



Isothermal calorimeter for measurements of time-dependent heat generation rate in individual supercapacitor electrodes



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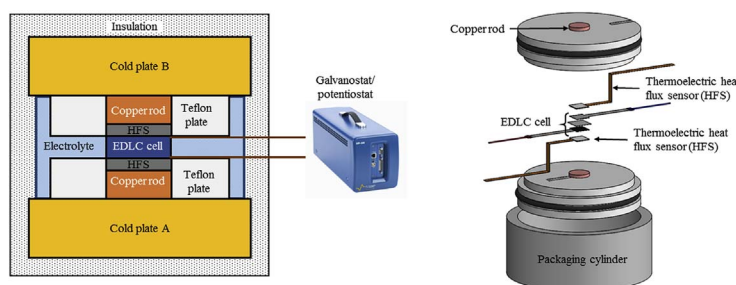
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HIGHLIGHTS

- An isothermal calorimeter was designed, manufactured, and carefully validated.
- The device can measure heat generation rate at each electrode of supercapacitors.
- Its capabilities were illustrated with EDLC electrodes and various electrolytes.
- Irreversible heat generation rate was due to Joule heating.
- Reversible heat generation rate was significantly lower at the negative electrodes.

GRAPHICAL ABSTRACT



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ABSTRACT

Heat generation in electric double layer capacitors (EDLCs) may lead to temperature rise and reduce their lifetime and performance. This study aims to measure the time-dependent heat generation rate in individual carbon electrode of EDLCs under various charging conditions. First, the design, fabrication, and validation of an isothermal calorimeter are presented. The calorimeter consisted of two thermoelectric heat flux sensors connected to a data acquisition system, two identical and cold plates fed with a circulating coolant, and an electrochemical test section connected to a potentiostat/galvanostat system. The EDLC cells consisted of two identical activated carbon electrodes and a separator immersed in an electrolyte. Measurements were performed on three cells with different electrolytes under galvanostatic cycling for different current density and polarity. The measured time-averaged irreversible heat generation rate was in excellent agreement with predictions for Joule heating. The reversible heat generation rate in the positive electrode was exothermic during charging and endothermic during discharging. By contrast, the negative electrode featured both exothermic and endothermic heat generation during both charging and discharging. The results of this study can be used to validate existing thermal models, to develop thermal management strategies, and to gain insight into physicochemical phenomena taking place during operation.

1. Introduction

Electric double layer capacitors (EDLCs) have attracted significant interest as energy storage systems thanks to their large power densities, long cycle life, and high cycle efficiency compared with batteries [1,2].

They are attractive for many applications requiring rapid charging/discharging, such as regenerative braking in hybrid or electric vehicles and renewable energy harvesting systems [2–7]. EDLC devices consist of two carbon-based electrodes and a separator immersed in aqueous or organic electrolytes. They store electric charges in the electric double

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Nomenclature			
A	Footprint area of the heat flux sensor, cm^2	T_c	Cold plate temperature, $^\circ\text{C}$
c_p	Specific heat, $\text{J}/(\text{kg}\cdot^\circ\text{C})$	T_o	Operating temperature, $^\circ\text{C}$
C_g	Gravimetric capacitance, F/g	ΔV	Voltage difference generated in the heat flux sensor, μV
I	Current, mA	<i>Greek symbols</i>	
k	Thermal conductivity, $\text{W}/(\text{m}\cdot^\circ\text{C})$	ν	Scan rate, mV/s
L	Electrode thickness, cm	ψ_s	Potential across an EDLC cell, V
m	Mass loading of active material in electrode, mg/cm^2	<i>Superscripts and subscripts</i>	
n	Cycle number, -	A or B	Refers to heat flux sensor A or B
q	Heat flux, mW/cm^2	c	Refers to charging step
\dot{q}	Volumetric heat generation rate, mW/cm^3	cd	Refers to charging-discharging cycle
\dot{Q}	Heat generation rate, mW	d	Refers to discharging step
\bar{Q}	Time-averaged heat generation rate, mW	J	Refers to Joule heating
R_i	Electric resistance of resistor or electrode “i”, Ω	$J, 1 \text{ or } J, 2$	Refers to Joule heating in Resistor 1 or 2
R_s	Internal resistance for entire EDLC device, Ω	max	Refers to maximum
S	Heat flux sensor sensitivity, $\mu\text{V}/(\text{W}/\text{m}^2)$	min	Refers to minimum
S_o	Heat flux sensor sensitivity at 22.5°C , $\mu\text{V}/(\text{mW}/\text{cm}^2)$	T	Refers to entire cell
S_c	Heat flux correction factor, $\mu\text{V}/[^\circ\text{C}(\text{mW}/\text{cm}^2)]$	rev, i	Refers to reversible in electrode “i”
t	Time, s	$+ \text{ or } -$	Refers to positive or negative electrode
t_c^-	Time immediately after the beginning of the discharging step, s		
t_c^+	Time at the end of the charging step, s		

layer (EDL) forming at the mesoporous electrode/electrolyte interfaces.

