to a material prepared using a 25:75 mixture by weight of ZrO_2 and CeO_2 . Each ceria-zirconia mixture was prepared to have a 10 wt percent iron loading based on the optimal iron loading determined previously [39]. The resulting dispersion was

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