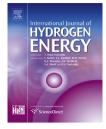


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## H<sub>2</sub> production by Escherichia coli batch cultures during utilization of acetate and mixture of glycerol and acetate



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#### ABSTRACT

Escherichia coli produces molecular hydrogen (H<sub>2</sub>) from different carbon substrates like sugars, glycerol and some organic acids during mixed-acid fermentation. H<sub>2</sub> production in batch cultures during acetate utilization of different concentrations (1 g L<sup>-1</sup>–5 g L<sup>-1</sup> was used) was investigated at different pHs. H<sub>2</sub> yield in *E*. coli wild type cells was highest at the log growth phase in the presence of 5 g L<sup>-1</sup> acetate. Either at pH 7.5 or pH 6.5 H<sub>2</sub> yield was 5.07 mmol L<sup>-1</sup>. At pH 5.5, H<sub>2</sub> production was detected when 1 g L<sup>-1</sup> acetate Was supplemented in the growth medium. Interestingly, in the presence of 1 g L<sup>-1</sup> acetate H<sub>2</sub> yield was highest at pH 6.5 compared to 2 and 5 g L<sup>-1</sup> concentrations. As acetic acid and glycerol are unavoidable constituents of various industrial or agricultural wastes, H<sub>2</sub> generation using the mixture of acetate (5 g L<sup>-1</sup>) and glycerol (10 g L<sup>-1</sup>) at different pHs was also investigated. The highest H<sub>2</sub> yield of 5.16 mmol L<sup>-1</sup> was detected at the log growth phase at pH 7.5. H<sub>2</sub> generation was continuously detected at pH 7.5 and pH 5.5 for 96 h of growth. These data can be applied to further enhancement of H<sub>2</sub> energy production biotechnology and to use different industrial or agricultural wastes where acetate and/or glycerol is present to produce H<sub>2</sub>.

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#### Introduction

The substantial shrinkage of natural gas and oil anticipates the exploration of suitable alternative and renewable energy sources. One of these sources is dihydrogen (H<sub>2</sub>), which can be evoked by diverse microbial or other biomasses and is perspective alternative to petroleum-based processes [1]. Conversion of sugars, glycerol or organic carbon-containing industrial, agricultural or water wastes to H<sub>2</sub> by microbial fermentation has been affirmed, and the description and engineering of these bioprocesses have been already developed. Co-fermentation or co-utilization of different carbon sources by various bacteria have been featured [2–6] but dependence of H<sub>2</sub> formation on different carbon sources is not clear yet, therefore investigation to disclose a cheap and effective one are highly pertinent.

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In 2006 it has been discovered that glycerol can be utilized anaerobically by Escherichia coli at acidic [7,8] and further at alkaline [9] pHs. This is essential because crude glycerol or glycerol-containing wastes are very cheap and readily available [10,11]. Furthermore, development of  $H_2$  production technology currently trends towards the use of inexpensive substrates for producing valuable fuels and chemicals from different organic acids such as formate, acetate, lactate or sugars like lactose, xylose which can be found in miscellaneous industrial or agricultural wastes [12,13].

Acetate and formate are major mixed-acid fermentation end products of *E*. coli. The high concentration of these acids inhibits bacterial cells growth [14]. The production of these two acids reaches maximal concentrations during anaerobic conditions which are an essential concern for large-scale industrial production using bioreactors [15]. During glucose fermentation by *E*. coli up to one-third of this carbon can be converted to formate reaching a concentration of ~20 mM [16]. H<sub>2</sub> production by *E*. coli from formate has been shown clearly [17–19].

Acetate or acetic acid is widely present at hydrolysates generated from hemicellulose and lignin. Acetate in concentrations >5 g L<sup>-1</sup> has inhibitory effect on the growth of *E.* coli and also reduces ethanol production by *E.* coli and *Sacharomyces cerevisiae* [20,21]. It has been shown that in the mixture of different carbon source, especially glucose and xylose, *E.* coli was engineered to remove acetate under aerobic conditions [22]. Moreover, in industrial production acetate is mainly formed, and problem is to remove and use acetate for producing various valuable chemicals and fuels.

