



ELSEVIER

Available online at [www.sciencedirect.com](http://www.sciencedirect.com)

ScienceDirect

journal homepage: [www.elsevier.com/locate/he](http://www.elsevier.com/locate/he)

# Gas-phase transport and entropy generation during transient combustion of single biomass particle in varying oxygen and nitrogen atmospheres

Linwei Wang, Nader Karimi\*, Manosh C. Paul

Systems, Power & Energy Research Division, School of Engineering, University of Glasgow, Glasgow G12 8QQ, United Kingdom

## ARTICLE INFO

### Article history:

Received 25 November 2017

Received in revised form

8 March 2018

Accepted 9 March 2018

Available online xxx

### Keywords:

Biomass

Entropy generation

Single particle combustion

Gaseous transport

Varying gas-phase atmosphere

## ABSTRACT

Transient combustion of a single biomass particle in preheated oxygen and nitrogen atmospheres with varying concentration of oxygen is investigated numerically. The simulations are rigorously validated against the existing experimental data. The unsteady temperature and species concentration fields are calculated in the course of transient burning process and the subsequent diffusion of the combustion products into the surrounding gases. These numerical results are further post processed to reveal the temporal rates of unsteady entropy generation by chemical and transport mechanisms in the gaseous phase of the reactive system. The spatio-temporal evolutions of the temperature, major chemical species including CO, CO<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub> and H<sub>2</sub>O, and also the local entropy generations are presented. It is shown that the homogenous combustion of the products of devolatilisation process dominates the temperature and chemical species fields at low concentrations of oxygen. Yet, by oxygen enriching of the atmosphere the post-ignition heterogeneous reactions become increasingly more influential. Analysis of the total entropy generation shows that the chemical entropy is the most significant source of irreversibility and is generated chiefly by the ignition of volatiles. However, thermal entropy continues to be produced well after termination of the particle life time through diffusion of the hot gases. It also indicates that increasing the molar concentration of oxygen above 21% results in considerable increase in the chemical and thermal entropy generation. Nonetheless, further oxygen enrichment has only modest effects upon the thermodynamic irreversibilities of the system.

© 2018 Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

## Introduction

It is well-established that combustion is, by far, the most irreversible process taking place in thermal power stations

[1,2]. Recent studies of coal fired power stations showed that the exergy efficiency of circulating fluidised bed boiler can be lower than 30% [3,4]. This figure clearly reflects the significant role of combustion process in exergetic losses of thermal power generation. Thus, future improvements in power

\* Corresponding author.

E-mail address: [Nader.Karimi@glasgow.ac.uk](mailto:Nader.Karimi@glasgow.ac.uk) (N. Karimi).

<https://doi.org/10.1016/j.ijhydene.2018.03.074>

0360-3199/© 2018 Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

Nomenclature	
A	pre-exponential factor, unit vary
$A_p$	particle surface area, $m^2$
$a_1, a_2, a_3$	constants
$C_D$	drag coefficient
c	concentration, $kmol/m^3$
$c_p$	specific heat capacity, $J/kg \cdot K$
$D_{ij}$	binary diffusion coefficient for the $i - j$ species pair, $m^2/s$
$D_{T,i}$	thermal diffusion coefficient for the $i^{th}$ species, $m^2/s$
$D_i$	diffusion coefficient of species $i$ , $m^2/s$
d	diameter, m
e	specific internal energy, J
E	entropy generation rate, $W/K$
$E_a$	active energy, $J/kmol$
$E_h$	rate of entropy generation due to heat transfer, $W/K$
$E_m$	rate of entropy generation due to mass transfer, $W/K$
$E_r$	rate of entropy generation duo to chemical reactions, $W/K$
$E'$	average entropy generation rate, $W/K$
$F_d$	drag force, N
$\frac{f_h}{f_i}$	fraction of heat absorbed by the particle body force per unit mass
$H_{r_{cr}}$	enthalpy of reaction $cr$ , $J/kmol$
h	specific enthalpy, $J/kmol$
$h_{fg}$	latent heat of devolatilization, $J/kg$
$h'$	enthalpy of mixture, $J/kmol$
$g_x$	acceleration gravity, $m/s^2$
$J_{i,j}$	molecular mass flux, $kg/m^3 \cdot s$
K	reaction rate, $kmol^{1-(d+e)}/(m^3)^{1-(d+e)} \cdot s$
$k_a$	rate constant of char combustion reactions, $kmol/m^3 \cdot s$
$k_c$	thermal conductivity, $K \cdot m/W$
$k_{cr}$	rate constant of reaction $cr$ , $kmol/m^3 \cdot s$
$k_d$	kinetic rate of devolatilization reaction, $s^{-1}$
Le	Lewis number
M	molecular weight, $kg/kmol$
$\bar{M}$	average molecular weight, $kg/kmol$
m	mass, kg
N	number of chemical species
$n_{cr}$	number of chemical reactions
Nu	Nusselt number
p	pressure, Pa
$p^0$	reference pressure, Pa
$Q_r$	internal production rate for thermal energy, $J/s$
$q_j$	energy flux
$\vec{q}$	heat-flux vector
$\vec{q}_R$	radiant heat-flux vector
Re	Reynolds number
Ru	universal gas constant, $kg/kmol$
$R_i$	net rate of production of species $i$ due to chemical reactions, $kg/m^3 \cdot s$
$R_{i,cr}$	chemical production rate for species $i$ , $kmol/m^3 \cdot s$
$S_E$	effective area of entropy generation, $m^2$
$\vec{s}$	entropy flux vector
s	specific entropy, $J/kmol \cdot K$
$S_b$	Stefan-Boltzmann constant, $5.67032 \times 10^{-8} W/m^2 \cdot K^4$
T	temperature, K
$T^0$	reference temperature, K
t	time, s
$t_t$	effective time of entropy generation, s
u	velocity, m/s
$\vec{u}$	velocity vector
$\vec{V}_i$	diffusion velocity of the $i^{th}$ species
$V'_{i,cr}$	stoichiometric coefficients of the reactants of species $i$ in reaction $cr$
$V''_{i,cr}$	stoichiometric coefficients of the products of species $i$ in reaction $cr$
X	mole fraction
Y	mass fraction
<b>Greek Symbols</b>	
$\alpha$	distribution coefficient of volatile in biomass
$\mu$	viscosity, $kg/m \cdot s$
$\mu_c$	specific chemical potential, $J/kg$
$\bar{\mu}_c$	Molar chemical potential, $J/mol$
$\mu_m$	molecular viscosity, $kg/m \cdot s$
$\lambda$	thermal conductivity, $W/m \cdot K$
$\rho$	density, $kg/m^3$
$\omega_i$	rate of species $i$ mass production per unit volume
$\varepsilon_p$	particle emissivity
$\theta_R$	radiation temperature, K
$\sigma$	Rate of entropy generation per unit volume, $W/m^3K$
$\Phi$	viscous dissipation
<b>Subscripts</b>	
cr	chemical reaction number
cr'	char reaction number
i	$i^{th}$ species
j	indices: 1,2, ...,N
g	gas
p	particle
rg	gaseous reactants
X	composition of chemical element H
Y	composition of chemical element O
x, r	coordinates
<b>Superscripts</b>	
$a_{i,cr}$	reaction order of species $i$ in reaction $cr$
b	temperature exponent
d	reaction order of related gaseous reactants
e	reaction order of oxygen

Download English Version:

<https://daneshyari.com/en/article/7706320>

Download Persian Version:

<https://daneshyari.com/article/7706320>

[Daneshyari.com](https://daneshyari.com)