EDLCs are usually cycled at high current densities resulting in significant amount of volumetric heat generation. This, in turn, can result in excessive temperature rise during normal operation leading to (i) accelerated cell aging [3,4,8–11], (ii) increased self-discharge rates [3,8–10], and possibly (iii) electrolyte decomposition and evaporation [10,12]. Heat generation in EDLCs can be attributed to irreversible and reversible processes. Irreversible heat generation has been shown to correspond to Joule heating [2,8,13–16]. It is proportional to the square of the current and, as such, is always positive. It remains constant throughout the cell under constant current cycling [15–18]. On the other hand, recent physical modeling indicates that reversible heat generation is affected by ion diffusion, steric effects, entropy of mixing, and possible redox reactions [16,18]. It occurs mostly near the electrolyte/electrode interface where the EDL forms [16]. The amount of reversible heat generated in the device during a charging step under constant current cycling has been found, both experimentally [8,15] and theoretically [8,16,17], to be proportional to the current.

The present study aims to measure the instantaneous heat generation rates in each electrode of EDLC devices under galvanostatic cycling in order to improve our understanding of the responsible physicochemical phenomena. To do so, an isothermal calorimeter was designed, assembled, and validated to measure the time-dependent irreversible and reversible heat generation rates in each electrode of electrochemical cells. Several EDLC devices consisting of two identical electrodes made of activated carbon and different aqueous or organic electrolytes were investigated. The results will be instrumental in validating and/or improving existing thermal models and in developing thermal management strategies. They can also be used to give insight in the physicochemical processes involved in charging and discharging of electrochemical energy storage systems.

2. Background

2.1. Thermal models

Several thermal models of EDLCs have been proposed in the literature [3,8–10,15–19]. Most of them aimed to predict the temperature distribution within a cell by solving the energy equation considering Joule heating as the only source of heat generation. By contrast,

Schiffer et al. [8] developed a thermal model accounting for reversible heat generation rate through an ad hoc model based on entropy change considerations and experimental observations [8]. Their model assumed that the reversible heat generation rate was proportional to the current [8].

More recently, d’Entremont and Pilon [16] developed a spatio-temporal physical model based on first principles by coupling the heat diffusion equation with the modified Poisson-Nernst-Planck (MPNP) model to derive analytical expressions for both irreversible and reversible heat generation rates in EDLCs. The irreversible heat generation rate was attributed solely to Joule heating. By contrast, the reversible heat generation rate was attributed to diffusion, steric effects, and entropy changes [16]. Numerical simulations of the heat generation rate in a binary and symmetric electrolyte were performed for planar electrodes during constant current cycling. First, the irreversible heat generation rate was found to be proportional to the square of the imposed current I^2 . On the other hand, the time-averaged reversible heat generation rate was exothermic during charging and endothermic during discharging and proportional to the imposed current [16]. These results were in qualitative agreement with experimental data reported in the literature [8,19].

D’Entremont and Pilon [17] extended their physical model for heat generation rate in EDLCs to electrolytes consisting of multiple and/or asymmetric ion species with arbitrary ion diameter and diffusion coefficient. They observed that dissimilarity in ion valency, diameter, and/or diffusion coefficient between cations and anions of the electrolyte resulted in different heat generation rates at the two electrodes of EDLC devices [17]. In fact, larger ion valency and/or diffusion coefficient led to smaller irreversible heat generation rate due to an increase in electrolyte electrical conductivity [17]. In addition, the total reversible heat generation rate during charging was larger for smaller ion diameter and/or larger valency [17]. Additionally, d’Entremont and Pilon [18] further extended their model to hybrid pseudocapacitors to account for both electric double layer (EDL) formation and faradaic reactions in the pseudocapacitive electrode. First, carbon electrode exhibited the same thermal behavior observed in EDLC carbon electrodes [16,18]. Second, two regimes of operation were observed at the pseudocapacitive electrode namely a faradaic and a capacitive regime [18]. The faradaic regime occurred at low current densities and slow charging/discharging when the heat generation rate associated with

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