 $H_2$  has been well established to be produced by multiple hydrogenases (Hyd), which reversibly oxidize  $H_2$  to  $2H^+$ . A large membrane-associated complex combining a hydrogenase with a formate dehydrogenase (FDH) is embodied in the formate hydrogenlyase (FHL) complex. E. coli forms two FHL complexes which are active depending on pH [17,18,23]. Hyd-3, encoded by the hyc operon, together with FDH-H forms the FHL-1 complex while Hyd-4, encoded by hyf operon, together with FDH-H is suggested to form the FHL-2 complex [17,18,23].  $H_2$  is mainly produced by FHL complex from formate [17,18,23] which further oxidizes formate to  $H_2$  and CO<sub>2</sub>. The other organic acids namely acetic acid which is generated as a byproduct from mixed-acid fermentation has been not investigated for the production of  $H_2$  by E. coli.

The main goal of the present work, therefore, was to study H<sub>2</sub> production by *E*. coli during fermentation in the presence of acetate and the mixture of acetate and glycerol at different pHs. This would be important for the removal and usage of acetate for a two- or multi-stage H<sub>2</sub> production biotechnology using glycerol and/or acetate as cheap substrates for valuable fuel production.

#### Materials and methods

#### Bacterial strain and growth

The E. coli wild type strain BW25113 from the Keio collection was used [24].

Bacteria from an overnight culture were transferred into the buffered peptone liquid medium (20 g L<sup>-1</sup> peptone, 15 g L<sup>-1</sup> K<sub>2</sub>HPO<sub>4</sub>, 1.08 g L<sup>-1</sup> KH<sub>2</sub>PO<sub>4</sub>, 5 g L<sup>-1</sup>NaCl) with sodium acetate added in a range of 1 g L<sup>-1</sup>—5 g L<sup>-1</sup> and/or glycerol 10 g L<sup>-1</sup>, as carbon sources, at different pHs. Bacteria were grown in batch cultures under anaerobic fermentative conditions at 37 °C, as described in literature [4,25]. To achieve anaerobic conditions glass vessels with plastic press caps were used; O<sub>2</sub> and N<sub>2</sub> were bubbled out of the media by autoclaving, after which the vessels were closed by presscaps. The pH was determined by a pH-meter with a selective pH-electrode (ESL-63-07, Gomel State Enterprise of Electrometric Equipment (GSEEE), Gomel, Belarus; or HJ1131B, Hanna Instruments, Portugal) and adjusted using 0.1 M NaOH or HCl.

## Measurement of redox potential and hydrogen production assays

Redox potential (ORP) determination and H<sub>2</sub> production assays were done by using a pair of redox, titanium–silicate (Ti–Si) (EO-02, GSEEE) and platinum (Pt) (EPB-1, GSEEE; or PT42BNC, Hanna Instruments, Portugal) electrodes, as described previously [4,17,18,25–27]. H<sub>2</sub> production rate (V<sub>H2</sub>) was calculated from the difference between the initial decreases in Pt- and Ti–Si-electrodes readings per time and expressed in mol H<sub>2</sub> per min per g dry weight (mol min g dw)<sup>-1</sup>; calibration of ORP decrease with H<sub>2</sub> was done as described recently by Piskarev et al. [28]. The H<sub>2</sub> yield was calculated by the marked decrease of ORP to low negative values in liquid and expressed in mol H<sub>2</sub> per L of growth medium (mol L<sup>-1</sup>); calibration of ORP decrease with H<sub>2</sub> was done as above. These expressions were presented for V<sub>H2</sub> and H<sub>2</sub> yield in batch cultures in many papers [29–31].

The  $H_2$  production assays were performed in the assay buffer (150 mM Tris-phosphate (appropriate pH mentioned) containing 0.4 mM MgSO<sub>4</sub>, 1 mM NaCl and 1 mM KCl) upon glycerol supplementation to bacterial suspension. In the assays, glycerol was supplemented at the same concentrations as added to the growth medium.

#### Others, reagents and data processing

Preparation of whole cells for  $H_2$  production assays was described before [4,17,18,25–27]. The assays were performed in a thermostatically controlled chamber at 37 °C; bacterial suspension in the closed vessel was mixed gently with a magnetic stirrer bar. Dry weight of bacteria was determined as described previously [4,32].

Agar, glycerol, peptone, sodium acetate, Tris (Carl Roths GmbH, Germany), and the other reagents of analytical grade were used.

Each data point represented is averaged from independent triplicate cultures; the standard deviation, calculated as described [4,26,32], was not more than 3% if they are not represented. The validity of differences between experimental and control data is evaluated by Student's criteria (p) [33]; p < 0.01 or less if this is not represented, otherwise p > 0.5 if the difference is not valid.

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